In Reply To: MS 5232

Mr. Mickey W. Shaw ATP Oil & Gas Corporation 4600 Post Oak Place, Suite 200 Houston, Texas 77027-9726

Dear Mr. Shaw:

Reference is made to the following application that has been reviewed by the Minerals Management Service:

Application Type: New Right-of-Way Pipeline

Application Date: May 23, 2005

Supplemental Data Date: June 7, 2005, June 7, 2005, November 17, 2005,

November 17, 2005, November 23, 2005, November 17,

2005, December 13, 2005

Work Description: Create 200-foot wide right-of-way and install, operate, and maintain the following:

One 6-3/4-inch pipeline 0.73 mile long to transport bulk oil from Subsea Well No. 6 through a PLET in Mississippi Canyon (MC) Block 711 and looping through Mississippi Canyon Block 755 back to Mississippi Canyon Block 711 "A". Also, an associated umbilical, 1.43 miles long, from the MC 711 "A" looping through MC 755 ending at the PLET in MC 711.

Assigned Right-of-Way Number: OCS-G26865

Assigned Segment Number: 15168 Umbilical Segment Number: 15169

Pursuant to 43 U.S.C. 1334(e) and 30 CFR 250.1000(d), your application is hereby approved.

The approval is subject to the following:

- 1) There is evidence that an historic period shipwreck may be located in the area of your proposed activities. If you discover any site, structure, or object of potential archaeological significance while conducting operations, the provisions of 30 CFR 250.194(c) requires you to immediately halt operations within the area of discovery and report this discovery to the Regional Director. Every reasonable effort must be taken to preserve the archaeological resource from damage until the Regional Director has told you how to protect it.
- 2) Our review of your application indicates that the proposed pipeline route is in the vicinity of the unidentified side-scan sonar target listed in the Enclosure, a feature that may represent a significant archaeological resource. In accordance with 30 CFR 250.194(b), you will either (1) conduct an underwater

archaeological investigation prior to commencing construction activities to determine whether this feature represents an archaeological resource, or (2) ensure that all seafloor disturbing actions required by pipeline construction avoid the unidentified feature by a distance greater than that listed in the Enclosure. Submit lay barge anchor position plats, at a scale of 1-in. = 1,000-ft. with DGPS accuracy, with your pipeline construction report required by 30 CFR 250.1008(b) that demonstrate that the feature was not physically impacted by the construction activities. If you conduct an underwater archaeological investigation prior to commencing operations, comply with the investigation methodology and reporting requirements found at: http://www.gomr.mms.gov/homepg/regulate/envir/archaeological/evaluation.html.

Your request to use navigational positioning equipment to comply with Notice to Lessees and Operators No. 98-20, Section IV.B, is hereby approved.

Please be reminded that, in accordance with 30 CFR 250.1008(a), you must notify the Regional Supervisor at least 48 hours prior to commencing the installation or relocation of a pipeline or conducting a pressure test on the pipeline. Commencement notification(s) should be faxed to (504) 736-2408. In accordance with 30 CFR 250.1008 (b), you are reminded to submit a report to the Regional Supervisor within 90 days after completion of any pipeline construction. Also in accordance with a Letter to Lessees dated April 18, 1991, a copy of the asbuilt plat(s) must be submitted to the National Ocean Service, N/CS26 Room 7317, 1315 E-W Highway, Silver Spring, MD 20910-3282

Sincerely,

Donald C. Howard Regional Supervisor Field Operations

bcc: 1502-01 Segment No. 15168, 15169, ROW OCS-G26865 (MS 5232)
MS 5250 New Orleans District w/flow schematic

MS 5232 Cartography bshrestha:bs:15168

Side	e-Scan	Sonar Targets				
	Area/ Block	-			Coordinates	Minimum Avoidance Distance(Feet)
MC	711	YES	200x30x16	X= Y=	801546.19 10248459	

Proposed Pipeline Application Review Report

Segment number: 15170

Right of Way Number: G26866

Application Date: 05/23/2005 0:00:00 Operator: ATP Oil & Gas Corporation

Operator Code: 01819

Review User: shresthb

Review Run Date: Fri Aug 12 09:44:01 2005

---- The Proposed Pipeline Pass Following Blocks -----

MC711

MC755

(1) Blocks and Leases

Lease No. Status Operator Area

G14016 SOP MC711 Anadarko E&P Company LP MC755 Nexen Petroleum U.S.A. Inc. G24105 PRIMRY

(2.3) --- Crossed Proposed Pipelines ---

Seg.No.	Row No.	Area	Product	Status	H2S	Operator-Lease/ROW Holder-ROW
15169		MC711~MC711	UMBH	PROP	N	
15168	G26865	MC711~MC711	BLKO	PROP	N	ATP Oil & Gas Corporation
15171		MC711~MC711	UMBH	PROP	N	
NO						

(8) Fish and Wildlife Service

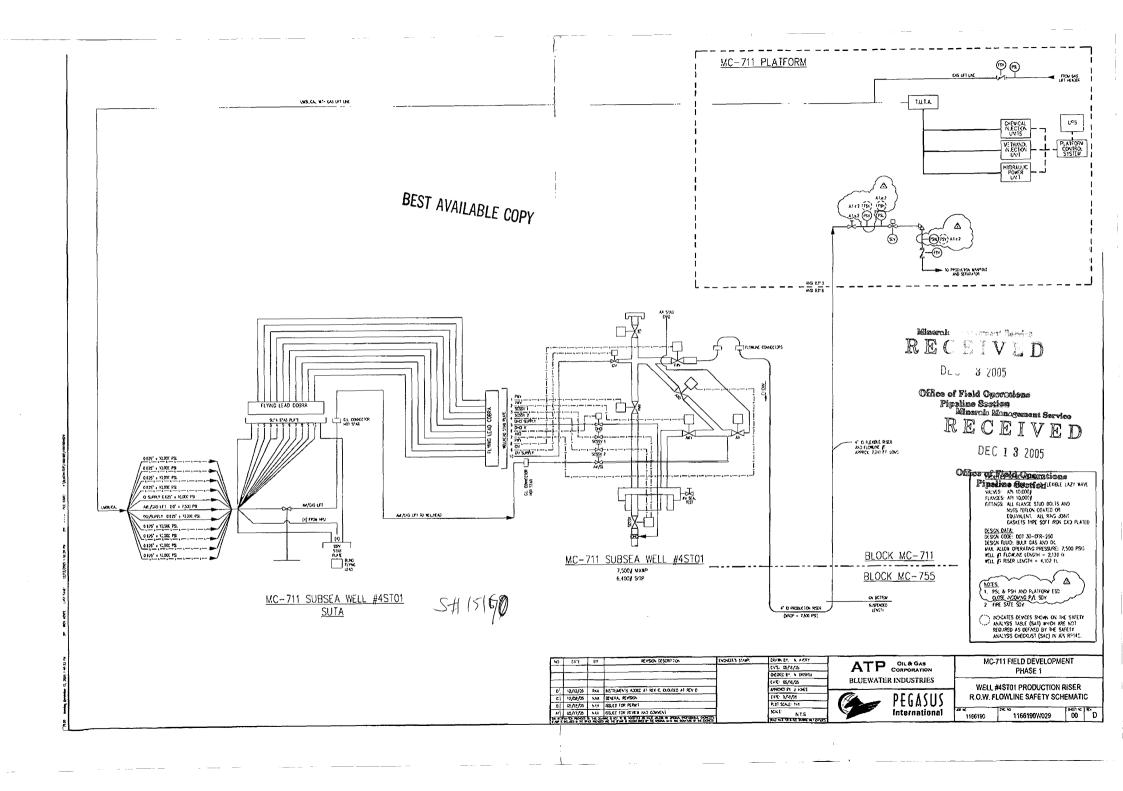
902

(10) MMS District

New Orleans

- (11) U.S. Coast Guard Morgan City COTPZ
- (15) 400 Meter Water Depth The Proposed pipeline crosses water depth greater than 400 meter area
- (17) CZM cheking louisiana CZM is required

SH 15/68/69 G 2685 MMM



MI(RC) Page 1 of 1

(3-26865)

574 15168, (9

Shrestha, Bimal

From: Sharon DeSimoni [Sharon.DeSimoni@jccteam.com]

Sent: Tuesday, August 09, 2005 1:55 PM

To: Dunlap, Karen; Shrestha, Bimal

Cc: Wetzel, Nick; Gregory Roland

Subject: ATP - (Gomez) MC 711- Plan Control No. N-8389 & Pipeline Segment No's 15168, 15169, 15170 & 15171

To all,

Please be advised that ATP met with Nexen last week regarding their objection to ATP's MC 711 Gomez Project and came to a tentative agreement. As a result Nexen will (soon) withdraw their objection to the Project.

At this time it does not appear that a meeting will be necessary.

I will keep you posted.

Thanks
Sharon
Sharon DeSimoni
J.Connor Consulting, Inc.
16225 Park Ten Place, Suite 700
Houston, Texas 77084
281-578-3388

BEST AVAILABLE COPY



tatler of No object on

NEXEN PETROLEUM U.S.A. INC. 12790 Merit Drive Suite 800 Dallas Texas 75251 1270 T 972 450.4600 www.nexeninc.com

October 21, 2005

U.S. Department of the Interior Minerals Management Service 1201 Elmwood Park Blvd. New Orleans, LA 70123-2394

Attn: Mr. Alex Alvarado

RE: ATP Oil & Gas Corporation Lease OCS-G-14016, Mississippi Canyon Block 711 Nexen Petroleum U.S.A. Inc. Lease OCS-G-24105 Mississippi Canyon Block 755

Dear Mr. Alvarado:

In letter dated May 23, 2005, from Mickey W. Shaw with ATP Oil & Gas Corporation (ATP), it was requested that Nexen Petroleum U.S.A. Inc. ("Nexen") concur with ATP's proposal for installation of the a 6.895-inch OD bulk oil pipeline and associated umbilical originating at Subsea well No. 006 located on ATP's Lease OCS-G-14016, Mississippi Canyon Block 711. The proposed routing comes into close proximity of the existing Nexen Well No. 2 in Mississippi Canyon Block 755 Lease OCS-G-24105. ATP also sent a proposal letter dated May 9, 2005 in which Right-of-Use and Easement covering proposed anchor placement was presented.

Additionally, Nexen has submitted in their Revised Exploration Plan to drill MC 755 Well No. 3, a proposed mooring arrangement for the "GSF Arctic I" which poses potential conflicts associated with the ATP flowline and umbilical installation proposal. In letters dated June 2, 2005 and June 20, 2005, signed by Larry McRae of Nexen, it was requested that the MMS not approve ATP's proposed plans until both companies could discuss these conflicts.

After extensive discussions and negotiations between Nexen and ATP, both parties have agreed to a resolution of the mooring conflicts associated with development of resources on the two leases.

Please let this letter serve as Nexen's Letter of No Objection to ATP's mooring and subsea equipment installation in MC 755 and MC 711 as agreed by both parties in the letter agreement dated October 14, 2005.



If you should need further information on the activities subject to this waiver letter, please feel free to contact me at 972-450-4757.

Very truly yours,

NEXEN PETROLEUM U.S.A. INC.

Larry D. McRae Vice President - Operations

LDM:mcp

cc: MMS: Nick Wetzel, Plans Unit

ATP/M. Shaw

ATP/Robert M. Shivers

L. Bohot

R. Sommer

M. Patton

B. Bagley

C. Gill

J.: Connor Consulting, Inc. - Ms. Sharon DeSimoni

SCANNED

AMENDMENT

JUN 2 1 2005



NEXEN PETROLEUM U.S.A. INC.

12790 Merit Drive Suite 800 Dallas Texas 75251 1270 † 972 450.4600 www.nexeninc.com

June 20, 2005

J. Connor Consulting, Inc.Attn: Ms. Sharon DeSimoni16225 Park Ten Place, Suite 700Houston, TX 77084

RE: ATP Oil & Gas Proposal Letter dated May 23, 2005

Dear Sharon:

This letter is a formal response to a proposal letter dated May 23, 2005, from Mickey W. Shaw with ATP Oil & Gas Corporation in which he requested Nexen Petroleum U.S.A. Inc. concur with ATP's proposal for installation of the a 6.895-inch OD bulk oil pipeline and associated umbilical originating at Subsea well No. 006 located on ATP's Lease OCS-G-14016, Mississippi Canyon Block 711. The proposed routing loops onto the northern section of Nexen Petroleum U.S.A. Inc. Mississippi Canyon Block 755 Lease OCS-G-24105 and comes into close proximity of the existing Well No. 2. After careful consideration of all of the issues surrounding this proposal, we regretfully inform you that Nexen will strongly oppose ATP's proposed application as it currently exists.

Nexen Petroleum cannot concur with the flowline routing due to the lack of resolution surrounding the previous ATP Oil and Gas proposal letter dated May 9, 2005 in which Right-of-Use and Easement covering proposed anchor placement was discussed and rejected due to considerable mooring conflicts. Nexen has considerable concerns associated with the flowline placement severely limiting the options for the mooring conflict resolution. Nexen Petroleum would prefer a north routing for the proposed bulk flowline to limit the effects to ongoing mooring analysis surrounding future re-entry of the Mississippi Canyon 755 Well No.2. The proposed ATP bulk flowline and umbilical increases hardship and financial burden on Nexen's future operations due to the need to install a preset mooring system and potential use of highbred mooring systems to accommodate the associated risk of the close proximity of the drilling and FOI mooring systems. The additional commercial burden and associated risk are currently being



evaluated and it is our intent to work towards a win-win solution for both parties. This will require considerable effort and cooperation from both parties and will include reduction of safe zones and careful SIMOPs planning. We have included a proposed mooring arrangement for the "GSF Arctic I" which illustrates the potential conflicts associated with the flowline and umbilical installation.

We hope that this detail will help you to understand why we cannot assent to your proposed application and we welcome the opportunity to meet with you at a future date to discuss alternatives and solutions.

Very truly yours,

NEXEN PETROLEUM U.S.A. INC.

Larry D. McRae V.P. Operations

LDM/bj

Enclosures

cc: Minerals Management Service

Attn: Mr. Nick Wetzel, Plans Unit

ATP / Attn: M. Shaw

L. Bohot

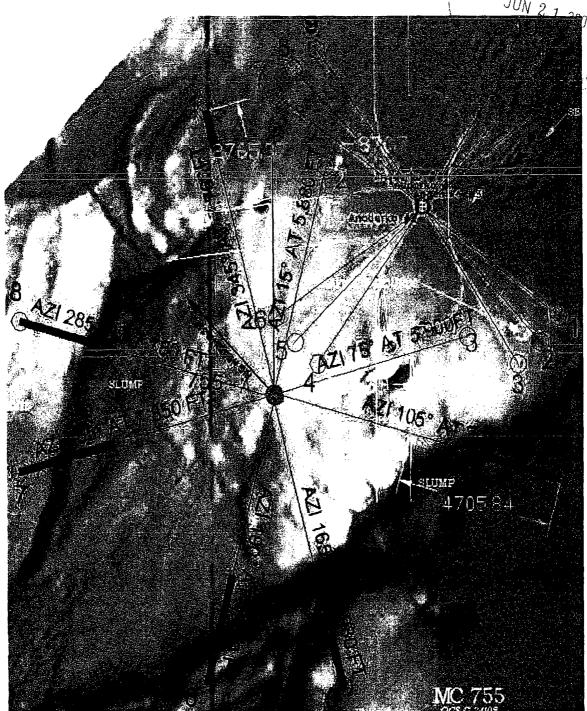
R. Sommer

M. Patton

B. Bagley

C. Gill

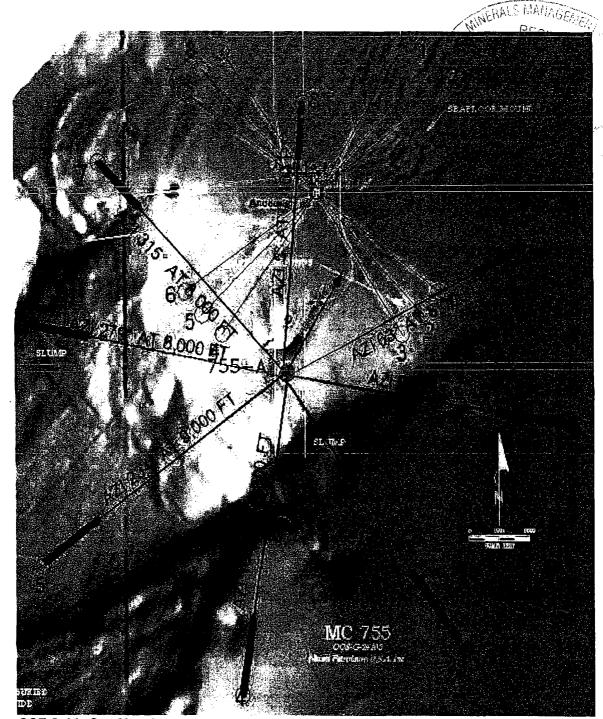
B. Whitney



GSF Arctic I Mooring Pattern

This system has been designed using single line catenary analysis, and no mooring analysis has been completed. Prior to final approval, a mooring analysis should be carried out to verify the feasibility of this system.

The following figure depicts the As-Installed mooring pattern for the *GSF Celtic Sea* when it was previously located on MC 755 January of 2005



GSF Celtic Sea Mooring Pattern

If you have any questions or comments, please feel free to contact us.

Best regards,

David Adam Adair Staff Engineer Delmar

&

Evan Zimmerman, JD Engineering Manager Delmar

Production System Cathodic Protection

Scope

This Document summarizes the Cathodic Protection provided for the MC-711 production system. A thorough overall Cathodic Protection check has been performed on the jumpers, PLETs, flexible risers and end fittings.

General

The production system is composed of the tree connectors (CRA and 4130), the rigid jumpers (Duplex/Sduplex CRA) c/w connectors (CRA and 4130), the PLET connector (CRA and 4130) and pipework (Duplex/SDuplex CRA), the flexible (316 CRA and steel wires) with 4130 end fittings and the interface with topsides pipework.

The Cathodic Protection of the Tree is not addressed in this document, it is in the scope of the tree manufacturer.

From the Tree connectors all the way to the flexible riser end fittings, the protection is provided by the anodes on the PLET as follows:

- To protect the tree connector, the jumper and the connector to the PLET, 30lb of aluminum anode are required (Annex A). The anodes at the PLET are sufficient to provide this mass requirement for protection over 20 years.
- To protect the Production PLET structure, pipework and connectors, 669 lb of aluminum anodes are required (Annex B). The anodes at the PLET structure can provide this mass requirement for protection over 20 years.
- To protect the flexible riser and end fittings, 149 lb of aluminum anode are required (Annex C). The anodes at the PLET are sufficient to provide this mass requirement for protection over 20 years.

The PLET is designed with 10 anodes of 87 lb each for a total aluminum anode mass of 870 lb. From the 870 lb, 30 lb are allocated to protect the tree connector, the jumper and

PLET connector; 669 lb are allocated to protect the PLET structure, pipework and connectors; and 149 lb are allocated to protect the flexible riser and end fittings. The remainder of 22 lb can be retained to cover against any contingency thereafter.

Annex A

GOMEZ PROJECT - PRODUCTION JUMPERS AND CONNECTORS

Cathodic Protection Calculation using DEP 30.10.73.32-Gen

Design Life;

 $T_{design} := 20 \cdot yr$

Coating constants;

 $k_1 := 0.05 \quad k_2 := 0.005$

Inputs

Jumper Details(Including connectors):

Coating Breakdown Factors: FBE

4.5" Jumper Length;

Li := 43rr

Jumper Connectors length:

Lc := 17m

finitial;

 $f_{initial} := 5.\%$

Overall Length; $L_{16pipe} := Lj + Lc$ $L_{16pipe} := 60 \text{ m}$

 $f_{average}$; $f_{average} = k_1 + T_{design} \frac{k_2}{2.yr}$ $f_{average} = 0.1$

4.5" Pipe Diameter;

 $D_{16pipe} := 114.3 \, mn$

f_{final};

 $f_{\text{final}} := k_1 + T_{\text{design}} \cdot \frac{k_2}{vr}$

4.5" Coating Thickness;

 $t_{16coat} := 0.5 \cdot mr$

Current Densities:

Pipe Joint Length;

 $L_{\text{joint}} := 12.2 \text{ m}$

Anode Details: Details of the anodes on the PLET

Initial:

 $C_{initial} := 20 \text{ mA} \cdot \text{m}^{-2}$

Average;

 $C_{average} := 20 \text{ mA} \cdot \text{m}^{-2}$

Anode Length;

 $L_{anode} := 750 \, mr$

Final:

 $C_{\text{final}} := 20 \cdot \text{mA} \cdot \text{m}^{-2}$

Anode Thickness;

 $t_{anode} := 40 \text{ mm}$

 $t_{gap} := 40 \text{-mm}$

Environment and Potentials:

Anode Utilisation;

Anode Gap;

u := 80%

Steel Potential;

 $E_{\text{steel}} := -0.8 \text{ V}$

Anode Temperature;

 $T_{anode} := 10 \cdot C$

Anode Potential;

 $E_{anode} := -1.05 \text{ V}$

4.5" Steel Temperature;

 $T_{16steel} := 70 \, C$

Env. Resistance;

 $R_{env} := 0.3 \cdot \Omega \cdot m$

Anode Material Density;

 $\rho_{\text{anode}} := 2750 \,\text{kg} \cdot \text{m}^{-3}$

Base Anode Efficiency; can use 2500 A-hr/kg because the anodes are cooled on the PLET/tree

 $E_{\text{base}} := 2500 \,\text{A} \cdot \text{hr} \cdot \text{kg}^{-1}$

Calculation of Current Demand

Lengths and Areas

$$L_{16pipe} = 60 \text{ m}$$

$$A_{16protect} := \pi \cdot D_{16pipe} \cdot L_{16pipe}$$

$$A_{16\text{protect}} = 21.545 \,\text{m}^2$$

Increase in Current Demand due to Temperature:

$$i := 1 \cdot mA \cdot m^{-2} \cdot C^{-1}$$

$$T_{ref} := 25 \cdot C$$

$$\begin{split} I_{16initial} &:= \begin{bmatrix} C_{initial} & \text{if } T_{16steel} < 25 \cdot C \\ \\ C_{initial} + i \cdot \left(T_{16steel} - T_{ref} \right) & \text{if } T_{16steel} > 25 \cdot C \end{bmatrix} \\ I_{16initial} &= 65 \, \text{mA} \cdot \text{m}^{-2} \end{split}$$

$$I_{16initial} = 65 \text{ mA} \cdot \text{m}^{-2}$$

Current Demands

4.5" jumper and connectors

$$I_{16init} = 0.07 A$$

$$I_{16avg} = 0.14 A$$

$$I_{16 \text{final}} = 0.21 \text{ A}$$

$$T_{refl} := 20 \cdot C$$

Anode Mass and Requirements

$$Corr := 27 \cdot A \cdot hr \cdot kg^{-1} \cdot C^{-1}$$

$$\begin{split} E &:= \begin{bmatrix} E_{base} & \text{if } T_{anode} < 20 \cdot C \\ E_{base} - Corr \cdot \left(T_{anode} - T_{refl} \right) & \text{if } T_{anode} > 20 \cdot C \end{bmatrix} \end{split}$$

$$E = 2500 \,\mathrm{kg}^{-1} \cdot \mathrm{A} \,\mathrm{hr}$$

Total Anode Mass Required, based upon average current;

$$M_{req} := \frac{I_{16avg} T_{design}}{F_{cu}}$$

$$M_{req} = 12.276kg$$

From the calculations, it is evident that 27 lb total anode material is needed to provide Cathodic Protection for the jumper and the connectors.

Annex B

PEGASUS INTERNATIONAL, INC. OFFSHORE STRUCTURE CATHODIC PROTECTION DESIGN

CLIENT:

Bluewater Industries

PROJECT:

"MC 711 - 4"" Production Plets - PLET"

JOB NUMBER:

116-6865

ENGINEER: Matias Wilson

GULF OF MEXICO DESIGN CRITERIA:

Current Density:

above mudline:

(Cs) 0.006 Amp/Ft.^2

below mudline:

0.002 Amp/Ft.^2 (Cp)

Utilization Factor:

0.900 (U)

Life Expectancy:

(T) 20 Yrs.

Energy Capabilities:

1100 Amp-Hr./Lb. (Ec)

Surface Area:

above mudline:

(As) 552.00 Ft.^2

below mudline:

(Ap) 0.00 Ft.^2

Weight of Single Anode:

87 Lb. (W)

RESULTS:

Combined Current

(CC) 3.08 Amp CC=(Cs)(As)+(Cp)(Ap)

Total Weight Required:

(Wt) 545.47 Lb.

Wt = CC(8766)(T)/[(Ec)(U)]

NUMBER OF ANODES REQUIRED:

(N) 7 N=(Wt/W)

References:

"NACE Standard RP0176-83, Item No. 53036"

PEGASUS INTERNATIONAL, INC. OFFSHORE STRUCTURE CATHODIC PROTECTION DESIGN

CLIENT:

Bluewater Industries

PROJECT:

"MC 711 - 4"" Production Plets - YOKE"

JOB NUMBER:

116-6865

ENGINEER: Matias Wilson

GULF OF MEXICO DESIGN CRITERIA:

Current Density:

above mudline:

(Cs) 0.006 Amp/Ft.^2

below mudline:

(Cp) 0.002 Amp/Ft.^2

Utilization Factor:

0.900 (U)

Life Expectancy:

(T) 20 Yrs.

Energy Capabilities:

1100 Amp-Hr./Lb. (Ec)

Surface Area:

above mudline:

125.00 Ft.^2 (As)

below mudline:

0.00 Ft.^2 (Ap)

Weight of Single Anode:

(W) 87

Lb.

RESULTS:

Combined Current

(CC) 0.70 Amp CC=(Cs)(As)+(Cp)(Ap)

Total Weight Required:

(Wt) 123.52 Lb.

Wt = CC(8766)(T)/[(Ec)(U)]

NUMBER OF ANODES REQUIRED:

(N) 2 N=(Wt/W)

References:

"NACE Standard RP0176-83, Item No. 53036"

Annex C

PEGASUS INTERNATIONAL, INC. FLOWLINE CATHODIC PROTECTION DESIGN

CLIENT:

Bluewater Industries

PROJECT:

"MC 711 - 4"" Production Flexible Risers"

JOB NUMBER:

116-6190

ENGINEER:

Ernesto Forero

GULF OF MEXICO DESIGN CRITERIA:

(tf)	20	Yrs.
(D)	9.76	in
	247.90	mm
(tcor)	0.168	in
	4.27	mm
(Ltot)	8711	ft
	2655.11	m
(Ac)	22258	ft^2
	2067.84	m^2
ity: (icm)	0.060	A/m^2
;		
(fcm)	0.007	
(fcf)	0.009	
(W)	87	Lb.
(u)	0.9	
(Icm)	0.87	Amp
(Mb)	68	kg
	149.09	lb
	(D) (tcor) (Ltot) (Ac) ty: (icm) : (fcm) (fcf) (W) (u) (Icm)	(D) 9.76 247.90 (tcor) 0.168 4.27 (Ltot) 8711 2655.11 (Ac) 22258 2067.84 (ty: (icm) 0.060 : (fcm) 0.007 (fcf) 0.009 (W) 87 (u) 0.9 (Icm) 0.87 (Mb) 68

NUMBER OF ANODES REQUIRED:

(N) 1.7

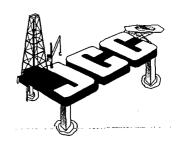
References:

Reference 1. DNV-RP-F103 OCTOBER 2003

Reference 2. ISO 15589-2 2004

BEST AVAILABLE COPY

J. Connor Consulting, Inc.



DOCUMENT TRANSMITTAL

DATE:

November 17, 2005

TIME:

3:55 pm

Attention:	From:
Bimal Shrestha	Sharon DeSimoni
Company Name:	
Minerals Management Service	
1201 Elmwood Park	
New Orleans, Louisiana 70123-2394	

Bimal,

Enclosed please find the certified plats for ATP Oil & Gas Corporation's proposed flowline and umbilical Segment No.'s 15168, 15169, 15170, & 15171 to be located in MC 711.

I think that I sent you everything that you needed except for the Corrosion Inhibition Program and I am still waiting for that. I will forward to you upon receipt

Please let me know if you need additional information. Thanks

From the desk of:

Sharon DeSimoni Regulatory Consultant J. Connor Consulting, Inc. Telephone: 281-578-3388

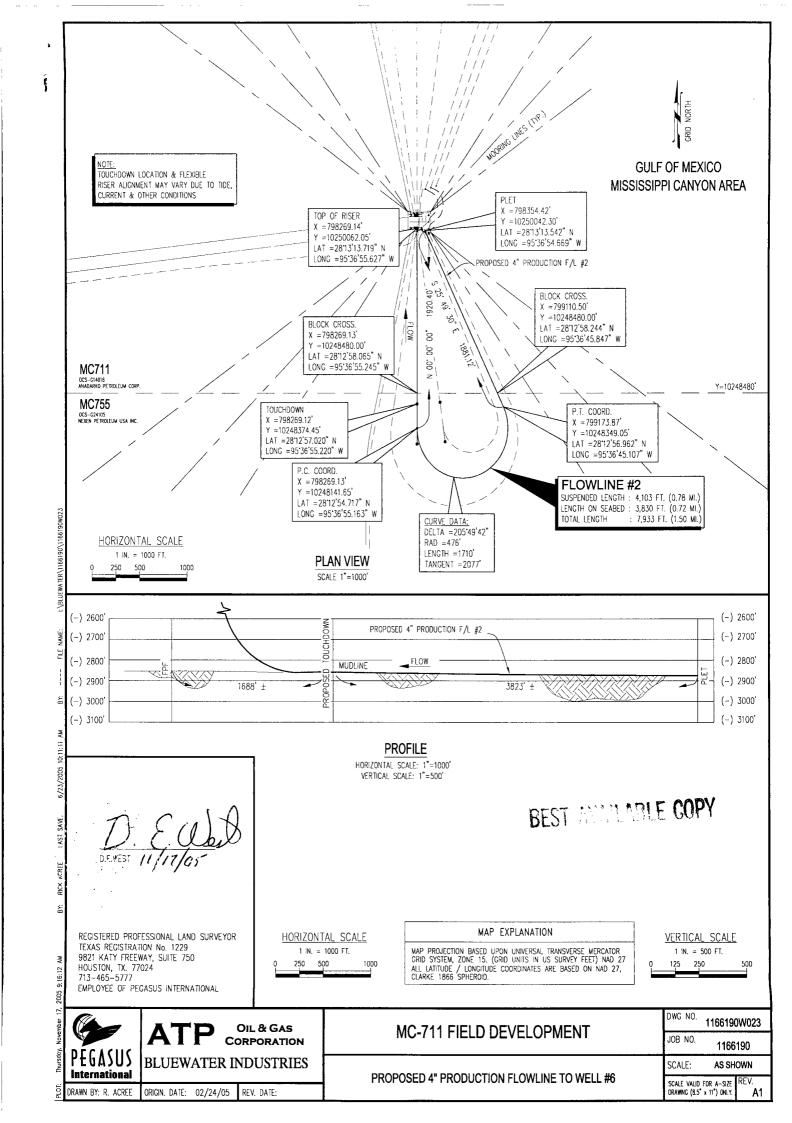
Fax: 281-578-8895

E-mail: Sharon.desimoni@jccteam.com

Minerals Management Service
RECEIVED

NOV 1 8 2005

Office of Field Operations
Pipeline Section



Shrestha, Bimal

From:

Sharon DeSimoni [Sharon.DeSimoni@jccteam.com]

Sent:

Thursday, November 17, 2005 11:11 AM

To:

Shrestha, Bimal

Subject:

FW: UMBILICALS: More Questions From MMS

Attachments: CSP-1135-B1 rev B - umbilical cross section.pdf

Bimal,

The emails below came from Pegasus regarding the gas lift line and the lengths of the umbilicals.

I am working on the remainder of the information.

Sharon

----Original Message----

From: John Hines [mailto:jhines@Pegasus-International.com]

Sent: Thursday, November 17, 2005 11:08 AM

To: Sharon DeSimoni

Cc: Robert Shivers (rshivers@atpog.com); Phillip Shin; Carlos Pernalete; Don Ross; Gary Ford; Norman

Subject: RE: UMBILICALS: More Questions From MMS

Sharon,

The umbilicals are bundled:

They comprise a 1.75" ID gas lift line at the center, surrounded by 10 x 0.5" ID hydraulic lines with a nominal bundled OD of 4.04".

I have attached the manufacturer's cross section for information.

The umbilical lengths are as follows:

Umbilical number 1, total length 6,879ft comprising 2,567ft on seabed and 4,312ft suspended
Umbilical number 2, total length 7,576ft comprising 3,264ft on seabed and 4,312ft suspended
Regards
John Hines
Pergesus International Lea

Pegasus International Inc

777 North Eldridge Parkway, Suite 300

Houston Texas 77079

Direct:713-463-4939 Main:713-465-5777

----Original Message----

From: Sharon DeSimoni [mailto:Sharon.DeSimoni@jccteam.com]

Sent: Thursday, November 17, 2005 10:47 AM

To: John Hines

Subject: RE: FLYING LEADS RE: More Questions From MMS

John.

What about the length of the umbilicals - each one and are they bundled?

Sharon

-----Original Message-----

From: John Hines [mailto:jhines@Pegasus-International.com]

Sent: Thursday, November 17, 2005 10:35 AM

To: Sharon DeSimoni

Cc: Robert Shivers (rshivers@atpog.com); Phillip Shin; Carlos Pernalete; Don Ross; Gary Ford; Norman

Driskill

Subject: FLYING LEADS RE: More Questions From MMS

Sharon,

The gas lift and hydraulic flying leads will be installed during this phase.

The gas lift flying lead is a single tube of 1.25" ID.

The hydraulic flying lead is a bundle of 0.5" ID hydraulic tubes

There are two gas lift flying leads, one nominally 400ft and the other nominally 500ft

Similarly there are two hydraulic flying leads, one nominally 400ft and the other nominally 500ft

Regards J Hines

John Hines Pegasus International Inc 777 North Eldridge Parkway, Suite 300 Houston Texas 77079

Direct:713-463-4939 Main:713-465-5777 -----Original Message-----

From: Sharon DeSimoni [mailto:Sharon.DeSimoni@jccteam.com]

Sent: Thursday, November 17, 2005 9:22 AM

To: John Hines

Subject: More Questions From MMS

John,

The additional questions this morning...

On Drawing No, 1166190W025 - Subsea Infield Layout - there are gas lift lines shown. Will those be installed during this phase? They have not been discussed at all in the applications. And second, Bimal needs the length of each umbilical - and to know if they will be bundled. If I remember correctly - they will not be bundled. Please confirm.

Thanks for your assistance. Sharon

Sharon DeSimoni
J.Connor Consulting, Inc.
16225 Park Ten Place, Suite 700
Houston, Texas 77084
281-578-3388

API 1111

Internal Pressure (Burst) Design

The following formulas were used in determining the wall thickness with respect to internal pressure design:

$$P_{t} \le f_{d} f_{e} f_{t} P_{b}$$

$$P_{d} \le 0.80 P_{t}$$

$$P_{d} \le 0.90 P_{t}$$

where:

 f_d = internal pressure design factor (0.90 for pipelines, 0.75 for risers)

 f_e = weld joint factor (only materials with a factor of 1.0 are acceptable)

 f_t = temperature de-rating factor as specified in ASME B31.8

P_a = incidental overpressure (internal minus external pressure)

 P_b = specified minimum burst pressure of pipe

 P_d = pipeline design pressure

 P_t = hydrostatic test pressure (internal minus external pressure)

$$P_b = 0.45(S + U) \ln \left(\frac{D}{D_i}\right)$$

where:

D = outside diameter of pipe

 $D_i = D-2t = inside diameter of pipe$

S = specified minimum yield strength (SMYS) of pipe

U = specified minimum ultimate tensile strength of pipe

t = nominal wall thickness of pipe

ln = natural log

Collapse Due to External Pressure

$$(P_o - P_i) \le f_o P_c$$

where:

 f_o = collapse factor (0.7 for seamless or ERW pipe, 0.6 for cold expanded pipe) P_c = collapse pressure of pipe

$$P_{c} = \frac{P_{y}P_{e}}{\sqrt{P_{y}^{2} + P_{e}^{2}}}$$

$$P_{y} = 2S\left(\frac{t}{D}\right)$$

$$P_{e} = 2E\frac{\left(\frac{t}{D}\right)^{3}}{\left(1 - \upsilon^{2}\right)}$$

where:

E = modulus of elasticity

 P_e = elastic collapse pressure of the pipe

 P_y = yield pressure at collapse

v = Poisson's ratio (0.3 for steel)

ASME B31.8

Hoop stress : Sh = (Pi-Pe)*(D/2t)

Pi = internal pressure

Pe = external pressure

D = nominal outside diameter of pipe

t = wall thickness

ASME B31.4

Hoop stress : Sh = (Pi-Pe)*(D/2t)

Pi = internal pressure

Pe = external pressure

D = nominal outside diameter of pipe

t = wall thickness

ASME B31.3

Not applicable for this case

B31.8 Ch. VIII

B31.3 Normal Pressure

B31.3 High Pressure

Wall Thickness Requirements
Note: Highlighted Cells are User input cells

Pipe Outside Diameter (D) (in)	= 4.500
Internal Design Pressure (P) (psi)	= 7500
Corrosion Allowance (CA) (in)	= 0.000
Design Water Depth (WD) (ft)	= 3000
SMYS (Sy) (psi)	= 80000
Specified Minimum Ultimate Tensile Strength (U) (psi)	= 109000
Modulus of Elasticity (E) (psi)	= 29000000
Poisson's Ratio (v)	= 0.3
Mil Tolerance	= 12.5%
Allowable Tensile Stress at Temperature (for B31.3 Calculations) (psi)	= 36220
Design Wall Thickness (in)	= 0.674
Actual Wall Thickness (less corrosion) (in) =	= 0.674
Complies with Code?	
API 1111	OK
B31.4 Ch. IX	ок

ΟK

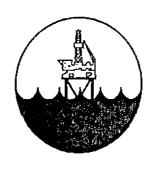
ОК

OK

<u>API 1111</u>

Hydrostatic Test Pressure (Pt) (psi)	11250
INTERNAL BURST	
fd (0.75 for pipeline risers; 0.90 for pipelines) = fe = ft (see ASME B31.8; 1.0 for T < 250 deg F) = Pt = Pd =	0.9 1.0 1.0 11250 7500
Pi = External Pressure (P_o) (psi) = Inside Diameter of Pipe (Di) (in) = Incidental Overpressure (Pa = Pi-Po) (psi) =	7500 1333.33 3.152 6166.67
Specified Minimum Burst Pressure (Pb = 0.45(Sy+U)ln(D/Di)) fd*fe*ft*Pb	30281.22 27253.10
Check: $P_t \le f_d f_e f_t P_b$? Check: $P_d \le 0.80 P_t$? Check: $P_a \le 0.90 P_t$?	ок ок ок
EXTERNAL COLLAPSE	
$(P_o-P_i) \le f_oP_c$	
f_o (0.7 for seamless or ERW; 0.6 for cold expanded pipe such as DSAW) = External Pressure (P_o) (psi) =	0.7 1333.33
Yield Pressure at Collapse (Py) (psi) = Elastic Collapse Pressure (Pe) (psi) = Collapse Pressure of Pipe (Pc) (psi) =	23964.44 214155.26 23815.80
$P_o-P_i =$	1333.33
Check: $P_o-P_i \le f_oP_c$?	ОК
B31.4 Ch. IX (t used in calcs is NOT decreased by mil tolerance)	
Hoop Stress Design Factor (F) (0.72 for Pipeline; 0.6 for Riser and Platform Piping) =	â0 72
Internal Pressure (Pi) = External Pressure (Pe) =	7500 1333.33
Pi-Pe =	6166.67

Hoop Stress (S _h) =	20586.05
Check S _h <= F*Sy	ОК
B31.8 Ch. VIII (t used in calcs is decreased by mil tolerance)	
Hoop Stress Design Factor (F) (0.72 for Pipeline; 0.5 for Riser and Platform Piping) = Temperature Derating Factor (T) (from Table 841.116A; 1.00 for Temp <= 250 deg F) =	0.72 (2) (4) (1.00
Internal Pressure (Pi) = External Pressure (Pe) =	7500 1333.33
Hoop Stress (S _h) =	23526.92
Check S _h <= F*Sy	ОК
B31.3 - Normal Pressure (Ch. II) (note: this calc includes external pressure to help against internal overpressure)	
tm =	0.58975
Coefficient (Y) = Quality Factor (E1) (=1.00 for API 5L seamless pipe) =	0.4 1.00
tcalc =	0.3538
Check tm >= tcalc	ОК
B31.3 - High Pressure (Ch. IX) (note: this calc includes external pressure to help against internal overpressure)	
tm =	0.58975
tcalc =	0.4017
Check tm >= tcalc	ОК



BLUEWATER INDUSTRIES

MC-711 FIELD DEVELOPMENT

PHASE 1 RIGID JUMPER AND PRODUCTION PLET PIPEWORK DESIGN REPORT



					-		
A	Issued for Comment	8/25/05	P. Fry	O. Mauvoisin	N. Driskill		
Rev	Description	Date	Originator	Checker	Project Approval	Pegasus Approval	Client Approva

DOCUMENT NO.: 1166-190-TR-364

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1.0 INTRODUCTION

1.1 Project Description

ATP Oil & Gas Corporation (ATP) is developing the MC-711 field in Mississippi Canyon located in the Gulf of Mexico.

The development will comprise up to four wells tied-back to a converted drill rig semi-submersible floating production facility (FPF).

Two export lines are required, one oil export line and one gas export line, using dynamic flexible risers and rigid pipeline. Provision for a future third-party tie-in to the FPF is to be made.

All subsea well tiebacks to the FPF are provided using flexible flowlines. The subsea well controls will be provided by using direct hydraulic, closed loop, systems via individual dynamic umbilicals.

The FPF topsides process facilities for the oil and gas production from the subsea wells will be provided in the form of pre-fabricated pancakes or modules which are independent to the existing rig facilities.

Pegasus-International Inc has been contracted to undertake the subsea, controls, pipelines and topsides design engineering for the project. Excluded from the scope of work is the conversion design of drilling rig semi-submersible and its mooring system.

1.2 Scope

This rigid jumper and PLET pipework design report, prepared by Pegasus International, Inc., details the engineering work performed and technical basis for the design of the two proposed Phase 1 4-inch rigid jumpers connecting well 1 and well 2 to their respective PLETs. The overall field layout, shown on Drawing No. 1166190F004 (Ref. 2), illustrates the location of the proposed wells and PLETs.

The remainder of this report is arranged as follows:

- Section Two presents the basis for the design
- Section Three presents the method of analysis
- Section Four contains the computer model description
- Section Five contains the output for PLET design
- Section Six contains the output for jumper design
- Section Seven contains a demonstration of compliance with serviceability limits of the connectors

1.3 Summary

From the analysis of the jumpers for various lengths, it was found that the M-shaped jumpers presented in section 4 of this report are able to pass the code check for both oil and gas production for tree movements ranging of +/- 24". Since the M-shape jumper requires more pipe and bends, it is more expensive than a simple U-shaped jumper. If it can be shown that the maximum amount of displacement that the jumper will see is less than or equal to +/- 5" and the length of the jumper is 30 ft or less, than the 30 ft simple U-shaped jumper can be utilized as a more economical solution.

From the analysis of the jumpers for stress considerations as well as VIV considerations, it was found that the jumper dimensions provided in this report are adequate for the design criteria.

From the flow assurance data available, it was found that there was no significant slugging observed under any conditions of varying flowrate and reservoir pressure for either oil or gas production and therefore no stress analysis was performed for slug presence. The "Production Jumpers" drawing (Ref. 12) presents the design details and the seabed layout for the jumpers.

2.0 DESIGN BASIS

2.1 Introduction

The overall design premise is presented in Document No: 1166-190-TR-300 (Ref. 1). This section presents the design data to be utilized during the design of the Phase 1 rigid jumpers connecting the wells to their respective PLETs.

2.2 Design Codes and Standards

The general acceptance criteria for the design of the jumpers is as given in the following codes and standards:

- ASME B31.4 Pipeline Transportation Systems for Liquid Hydrocarbons and Other Liquids (Ref. 9)
- ASME B31.8 Gas Transmission and Distribution Piping Systems (Ref. 8)
- DnV-RP-F105 Free Spanning Pipelines (Ref. 10)
- DnV-RP-C203 Fatigue Strength Analysis of Offshore Steel Structures (Ref. 11)

All wells and jumpers are considered to be subject to both oil and gas production and therefore all of the jumpers will comply with all of the above codes.

For other project codes, regulations and standards, refer to the Design Premise, Pegasus document number 1166-190-TR-300 (Ref. 1).

2.3 Mechanical Data

The generic material properties summarized in Table 2.1 are established values within the industry for rigid pipelines. Due to the highly corrosive nature of the produced fluid, carbon steel will not be considered for the rigid jumper material (Ref. 3).

4-inch Rigid Jumpers #1 and #2

•	Outside Diameter:	4.5 inch
٠	Corrosion allowance:	0.000 inch (corrosion resistant material)
•	Wall thickness:	0.674 inch
•	FBE Coating:	18 mils

PLET Pipc

•	Outside Diameter:	4.5 inch
•	Corrosion allowance:	0.000 inch (corrosion resistant material)
•	Wall thickness:	0.531 inch
•	FBE Coating:	18 mils

Table 2.1 below, presents the properties of the Duplex steel.

Table 2.1 - Duplex Steel Properties

Property	Super Duplex (UNS 32740/50/60)	
0.15	7790kg/m³	
Steel Density	486.3lb/ft³	
Young's Modulus	200 x 10 ³ MPa	
of Elasticity	29 x 10³ksi	
Poisson's Ratio	0.3	
	13.0 x 10 ⁻⁶ /°C	
Coefficient of Linear Expansion	7.2 x 10 ⁻⁶ /°F	
	16.0 W/m.K	
Steel Thermal Conductivity	9.24Btu/ft.hr.°F	
	550MPa	
Yield Strength	79.8ksi	
Yield Strongth	480MPa	
(at 100°C)	69.6ksi	

2.4 Environmental Data

Wave and current data for the proposed pipelines for the MC-711 field in the Gulf of Mexico is provided by A.H. Glenn and Associates (Ref. 5). The data presented in this section is a summary of the environmental data which will govern the design of the rigid jumpers. Refer to the Design Premise (Ref. 1) for complete listings of the environmental data.

•	Surface Current Velocity	7.8 fVs
•	Current Velocity on Bottom (for static analysis)	1.7 fVs
•	Current Velocity on Bottom (for VIV analysis)	0.4 fVs
٠	Wave Height (Hmax)	74 N
•	Wave Period (Tmax)	14.4 sec
٠	Kinematic Viscosity	$1.63 \times 10^{-5} \text{ft}^2/\text{s}$
٠	Density	64 lb/ft³
٠	Ambient Temperature	39.2 °F

The wave and current are assumed to be perpendicular to the jumpers for the purpose of this analysis. The current velocity on bottom for static analysis is the value presented in the project Design Premise (Ref. 1) for pipeline design is used for stress analysis of the rigid jumpers. The current velocity on bottom for VIV analysis is the 100 year storm eddy ("Loop") current at the jumper depth (Ref. 5) is used for the natural frequency analysis of the jumpers. Note that from the current data in Ref. 5, the current velocity is 0.4 fVs for depths of 70% to 100% of water depth which would incorporate any height of the jumper above the seabed.

2.5 Process Data

The following data is a list of the properties used for the design. The pressures and temperatures can be found in section 5.2 of the Design Premise (Ref. 1).

Oil Production:

Fluid Density = 0.02818 lb/in³
Normal Operating Temperature = 120 F
Ambient Temperature = 39.2 F
MAOP = 7500 psi
Hydrotest Pressure = 9375 psi
Code Check = B31.4 Ch. IX (Ref. 9)

Gas Production:

Fluid Density = 0.00325 lb/in³
Normal Operating Temperature = 110 F
Ambient Temperature = 39.2 F
MAOP = 7500 psi
Hydrotest Pressure = 9375 psi
Code Check = B31.8 Ch. VIII (Ref. 8)

2.6 Jumper Lengths

The exact lengths of the jumpers connecting the PLETs to the wells are not known at this time. Due to the large water depth, the location of the PLETs will vary from the designed location. For this reason, a range of lengths will be designed for. The drawing of the seabed layout at the wells is provided in Pegasus drawing number 1166190F004 (Ref. 2). From this drawing, a nominal jumper length is assumed. The lengths of jumpers designed for are:

Jumper #1 Nominal Length = 90 ft Jumper #2 Nominal Length = 37 ft

2.7 Design Requirements

During analysis of the rigid jumpers, loadings from the flowlines, expansion loads (due to pressure and temperature), well movements during workover, and measurement tolerances must be taken into account. The table below provides the values to be used during analysis:

Table 2.2 - List of Values Assumed for Analysis

Description	Value Assumed
Loading from Flowlines	None
Expansion Loads	Caesar will calculate during analysis
Well Movements during Workover	Analysis run with 20" movement
Measurement Tolerances	+/- 4" inline with the jumper

It is assumed that there is no loading on the jumpers from the flowlines because there is a tether on the flowline which will remove any loading from the risers (Ref. 2). Also, the flowlines are flexible pipe so most of the forces will be transferred to the end with least resistance (the bend end away from the PLET) and the PLET will be able to resist any movement due to the remaining load that it faces from the flowlines.

3.0 METHOD OF ANALYSIS

Caesar II pipe modeling software was used to run the analysis of the jumper design. Due to the various design requirements presented in section 2.7 of this report, many cases had to be run in order to insure that the jumpers complied with the codes.

- Case 1 Nominal position of PLET and well
- Case 2 Well moved 24" towards PLET (this includes the maximum well movement during workover and the measurement tolerance in the same direction)
- Case 3 Well moved 24" away from PLET (this includes the maximum well movement during workover and the measurement tolerance in the same direction)

Due to the fact that each jumper is to be designed for both oil and gas production, each of the three cases presented above were run to check for code compliance containing oil or gas.

Input and output files from the Caesar II analysis are presented in Appendix A.

Due to VIV considerations, an Abaqus model was analyzed and the natural frequency obtained was used in conjunction with DnV-RP-F105 (ref. 10) to obtain a fatigue analysis. The fatigue analysis methodology and results are presented in Appendix B along with the Abaqus files and the fatigue calculation spreadsheet.

4.0 CAESAR II MODEL DESCRIPTION AND GEOMETRY

4.1 Rigid Jumper and PLET Piping

The PLET was assumed to have no clamps on the PLET piping on the Caesar model. The point where the production pipe (flexible) and the PLET pipe connect was modeled as an anchor point on the Caesar model. Also, the PLET was assumed to have a hub support height of 2'-6" above the centerline of the PLET piping. The PLET piping is at 110 deg angle and 103 deg angle from the jumper piping (Ref. 2) for well 1 and well 2 respectively. The PLET piping was assumed to have a length of 10' from the anchor flange at the flowline connection point to the centerline of the vertical portion of the PLET piping.

The Caesar analysis was performed for a hub support as a mix between an anchor and a pin support. The support is modeled as a pin with the following spring rates which were found using a model of the hub support on StruCad (Ref. 13):

```
Kx = Kz = 37.5 kip/in

Ky = 3250 kip/in

Rx = Rz = 5885 ft.kip/rad = 1232551.5 in.lb/deg

Rz = 955 ft.kip/rad = 200014.7 in.lb/deg
```

Each of the jumpers was designed as an M-shaped jumper in order to satisfy the stress check. A simple, U-shaped jumper was also tested for various lengths in order to determine the maximum length that this type of jumper could span without failing the stress check but no length of this type of jumper could pass the stress check with either 12" or 24" of tree displacement. Therefore, the simple U-shaped jumper is not a valid option for our jumpers under the 12" or 24" tree displacement criteria. A simple U-shaped jumper has been analyzed for 30 ft and 63 ft jumper lengths in order to determine the maximum amount of tree displacement that it could handle. Results of each of the M-shape jumpers analyzed as well as the results of the U-shaped jumper are presented in section 6 of this report.

4.2 Hub Modeling

The male and female hubs were modeled into Caesar as rigid elements with applied weights as follows:

```
Male Hub weight = 3'-1.25"

Male Hub weight = 480 lb

Female Hub length = 4'-8.219"

Female Hub weight = 800 lb (assumed)
```

The values presented above are from their respective Oil States drawings (Ref. 6 and Ref. 7). The female hub weight had to be assumed due to that information not being available.

4.3 Load Cases and Loadings

For each of the Caesar models, the following load cases were used for analysis:

```
Case 1 - W+T1+P1+D1 (OPE)
Case 2 - W+T1+P1+D1+WAV1 (OCC)
Case 3 - W+T1+P1+D2+WAV1 (OCC)
Case 4 - W+T1+P1+D3+WAV1 (OCC)
Case 7 - W+P1 (SUS)
```

Case 8 - WW+HP (HYD)

Where:

W = weight (submerged weight of pipe and contents)

T1 = temperature

P1 = pressure

D1 = applied tree displacement of 0"

D2 = applied tree displacement of 24" towards PLET(includes 4" measurement tolerance)

D3 = applied tree displacement of 24" away from PLET (includes 4" measurement tolerance)

WAV1 = environmental loads (acting perpendicular to the piping)

HP = hydrotest pressure

WW = Water weight (pipe filled with water)

For a description of the Cases run, refer to section 3.0 of this report. The temperature, pressure and environmental loads are presented in section 2 of this report.

Each of the load cases presented above were used for the stress check of the jumpers. However, only the middle load cases (OCC) were used to present the output on the hub support since this would be the worst case scenario.

4.4 90 ft Jumper (Jumper #1)

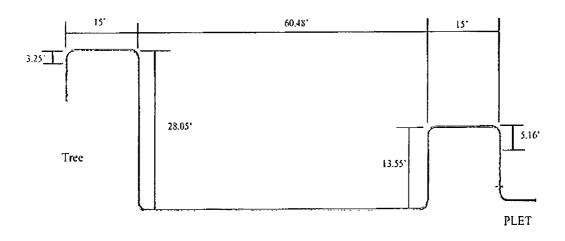
Hub Weights

Male = 480 lb

Female = 800 lb (assumed)

Figure 4.1 below presents the dimensioned Caesar model of the 90 ft rigid jumper. All bends are 5D bends. Note that the middle of the jumper is resting on the seabed.

Figure 4.1 Model of 90 ft Rigid Jumper





Note: The horizontal PLET piping is assumed 10' long in the x-z plane at an angle of 110 deg from the z-axis (Ref. 2).

4.5 37 ft M-shaped Jumper (Jumper #2)

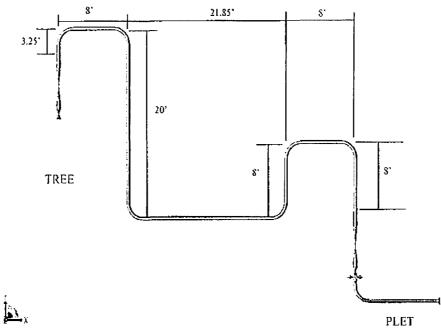
Hub Weights

Male = 480 lb

Female = 800 lb (assumed)

Figure 4.2 below presents the dimensioned Caesar model of the 37 ft rigid jumper. Note that all bends are 5D bends.

Figure 4.2 Model of 37 ft Rigid Jumper



Note: The horizontal PLET piping is assumed 8' long in the x-z plane at an angle of 103 deg from the z-axis (Ref. 2).

4.6 Simple U-shaped Jumper (Option)

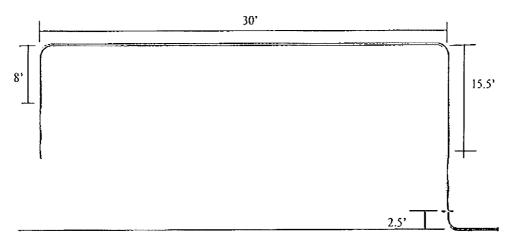
Hub Weights

Mate = 480 lb

Female = 800 lb (assumed)

Figure 4.3 below presents the dimensioned Caesar model of the 30 ft rigid jumper. Note that all bends are 5D bends.

Figure 4.3 Model of 30/63 ft U-Shaped Rigid Jumper





Based on the dimensions provided in Figure 4.3 above, it was found that the simple U-shaped rigid jumper is a viable option for tree displacements up to \pm -5. At \pm -5 of tree displacement, the code stress check resulted in a maximum stress in the 90% range of allowable code stress for the 30 ft and 63 ft options. Increasing the displacement to \pm -6 results in the jumper overstressing.

4.7 Product Vibration

From the flow assurance data available, it was found that there was no significant slugging observed under any conditions of varying flowrate and reservoir pressure for either oil or gas production and therefore no stress analysis was performed for slug presence.

5.0 RESULTS OF ANALYSIS

The 4-inch rigid jumpers were analyzed using the Caesar II pipe modeling software. Based on this analysis, the results for jumper design in order to pass the stress check as well as being available in the restricted time frame are provided in this section.

5.1 Static Analysis Stress Results

From the static analysis, the jumper design passes the stress check for each of the cases run. Tables 5.1 and 5.2 below present the stress results vs. the allowable stress for each of the cases.

Table 5.1 - Stress Results vs. Allowable Stress for 90 Ft. Jumper

	Case	Stress (psi)	Allowable Stress (psi)	% of Allowable
OIL				
	Case 2	41166	58770	70.0%
	Case 3	51144	58770	87.0%
	Case 4	45875	71820	63.9%
GAS				
	Case 2	42786	58770	72.8%
	Case 3	53892	58770	91.7%
	Case 4	47970	71820	66.8%

Table 5.2 - Stress Results vs. Allowable Stress for 37 Ft. Jumper

	Case	Stress (psi)	Allowable Stress (psi)	% of Allowable
OIL				
	Case 2	22819	57456	39.7%
	Case 3	52517	71820	73.1%
	Case 4	56500	71820	78.7%
GAS				
	Case 2	22819	55314	41.3%
•	Case 3	61208	71820	85.2%
	Case 4	61148	71820	85.1%

5.2 90 ft Jumper (Jumper #1) VIV Analysis

For a jumper length greater than 37 th, there is a risk for VIV. For this reason, a fatigue analysis was performed to determine the fatigue life of the jumper. Based on calculations performed in accordance with DnV-RP-F105 (ref. 10), it was found that the fatigue life of the jumpers is greater than the minimum required code life. The calculations are presented in Appendix B.

5.3 37 ft Jumper (Jumper #2) VIV Analysis

As stated in section 5.1, if the distance between the PLET and tree exceeds the 37' length, then the jumper is at risk for VIV. Based on calculations in accordance with DnV-RP-F105, the fatigue life is adequate for this jumper use. The fatigue analysis is provided in Appendix B.

5.4 Demonstration of Compliance with Serviceability Limits

In order for this system to work, it is necessary to ensure that every aspect of the system is able to withstand the forces acting on them. One of the limiting factors in our system are the connectors. Table 5.3 below provides the limits of the connectors (Ref. 4) and Table 5.4 provides the forces and moments that the connector will face from the M-shaped jumper designs.

Table 5.3 - Connector Capacities

Size (in)	OD (in)	ID (in)	Bending Capacity (ft.lb)	Torsion Capacity (ft.lb)	Axial Capacity (lb)
3	4.75	3.06	40,798	19,583	388,289
4	5.75	4.06	65,688	31,530	487,691
6	7.19	5.13	126,702	60,817	747,931

Table 5.4 - Connector Loads

	Size	Bending Moment	Torsion Moment	Axial Force
	(in)	(ft.lb)	(ft.lb)	(lb)
Loads from Analysis	4	21,705	1,283	3,160

The results presented in Table 5.4 are for the worst case of the 90 ft and 37 ft jumpers. Comparing the results in Table 5.4 to the values provided in Table 5.3 for the 4 inch connector, it appears that the connectors for the oil production and gas production piping should be sufficient for this model.

6.0 OUTPUT FOR PLET DESIGN

In order to design the PLET correctly, the forces acting on the hub support must be taken into account. Table 6.0 provides a summary of the loads and moments that the hub support on the PLET is to be designed for (maximum loads from analysis with some conservatism added). The actual forces and moments found from the analysis are given in the tables that follow. Tables 6.1 and 6.2 below present the forces and moments on the hub support for the 90 ft option (Jumper #1), and Tables 6.3 and 6.4 present the forces and moments on the hub support for the 37 ft Jumper #2. Ref. 13 is the PLET structure engineering design report.

The PLET was assumed to have a hub support height of 2'-6" above the centerline of the PLET piping. The PLET piping is at 110 deg angle from the jumper piping (Ref. 2) and has the same pipe properties as the rigid jumper. The PLET piping was assumed to have a length of 10' from the anchor flange at the flowline connection point to the centerline of the vertical portion of the PLET piping. The x, y, and z directions are as seen in Figures 4.1 and 4.2.

Table 6.0 - Summary of Max Loads and Moments for PLET Design

Fx (lb)	-4,500
Fy (lb)	-3,000
Fz (lb)	+2,000
Mx (ft.lb)	-2,000
My (ft.lb)	+1,500
Mz (ft.lb)	-16,000 / ÷18,000

Table 6.1 - 90 ft Oil Jumper Results

	Case 1	Case 2	Case 3
Fx (lb)	-2910	-2680	-3140
Fy (lb)	-2473	-2485	-2460
Fz (lb)	946	1041	\$51
Mx (ft.lb)	-1440	-1573	-1307
My (fl.lb)	927	951	902
Mz (fl.lb)	13291	12969	13612

Table 6.2 - 90 ft Gas Jumper Results

	Case 1	Case 2	Case 3
Fx (lb)	-2616	-2387	-2846
Fy (lb)	-2319	-2332	-2306
Fz (lb)	869	964	774
Mx (ft.lb)	-1296	-1429	-1163
My (fl.lb)	916	941	892
Mz (ft.lb)	12021	11699	12342

Table 6.3 – 37 ft Oil Jumper Results

	Case 1	Case 2	Case 3
Fx (lb)	-2164	104	-4433
Fy (lb)	-1743	-2293	-1194
Fz (lb)	543	586	500
Mx (ft.lb)	-317	-128	-505
My (fl.lb)	183	166	201
Mz (fl.lb)	679	-15779	17136

Table 6.4 - 37 ft Gas Jumper Results

	Case 1	Case 2	Case 3
Fx (lb)	-1947	321	-4216
Fy (lb)	-1662	-2211	-1113
Fz (lb)	497	540	454
Mx (ft.lb)	-241	-52	-429
My (ft.lb)	182	165	200
Mz (fl.lb)	643	-15815	17101

*NOTE: The results provided are based on an assumed female hub weight of 800 lb. All results are for the analysis including wave/current loading, temperature, pressure and the displacement of the tree where applicable.

7.0 CONCLUSION

From the analysis of the jumpers for various lengths, it was found that the M-shaped jumpers presented in section 4 of this report are able to pass the code check for both oil and gas production for tree movements ranging of +/- 24". Since the M-shape jumper requires more pipe and bends, it is more expensive than a simple U-shaped jumper. If it can be shown that the maximum amount of displacement that the jumper will see is less than or equal to +/- 5" and the length of the jumper is 30 ft or less, than the 30 ft simple U-shaped jumper can be utilized as a more economical solution.

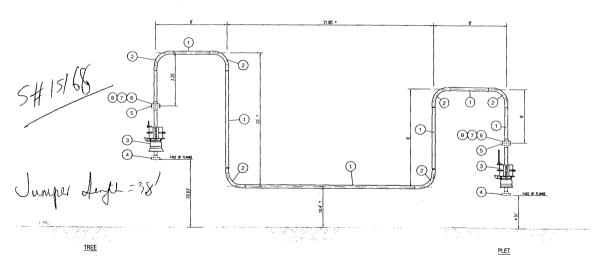
From the analysis of the jumpers for stress considerations as well as VIV considerations, it was found that the jumper dimensions provided in this report are adequate for the design criteria.

From the flow assurance data available, it was found that there was no significant stugging observed under any conditions of varying flowrate and reservoir pressure for either oil or gas production and therefore no stress analysis was performed for stug presence. The "Production Jumpers" drawing (Ref. 12) presents the design details and the scabed layout for the jumpers.

8.0 REFERENCES

- 1 MC-711 Field Development
 "Design Premise"
 Document Number 1166-190-TR-300
- 2 MC-711 Field Development
 "Overall Field Layout at MC-711 Phase 1 Manifold on West Option"
 Drawing Number 1166190F004
- 3 MC-711 Field Development
 "Materials Selection and Corrosion Protection Report"
 Document Number 1166-190-TR-320
- 4 Remote Articulated Connector Table provided by Oil States
- A. H. Glenn and Associates Services
 "Selected Meteorological and Oceanographic Data: Mississippi Canyon Block 711 (3000 Foot Mean Lower Low Water Depth) and Grand Isle Block 115 (350 Foot Mean Lower Low Water Depth): Offshore Louisiana."
- 6 Oil States Drawing
 "4 1/16" 10,000 RAC Male Hub General Arrangement"
 Drawing Number RA041100MHA\GAA0000C
- 7 Oil States Drawing
 "4 1/16" 10,000 Remote Articulated Connector Female Hub Assembly"
 Drawing Number RA041100FHA\GAA0000E
- 8 ASME B31.8
 "Gas Transmission and Distribution Piping Systems"
 2003 Edition
- 9 ASME B31.4
 "Pipeline Transportation Systems for Liquid Hydrocarbons and Other Liquids"
 1998 Edition
- 10 DnV RP-F105
 "Free Spanning Pipelines"
 2002 Edition
- 11 DnV RP-C203
 "Fatigue Strength Analysis of Offshore Steel Structures"
 2001 Edition
- Pegasus Drawing
 "Production Jumpers"
 Drawing No. 1166190N006
- 13 MC-711 Field Development
 "Export PLET Structure Engineering Design Report"
 Document No. 1166-190-TR-367

PRODUCTION JUMPER TYPE 1 - SEABED SUPPORTED



PRODUCTION JUMPER TYPE 2 - UNSUPPORTED SPAN

NOTE: THE DIMENSIONS PROVIDED FOR PRODUCTION JUMPER TYPE 2 ARE THE MADDIUM ALLOWABLE LEHERING FOR AN UNSUPPORTED SPAN. F ANY OF THE DIMENSIONS ARE NOTE-ASED, THEN THE NON FIELD EXTRAORDED DIMENSIONS OF JUMPER TYPE SPOULD BE USED AND THE JUMPER SHOULD BE ORGANIS SUPPORTED.

REVISION DESCRIPTION DRAWN BY: R. ACREE DATE: 03/10/05 O€OŒD BY: PJ.

0 05/16/05 RKA APPROVED FOR CONSTRUCTION

0 07/9/00 RA APPROVED FOR CURSINAL-HUP
20 07/19/00 RA ADDED PPT COATING
AT 02/74/2005 RA SECOND FOR REVER AND COMMENT
SECOND FOR REVER AND COMMENT
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DATE: 04/19/05 APPROVED BY: N.G.D. DATE: 04/21/05 PLOT SCALE: 1=1 SCALE: N.T.S.

ATP OIL & GAS BLUEWATER INDUSTRIES

PEGASUS

International

MC-711 FIELD DEVELOPMENT

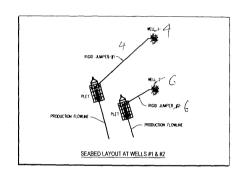
PRODUCTION JUMPERS

OO O 1166190 1166190N006

NOTES: 1. ITEM 4 IS NOT IN THE SCOPE OF WORK FOR THE JUMPERS.
THEY, ARE SHOWN FOR INFORMATION PURPOSES, ONLY. 2. 76FT. ADDITIONAL PIPE TO BE PROCURED FOR FIELD DETERMINED LENGTHS. 3. THE FLANGES ON THE FEMALE HUBS (FREE ISSUE) WILL BE OVERLAID. MITH LINS NO6675. * NOTE: FIELD DETERMINATION OF VALUES.

ITEM QTY.

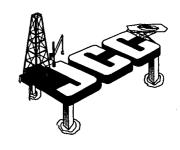
BILL OF MATERIAL - JUMPER SPOOL



BEST AVAILABLE COOK

BS

J. Connor Consulting, Inc.



DOCUMENT TRANSMITTAL

DATE:

June 7, 2005

Attention:	From:
Bimal Shrestha	Sharon DeSimoni
Company Name: Minerals Management Service.	
1201 Elmwood Park Boulevard	
New Orleans, Louisiana 70123-2394	

Bimal,

Enclosed please find eight copies each of the technical specifications and drawing of the RIGID Jumpers for Pipeline Segment No.'s 15168 and 15170.

Please include same in the applications previously submitted.

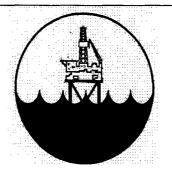
Thanks again for your assistance!

Sharon

From the desk of:

Sharon DeSimoni Regulatory Consultant J. Connor Consulting, Inc. Telephone: 281-578-3388 Fax: 281-578-8895

E-mail: Sharon.desimoni@jccteam.com



BLUEWATER INDUSTRIES

MC-711

SPECIFICATION FOR DUPLEX PIPE



0	Approved for Tender	04/05/05	G .Stevenson	O. Mauvoisin	J. Hines		
Rev	Description	Date	Originator	Checker	Project Approval	Pegasus Approval	Client Approval

DOCUMENT NO.: 1166-190-SN-036

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1.0 INTRODUCTION

1.1 Scope

This specification, when read in conjunction with the contract referenced standards, specifications, and other listed documents, defines the minimum requirements for the application, inspection and testing of duplex or super duplex pipe to specification API 5LC, as modified by this specification.

CONTRACTOR shall be responsible for the manufacture, fabrication, certification, test and delivery of the pipe, as outlined in this specification.

1.2 Abbreviations

Within this document the following abbreviations are used:

API American Petroleum Institute

ASTM American Society for Testing of Materials

AWS American Welding Society

BS British Standards

DPI Dye penetrant inspection

EN Euronorm

EPIC Engineer, procure, install and commission

MPI Magnetic particle inspection

NDE/T Non-destructive examination/testing

NPS Nominal pipe size

PREN Pitting resistance equivalent - nitrogen
PREW Pitting resistance equivalent - tungsten

SMYS Specified minimum yield stress

UNS Unified numbering system

UT Ultrasonic testing

2.0 APPLICABLE CODES AND STANDARDS

2.1 Revisions

Only the latest issues of the relevant standards, codes, statutory regulations and specifications referenced shall be applied to the WORK being performed.

2.2 Compliance

This specification is complementary to the requisition for individual item(s) of equipment, legislative requirements and guidance notes issued by any relevant authority and specifications referenced herein.

2.3 Conflict of Information

If there is any conflict between this specification or any other specification and related data sheets or with any applicable codes, standards and regulations, CONTRACTOR shall inform COMPANY in writing. Written clarification must be given by the COMPANY before CONTRACTOR commences work.

2.4 Project Specifications and Data Sheets

It is the responsibility of the CONTRACTOR to ensure that it has received from the COMPANY all specifications, etc, which are referenced within applicable specifications, to enable it to understand and comply with all aspects of work it is performing for the COMPANY.

2.5 Codes and Standards

It is the responsibility of the CONTRACTOR to ensure that only the latest issues of the following codes, standards and regulations shall be used in conjunction with this specification. Specific reference should be made to the following.

2.5.1 American Petroleum Institute

API 5LC	Specification for	CRA	Line	nine
THIDEO	opeomounon for	Olui		Pipe

2.5.2 British Standards

BS 4515	Specification for	Welding of Steel	Pipelines on I	Land or Offshore

BS 7079/ISO 8503-1 Preparation of Steel Substrate before Application of Paint

BS 7448 Fracture Mechanics Toughness Tests Part 1: Method for Determination of K_{ic} Critical CTOD and Critical J Values of Metallic

Materials

BS 8010 Part 3 Pipelines Subsea: Design, Construction and Installation

BS EN 10204 Metallic Products - Types of Inspection Documents

BS EN ISO 6507 Metallic Materials - Vickers Hardness Test

BS EN ISO 9000 Quality Management and Quality Assurance Standards

2.5.3 American Society for Testing and Materials

ASTM A370 Mechanical Testing of Ferritic Products **ASTM A789** Seamless and Welded Tube and Pipe **ASTM A790** Seamless and Welded Ferritic/Austenitic Stainless Steel Pipe ASTM E165 Test Method for Liquid Penetrant Examination ASTM E562 Practice for Determining Volume Fraction by Systematic Manual Point Count ASTM G48 Standard Test Methods for Pitting and Crevice Corrosion Resistance of Stainless Steels and Related Alloys with the Use of Ferric Chloride Solution 2.5.4 National Association of Corrosion Engineers NACE MR-01-75 Sulphide Stress Cracking Resistant Materials for Oil Field Equipment NACE TM-01-77 Testing of Materials for Resistance to Sulphide Stress Cracking at **Ambient Temperature** 2.5.5 **Euronorms** EN 473 Qualification and Certification of NDT Personnel 2.5.6 **EFC EFC 17** Corrosion Resistant Alloys for Oil and Gas Production - Guidance on General Requirements and Test Methods for H₂S Service

3.0 GENERAL REQUIREMENTS

3.1 General

- 3.1.1 The material shall comply with the requirements of API 5LC, NACE MR-01-75 and NEN 3650, except where modified or supplemented by this specification.
- 3.1.2 Seamless pipe shall be manufactured by hot forming. Solution annealing heat treatment shall be conducted.
- 3.1.3 CONTRACTOR shall provide COMPANY representatives with unhindered inspection access to all work sites and plant used in the execution of the work, both during procedure qualification and during production.

4.0 QUALITY ASSURANCE AND QUALITY CONTROL

4.1 General

- 4.1.1 All certification, test results, reports or any other documentation submitted to the COMPANY shall be in the English language.
- 4.1.2 The CONTRACTOR shall establish and maintain a fully documented APPROVED quality control system, in accordance with the applicable parts of BS EN ISO 9000, to ensure:
 - Adequate, effective inspection and objective evidence that items conform to contract requirements.
 - Adequate identification and suitable handling of items.
- 4.1.3 A quality assurance audit schedule shall be drawn up by CONTRACTOR to cover all aspects of the work.

4.2 Quality Plan

- 4.2.1 CONTRACTOR shall, as part of its tender, submit a written inspection plan which describes the inspection to the performed. The inspection plan shall be re-submitted, with COMPANY comments addressed, prior to commencement of the work for COMPANY APPROVAL. The inspection plan, reference procedure and changes shall be subject to APPROVAL.
- 4.2.2 CONTRACTOR shall also provide COMPANY with an exhaustive list of all works procedures prior to commencement of the WORK and shall provide copies of all procedures subsequently requested by COMPANY within 5 working days of receiving any such request. CONTRACTOR shall also provide COMPANY's INSPECTORS with unhindered access to a full set of work specific and all other works procedures as COMPANY's INSPECTORS see fit to consult.

4.2.3 The inspection plan shall include:

- A flowchart illustrating each inspection point, and its relative location in the procedure cycle, where conformance of characteristics is verified. The CONTRACTOR should include additional inspection points for CONTRACTOR's own verification of quality, which will be subject to APPROVAL.
- The characteristics to be inspected at each inspection point, the procedures, the responsible person and acceptance criteria to be used. The procedures shall be provided to the COMPANY's INSPECTOR as requested.
- Copies of specific forms used by the CONTRACTOR to record the results of each inspection.
- A column for COMPANY to identify its inspection points.

4.3 Special Process Procedures

The CONTRACTOR shall:

- Establish and maintain control of all special processes which are essential to production, inspection or safety. Equipment, processing environment and the CONTRACTOR's personnel shall be subject to appropriate qualifications, with certification, to the satisfaction of the COMPANY's INSPECTOR.
- Establish means to ensure that special processes are accomplished under controlled conditions
 by qualified personnel using APPROVED materials, procedures and equipment as required by
 specifications and THIRD PARTY requirements. APPROVAL shall be obtained prior to
 commencement of the work.
- Establish and maintain documented evidence of control of special processes.

- Establish and maintain documented status of personnel, processes or equipment according to the requirements of pertinent codes and standards.
- Ensure that all measuring and test equipment is calibrated. Records of all such calibrations shall be made available to the COMPANY's INSPECTOR for review and APPROVAL.

4.4 Quality Records

- 4.4.1 The CONTRACTOR shall maintain quality records as documentary evidence of compliance with quality requirements. Quality records shall be available to the COMPANY's INSPECTOR for analysis and review.
- 4.4.2 Quality records may include item identification by reference to drawing and revision number, acceptance criteria, specific inspections performed and results obtained (if measurements are not required, include, in the record, basis of acceptance), date of inspections, identification of inspector, data recorder charts, qualification of material, personnel procedures and equipment.

4.5 Final Inspection

- 4.5.1 The CONTRACTOR shall inspect the final item to ensure compliance with contract requirements. A check shall be made of all inspection records to verify that items were inspected at all points shown in the inspection plan. These records shall be complete and available to the COMPANY'S INSPECTOR.
- 4.5.2 Visual inspection and dimensional checks shall be carried out at the point of discharge or receipt to confirm that no damage has occurred during transportation.

4.6 Verification

- 4.6.1 All CONTRACTOR inspection systems shall be subject to evaluation and surveillance by the COMPANY's INSPECTOR to ensure that the system meets the requirements of this specification and the contract documentation.
- 4.6.2 All CONTRACTOR operations required by this specification are subject to:
 - Procedure compliance checking, at scheduled and unscheduled intervals, to determine that the CONTRACTOR's inspection system is effectively applied.
 - Product verification to determine compliance with control requirements. The method of verification shall be as per the agreed standards and procedures.
 - No items shall be released to COMPANY unless CONTRACTOR has been issued with an
 inspection release note (IRN) by COMPANY's INSPECTOR. A copy of the IRN shall form
 part of the delivery notes accompanying each dispatch of items.

4.7 Preparation for Shipment

- 4.7.1 The CONTRACTOR shall submit to the COMPANY a procedure detailing its method of packing and shipping for all items.
- 4.7.2 CONTRACTOR shall also detail its requirements for short (6 months) and long term storage, including any special maintenance procedures which may be required. CONTRACTOR shall proved APPROVED bevel protectors.
- 4.7.2 No welding of temporary attachments for handling or securing shall be permitted.
- 4.7.3 All handling, loading and unloading shall be performed in accordance with API recommended practices, as appropriate.

5.0 MATERIAL REQUIREMENTS

5.1 General

- 5.1.1 The pipe shall be seamless, as defined by Clause 2.1 of API 5LC, and supplied in the solution annealed and water quenched condition.
- 5.1.2 The finished straight pipe shall be suitable for the production of hot formed bends and, in such cases, shall possess the necessary dimensional and mechanical properties and chemical composition to satisfy these requirements, taking into account any changes that may occur during the bending process.
- 5.1.3 The pipe material shall be suitable for either manual, semi-automatic or automatic welding using inert gas shielded welding processes and conventional electrodes and filler wires. Welded joints shall be capable of meeting the metallurgical and mechanical properties and corrosion resistance as defined in this specification and specification for welding of pipelines, document number 1166-190-SN-038.
- 5.1.4 Pipes shall be solution annealed followed by water quenching. The heat treatment procedure shall be fully qualified as part of the manufacturing procedure, including transfer times from furnace to quenching medium and controls on quench bath.

5.2 Qualification and Manufacturing Trials

- 5.2.1 The CONTRACTOR shall submit for APPROVAL a complete and detailed pipe manufacturing procedure, incorporating all the requirements of this specification. This shall include procedures for steel making, casting, pipe-making, heat treatment, quality control and assurance, testing, pipe tracking and traceability for each manufacturing location. The CONTRACTOR shall also submit previous relevant pre-qualification test results for 22% chromium duplex and/or 25% chromium super duplex stainless steel linepipe produced by the same manufacturing process.
- 5.2.2 A manufacturing procedure specification shall be submitted immediately after award of purchase order and prior to a pre-production meeting prior to production. A manufacturing procedure qualification shall be performed on pipes from the first production run in accordance with Appendix A. After COMPANY acceptance of the manufacturing procedure qualification, no change shall be made to the manufacturing procedure specification and quality plan without written APPROVAL from the COMPANY.

5.3 Material Properties

5.3.1 General

Material properties shall be in accordance with API 5LC LC65-2205 (UNS S31803) or LC65-2506 as applicable and the modifications defined below. The following UNS designations or APPROVED equivalents are acceptable 25Cr alloys: UNS S32740, UNS S32750, UNS S32760 and UNS S39274.

5.3.2 Chemical Composition

- 5.3.2.1 The chemical composition shall be determined for each heat of steel used in the manufacture of linepipe specified on the data sheets. The chemical analysis shall conform to the requirements defined below.
- 5.3.2.2 Product analysis shall be performed for each lot of 50 pipes or once per heat as the minimum frequency as detailed in Table 5.1.

Table 5.1 Product Analysis

Element	Product Weight %		
елешент	25 Cr	22 Cr	
С	0.03 maximum	0.03 maximum	
Si	0.2-0.50	0.3-0.9	
Mn	1.00 maximum	1.8 maximum	
S	0.015 maximum	0.015 maximum	
P	0.03 maximum	0.03 maximum	
Ni	6.0-8.0	5.0-6.0	
Cr	24.0-26.0	21.0-23.0	
Mo	3.0-5.0	2.8-3.5	
N	0.24-0.32	0.14-0.2	
W	2.50 maximum	N/A	
Cu	1.0 maximum	0.20 maximum	
Al	0.03 maximum	0.03 maximum	

- 5.3.2.3 The results of all chemical analyses shall be supplied to the COMPANY as mill material test certificates and these shall include the results of any additional mill control analyses.
- 5.3.2.4 Variations to analysis outside the above limits shall not be permitted.
- 5.3.2.5 The product analysis for 22 Cr duplex shall have a minimum PREN value of 35. The PREN is defined in weight % as follows:

PREN =
$$%Cr + 3.3 \times %Mo + 16 \times %N$$

5.3.2.6 The product analysis for 25 Cr duplex shall have a minimum PREW value of 40. The PREW is defined in weight % as follows:

PREW =
$$%Cr + 3.3 \times %Mo + 1.65 \times %W + 16 \times %N$$

- 5.3.3 Material Condition
- 5.3.3.1 Mechanical testing shall be performed after final heat treatment. If performed prior to hydrotesting, then at least one pipe per size per heat shall be tested before and after hydrotesting. The requirement for repeated testing may, at COMPANY 's discretion and subject to prior written APPROVAL, be waived in favour of testing after heat treatment and prior to hydrotesting, provided the CONTRACTOR can demonstrate that hydrotesting results in no cold working of the finished pipe.
- 5.3.3.2 All mechanical and metallurgical test properties shall be performed on a pipe selected from each lot of 50 pipes or once per heat as the minimum frequency.
- 5.3.4 Tensile Tests
- 5.3.4.1 Longitudinal and transverse room and elevate temperature tests shall be carried out in accordance with Figure 4.1 of API 5LC and ASTM A370. The minimum requirements shall be as follows, in both the longitudinal and transverse directions:

Table 5.2 Tensile Test Requirements

	5-20°C			90°C				
	Minimum		Maximum		Minimum		Maximum	
0.2% Proof	25 Cr	22 Cr						
Stress N/mm ²	550	450	770	630	470	365	650	600
	Minimum		Maximum		Minimum		Maximum	
Tensile Strength	25 Cr	22 Cr						
N/mm ²	800	680	1120	950	700	620	980	800

- 5.3.4.2 The actual yield and ultimate stress values from any tensile test shall not exceed the specified minimum values by more than 40%. CONTRACTOR may offer guaranteed minimum values in excess of those specified.
- 5.3.4.3 Stress/strain curves shall be provided for all qualification tests.

5.3.5 Hardness Tests

Vickers HV10 hardness tests using a 10kg load to BS 427 shall be carried out on longitudinal sections from each pipe selected for tensile testing, in accordance with Clause 4.20 of API 5LC. Hardness surveys shall be made parallel to and 2mm from each surface with 3 impressions at each location. The maximum hardness shall not exceed NACE MR-01-75 requirements, if applicable.

5.3.6 Charpy Impact Tests

Charpy impact testing shall be carried out in accordance with ASTM A370 on specimens, in accordance with Figure 4.1 of API 5LC. The test conditions, orientation of samples and acceptance criteria for each size of pipe and all grades involved are defined in Table 5.3 below.

Table 5.3 Minimum Impact Energies

Nominal Bore	Specimen Size (mm) and Orientation	Test ⁽⁴⁾ Temperature	Minimum Impact Energy (J) ⁽¹⁾		
(inch)	and Orientation	(°C)	Average	Single Value	
≥6	Transverse 10 x 10	T-10	100	80	
< 6	Longitudinal 10 x 10	T-10	100	80	

Note 1: Specimens and test temperatures for bends shall be as per associated pipe.

Note 2: Specimen size for small diameter pipe is the maximum which can be taken from production pipe. The energy requirements shall be factored in accordance with Table 5.4

Note 3: Lateral expansion values shall be reported for all test pieces. The criteria of acceptance shall be 0.38mm minimum lateral expansion value for each test.

Note 4: T = minimum design temperature

Table 5.4 Energy Reduction Factors (ERFs)

Specimen Size	ERF
10 x 10mm	1
10 x 7.5mm	0.83
10 x 5mm	0.67

5.3.7 Metallographic Examination

- 5.3.7.1 Longitudinal and transverse sections shall be prepared for metallographic examination and etched to reveal the microstructure in accordance with ASTM E3 and E407 using APPROVED procedures.
- 5.3.7.2 One production pipe per heat shall be subject to metallographic examination.

The microstructure shall be consistent with that of solution annealed type UNS S31803 or UNS S32740/32750/32760/32974 duplex, as applicable, and free of grain boundary carbides and intermetallic phases, eg sigma, chi, Laves, etc phases.

- 5.3.7.3 Macros shall be handed over to COMPANY for retention.
- 5.3.8 Ferrite Determination
- 5.3.8.1 Ferrite determinations shall be carried out on the metallographic specimens prepared as for Section 6.3.7 using the intercept method in accordance with ASTM E562, except that 30 fields shall be sampled per determination.
- 5.3.8.2 Ferrite levels shall be in the range 35-55%.
- 5.3.8.3 The ferrite lath size shall be taken into account when selecting the field size and magnification.
- 5.3.8.4 Photomacrographs of the areas sampled for ferrite determination shall be produced and included in the reports.
- 5.3.9 Ferric Chloride Test
- 5.3.9.1 A ferric chloride test shall be performed on each procedure qualification and production test pipe, in accordance with ASTM G48, with a test temperature of 35°C for 25 Cr and 25°C for 22 Cr.
- 5.3.9.2 Samples 50mm x 40mm shall be exposed for 24 hours.
- 5.3.9.3 Visual examination aided by a low power microscope shall be carried out after exposure and likely corrosion sites probed with a sharp instrument.
- 5.3.9.4 Acceptance shall be based on no pitting being present on either the internal or external surface of the pipe when viewed with a microscope at 20 times magnification. End and side grain attack may be ignored.
- 5.3.10 Flattening Test

Flattening tests shall be carried out in accordance with Clause 4.13 of API 5LC on each seamless pipe selected for evaluation for procedure qualification and production control.

5.3.11 Re-Tests

In the event of one pipe failing to meet the chemical composition, micro-structural or mechanical property specified acceptance criteria, a re-test on four additional pipes from the same lot of 50 pipes shall be carried out. If these results are all acceptable, then only the pipe which gave the unacceptable results shall be rejected.

6.0 MANUFACTURING REQUIREMENTS

6.1 Hydrostatic Tests

- 6.1.1 Each length of pipe shall be hydrostatically tested in accordance with Section 5 of API 5LC.
- 6.1.2 The pipe shall be hydrostatically tested at a test pressure calculated to produce an outer fibre stress of 95% of the specified minimum yield stress. The test pressure shall be calculated using the following formula:

$$P = \underbrace{2 \sigma_y t_{min}}_{D} x 0.95$$

Where:

= minimum hydrostatic test pressure (N/mm^2)

 σ_y = minimum specified yield stress (N/mm²)

 t_{min} = minimum wall thickness (mm)

D = nominal outside diameter (mm) as per API 5L

6.1.3 The minimum time at test pressure shall be 10 seconds.

6.2 Dimensional Requirements

- 6.2.1 General
- 6.2.1.1 All procedures used for dimensional checks on finished pipe shall be subject to APPROVAL by the COMPANY prior to commencement of pipe production.
- 6.2.1.2 The dimensional checks detailed in Sections 6.2.2, 6.2.3 (pipe ends), 6.2.4 and 6.2.5 shall be carried out on each production pipe.
- 6.2.2 Pipe Length

All pipes shall be supplied in lengths as shown in Table 6.1 below. Jointers shall not be permitted.

Table 6.1 Pipe Lengths

Minimum 95%	Maximum 5%
11.7-12.5m	10.7-11.7m

6.2.3 Diameter and Out-of-Roundness

6.2.3.1 Diameter

Pipe Body: All pipes shall be checked and shall be within $\pm 1.0\%$ of the nominal outside diameter.

Pipe Ends: The ID for a length of 100mm from each end of the pipe shall be within ± 0.8 mm of the nominal internal diameter with.

Nominal ID = nominal OD - 2 x nominal wall thickness

Pipe ends may be machined to achieve these tolerances. Machining shall be to a 1 in 20 taper.

Machining/dressing of pipe ends shall be performed to remove internal lips, burrs, etc that may give false indications on radiographs.

6.2.3.2 Out of Roundness

The out of roundness measured at any point along the pipe length shall be within $\pm 1\%$ of specified nominal outside diameter.

The out of roundness over the length 100mm from each end measured internally shall not exceed $\pm 0.5\%$ of the nominal internal diameter.

6.2.4 Wall Thickness

6.2.4.1 Both ends of each pipe shall be checked for thickness with a limit gauge.

The specified thickness tolerance range shall be met along the whole length of the finished pipe which shall be checked using an ultrasonic method.

6.2.4.2 The tolerances on wall thickness shall be +15%, -12.5% of the specified nominal wall thickness.

6.2.5 Weight

The weight on car load shall not be less than 98.25% of the calculated weight based on nominal wall thickness. Each pipe shall be within +10% and -3.5% of the calculated weight. Each pipe shall be weighed.

6.2.6 Straightness

The deviation from a straight line shall not exceed 1.5mm per metre length over the length of pipe joint.

6.2.7 Pipe Ends

All pipe ends shall be supplied with a machined standard 30° bevel, in accordance with Clause 7.8 of API 5LC.

6.2.8 Gauge Plate

A gauging pig shall be passed through all pipes in the finished supply condition. The gauge shall consist of two parallel 6mm thick stainless steel circular plates each 98% of the minimum pipe ID (pipe minimum ID = minimum OD - 2 x maximum WT) spaced by rigid spacers to give a distance of twice the nominal pipe OD overall. The gauge shall pass through without deforming the plates.

7.0 TESTING AND INSPECTION

7.1 General

- 7.1.1 All procedures proposed for non-destructive testing shall be submitted for APPROVAL.
- 7.1.2 NDE shall be carried out after final heat treatment of the pipe. Where NDE is performed before hydrostatic test, then the first 30 production pipes shall be subject to NDE before and after hydrotest and the results submitted to the COMPANY for review and APPROVAL.

7.2 Personnel

NDE operators shall be qualified to EN 473 level 2 minimum. The supervisor shall be level 3. All operator qualification certificates shall be subject to APPROVAL by the COMPANY prior to commencing pipe production.

7.3 Visual Inspection

The full length of each pipe shall be visually inspected on the external surface for defects and surface finish.

7.4 Ultrasonic Inspection

- 7.4.1 Each length of pipe shall be fully examined in accordance with Section 8.16 (seamless pipe) of API 5LC.
- 7.4.2 The ultrasonic test equipment shall be calibrated using internal and external N5 notches in representative pipe material. Any defect indication in excess of that given by an N5 notch shall be cause for rejection.
- 7.4.3 The wall thickness shall also be checked by a compression probe scan along the whole length of the pipe. The test shall cover at least 25% of the pipe surface.

7.5 Radiographic Inspection

Not required for seamless pipe.

7.6 Dye Penetrant Inspection

- 7.6.1 The end 100m of each pipe and the bevel ends shall be examined by dye penetrant (DP).
- 7.6.2 DP shall be performed in accordance with ASME Section V Article 6 and Appendix 6.
- 7.6.3 Acceptance shall be in accordance with ASME Section VIII Appendix 8.
- 7.6.4 For pipe end bevel faces, indications of 3mm and greater shall be cause for rejection and such pipe shall be cut back and a new end bevel machined.

7.7 Magnetic Particle Inspection

- 7.7.1 The outside surface of the pipe body shall be inspected by fluorescent magnetic particle inspection (MPI).
- 7.7.2 MPI shall be performed in accordance with ASME Section V Article 7.
- 7.7.3 Acceptance shall be in accordance with ASME Section VIII Appendix 8.

7.8 Acceptance Limits

- 7.8.1 The requirements of API 5LC shall apply, together with the following:
 - Any linear discontinuity or any other imperfections having a depth greater than 5% of the specified nominal wall thickness or which, on removal by grinding, cause the wall to be reduced locally below the minimum specified shall be cause for rejection.
 - Surface laps, shells, slivers laminations and all sharp edged imperfections, eg gouges are unacceptable defects (see also Section 7.8.2 of this specification).
 - Laminations in the pipe body exceeding 30mm length or a total area of 500mm² shall be cause for rejection.
- 7.8.2 Bulges, dents and flat areas. Deviations from the original contour of the pipe shall not exceed 3mm depth nor shall they extend in any direction greater than 25% of the pipe outside diameter.

7.9 Workmanship

- 7.9.1 All pipe defect indications shall be assessed in accordance with Section 9 of API 5LC and Section 8.7 of this specification.
- 7.9.2 The entire external surface of each pipe shall be machine ground to St3 of BS 7079, with a surface roughness of:
 - Ra = $60\mu m$ maximum
 - Rz = 80µm maximum
- 7.9.3 Internal finish to be ground or blast finished.

7.10 Repair of Defects

- 7.10.1 Weld repair of seamless pipe shall not be permitted.
- 7.10.2 Surface defects such as laps, slivers, shells may be removed by local grinding to a shallow surface contour, provided that defect removal is confirmed by dye penetrant examination and the wall thickness in the ground area is checked by ultrasonics to show that this has not been reduced below the design minimum.
- 7.10.3 All repairs to be APPROVED by COMPANY. Localised defects in weld bevels may be repaired by re-bevelling or by localised grinding to remove defects up to 3mm in depth, provided ground area is blended to a smooth transition suitable for welding. All repairs are to be subject to repeated NDT and wall thickness checks in the presence of COMPANY.

8.0 DOCUMENTATION

8.1 Documentation to be Provided with Tender

CONTRACTOR shall submit the following with its tender:

- Manufacturing details.
- Quality plan.
- Quality documentation (BS EN ISO 9000 and/or API).
- Packing and marking proposals.
- · Proposed chemical analyses.
- Proposed mechanical properties.
- Any qualifications to this specification.
- Sample pipe tracking report.
- Level 1 schedule.

8.2 Documentation Required Prior to Commencement of WORK

All documents to be presented for APPROVAL prior to commencement of pipe production or production qualification, whichever is earliest:

- Quality plan (including inspection plan).
- Manufacturing procedures.
- NDE procedures.
- Handling procedures.
- Production schedule.
- Pipe tracking procedure.

8.3 Documentation/Certification Requirements on Completion of WORK

The following documentation is required with the supplied pipe:

- APPROVED copies of documents cited in Sections 9.1 and 9.2.
- Unique identification number of each pipe joint.
- Heat, heat treatment/lot (50 pipes) numbers from which the pipe joint originates.
- Length of bevelled pipes.
- Weight of pipe.
- Pipe material certificates according to BS EN 10204 3.2.
- Manufacturing procedure qualification reports.
- Complete statistics of chemical analysis and material properties.

APPENDIX A

MANUFACTURING PROCEDURE QUALIFICATION

A1 General

Prior to production or at CONTRACTOR's risk at the start of production, three pipes in each diameter and wall thickness shall be selected by the COMPANY and tested as follows.

A2 Tensile Tests

One longitudinal specimen shall be taken from each pipe and tested at room temperature and 90°C in accordance with Section 5.3.4 of this specification. Stress/strain curves shall be produced for each tensile test.

A3 Charpy Impact Tests

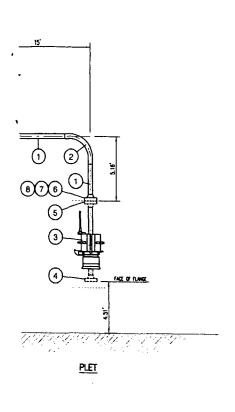
A Charpy transition curve shall be developed for each pipe by taking a set of 3 tests at 10°C intervals over the range -80°C to +20°C.

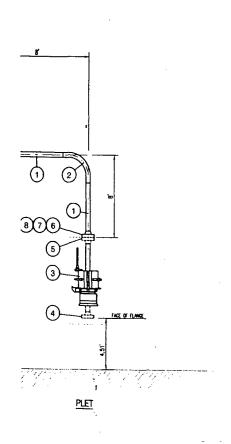
A4 Pitting Corrosion Tests

ASTM G48 pitting corrosion tests in accordance with Section 5.3.9 of this specification shall be carried out on a sample from each of the selected pipes.

A5 Micro-Structural Examination and Ferrite Count

A sample from each pipe shall be examined for ferrite content and presence of inter-metallic phases in accordance with Sections 5.3.7 and 5.3.8 of this specification.





		BILL OF MATERIAL - JUMPER SPOOL
ITEM	QTY.	DESCRIPTION
1	225 LF	4.500" O.D. x 0.438" W.T. LINS S32740/S0/60 DUPLEX SMLS LINE PIPE, WITH 18 MILS FBE COATING
2	12	4.500" D.D. x 0.438" N.T. UNS \$32740/50/60 DUPLEX SMLS INDUCTION BEIND, 90 DEG, 50 (20") RAD, 12" TANGENT, WITH 18 MILS FBE COATING
3	4 ,	FEMALE 4"-10,000 RAC (REMOTE ARTICLEATED CONNECTOR) IS MANUFACTURED BY OIL STATES (FREE ISSUE)
4	4	MALE 4"-10,000# RAC (REMOTE ARTICULATED CONNECTOR) IS MANUFACTURED BY OIL STATES
		(TWO ON WELLHEAD, TWO ON PRODUCTION PLETS)
5	4	4 1/16" API 10000# RTJ WN FLANGE, 4.09" DIA BORE, AND 4130 (FREE ISSUE BY OIL STATES)
-6	4	4 1/16" API 10000/ RTJ WN FLANCE, 3.624" DIA. BORE TAPER TO 4.09" DIA. AT FLANCE FACE END. A182 F53, F54, F55, UNS 32780
_7	4	RING TYPE METALLIC GASKET, R-155, TYPE BX, FOR API 4 1/16" 10000/ RTJ FLANCE, UNS NO6625
_B	4	SET OF (8) 1 1/8" DIA x 8" LG. FLG. STUDS, ASTM A320 L7M, W/ 2 HEAVY HEX HUTS, ASTM A194 2HM
	- 1	

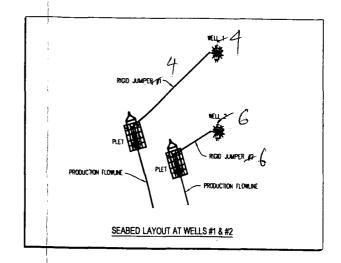
NOTES: 1. ITEM 4 IS NOT IN THE SCOPE OF WORK FOR THE JUMPERS.

THEY ARE SHOWN FOR INFORMATION PURPOSES ONLY.

2. 78FT. ADDITIONAL PIPE TO BE PROCURED FOR FIELD DETERMINED LENGTHS.

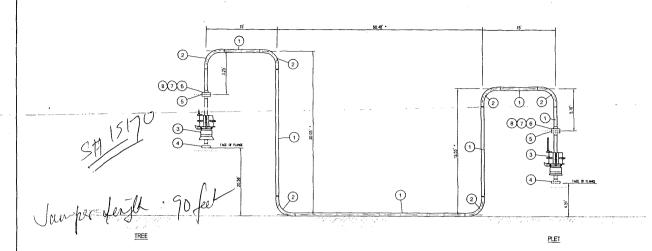
3. THE FLAMES ON THE FEMALE HURS (FREE ISSUE) WILL BE OVERLAD WITH UNS NOGEZS.

• NOTE: FELD DETERMINATION OF VALUES.

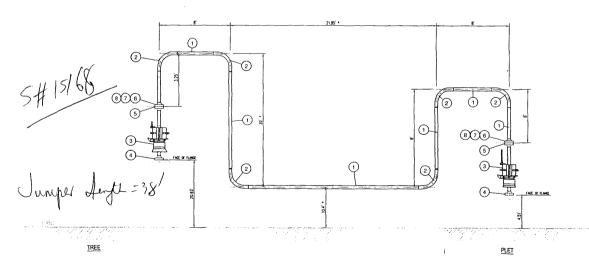


DATE	BY	REVISION DESCRIPTION APPROVED FOR CONSTRUCTION ADDRED PIPE COATING	ENCREER'S STAMP:	DRAIN BY: R. ACREE DATE: 03/10/DS CHECKED BY: P.F.		ATP OIL & GAS CORPORATION		MC-711 FIELD DEVELOPMENT		
05/16/05 15/13/2005 13/24/2005	RKA			DATE: 04/19/05 APPROVED BY: N.C.D. DATE: 04/21/05 PLOT SCALE: 1=1	_	BLUEWATE	PEGASUS	PRODUCTION JUMPERS		
	SJAY/ZOOS RIXA SSJED FOR REVEW AND COMMENT NEW MORRES OF THE SIMILE S SHIT TO BE ACCOMMEND AS WAS UNKNOWN MICHIGANNE DEGREETS 2000 In the SPACE PROTECTION ON THE STAMP S ACCOMMEND BY THE GROWN AND AND SHARING OF ME DICHER.			SCALE: N.T.S. SCAL THER FOR IT-SET (PARISE OUT (N° 18")			International	ле но. 1166190	1166190N006	энет ж 00

94ET NO. REV.



PRODUCTION JUMPER TYPE 1 - SEABED SUPPORTED



PRODUCTION JUMPER TYPE 2 - UNSUPPORTED SPAN

NOTE: THE DMENSONS PROVIDED FOR PRODUCTION AMPER TYPE 2 ARE THE MAXIMUM ALTOWARE EXHIBITS FOR AN UNSUPPORTED SHAF IF ANY OF THE DMENSONS ARE MOREAULT THEN THE NOW FREID DETERMENT DMENSONS OF JUMPER TYPE SHOULD BE GROWN SUPPORTED.

BILL OF MATERIAL - JUMPER SPOOL DESCRIPTION

ITEM QTY.

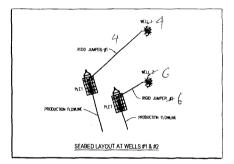
1 225 LT 4500° CD. * 0.408° RT. UMS SSZYAD/SO/SO DUPLES SMIS UMP PPE, WITH 18 MES FEE COATING
2 12 4500° CD. * 0.408° RT. UMS SZYAD/SO/SO DUPLES SMIS SMICTOR REPORT, 50° (20°) RM. 12° IMAGOVI, WITH 18 MES FEE COATING
3 4 TEVALET C*-100000 PAC (REDUITE APRICULATED COMMICTION) IS WARRAFCHERD BY OUT STATES (TREE SSSE)
4 4 WARE C*-100000 PAC (REDUITE APRICULATED COMMICTION) IS WARRAFCHERD BY OUT STATES (TREE SSSE)

Mag. 4 - 10,000 Pac (RADIC AMBOLARE DOMECTOR) IS WAN ACTURED BY DE STATES,
(1/10) ON MERIADI, THO OP RODOCTION PCE-1;
4 + 1/16" AP 10,000 RT W TLANG, 1,00" DB 1,00°, AP 130 (THE FISSA BY DL STATES)
4 + 1/16" AP 10,000 RT W TLANG, 1,30" DB 1,000 TAVER TO 1,00" DB A.X TLANGE TACE EDI. ALBE TSJ. TSA, 1/55, UNS. 32760
4 RIGG THY METALLIC CASETT, B-155, THY BB, TDR APF 4 1/76" TROODY BY TRANGE, UNS. 505505
5 SET 07 (6) 17 (6) DB 3 AF 16 TE, DS 3,DS AS MA 350 TW. 9/2 + 2447 TR 10/15, US 10/15 CAP
5 SET 07 (6) 17 (6) DB 3 AF 16 TE, DS 3,DS AS MA 350 TW. 9/2 + 2447 TR 10/15, US 10/15 CAP
5 SET 07 (6) 17 (6) DB 3 AF 16 TE, DS 3,DS AS MA 350 TW. 9/2 + 2447 TR 10/15, US 10/15 CAP
5 SET 07 (6) 17 (6) DB 3 AF 16 TE, DS 3,DS AS MA 350 TW. 9/2 + 2447 TR 10/15, US 10/15 CAP
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5 SET 07 (6) 17 (6) DB 3 AF 16 TE DS 350 AS MA 350 TW. 9/2 + 2447 TR 10/15 CAP
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5 SET 07 (6) DB 3 AF 16 TE DS 350 AS MA 350 TW. 9/2 + 2447 TR 10/15 CAP
5 SET 07 (6) DB 3 AF 16 TW. 10 T

NOTES: 1. ITEM 4 IS NOT IN THE SCOPE OF WORK FOR THE JUMPERS.
THEY ARE SHOWN FOR INFORMATION PURPOSES ONLY. 2. 76FT. ADDITIONAL PIPE TO BE PROCURED FOR FIELD DETERMINED LENGTHS.

3. THE FLANCES ON THE FEMALE HUBS (FREE ISSUE) WILL BE OVERLAD MITH LINS NOSE25.

NOTE: FIELD DETERMINATION OF VALUES.



DATE	BY	REVISION DESCRIPTION	ENCINEER'S STAMP:	DRAWN BY: R. ACREE	T
		L		DATE: 03/10/05	7
				OEOXED BY: P.F.	7
			1	DATE: 04/19/05	7
			1	APPROVED BY: N.C.O.	7-
05/16/05	RKA	APPROVED FOR CONSTRUCTION	1	DATE: 04/21/05	7
05/13/2005	RKA	ADDED PIPE COATING	1	PLOT SCALE: 1=1	7
	05/16/05	05/16/05 RKA	05/16/16 RAA APPROVED FOR CONSTRUCTION	00/4/05 RNA APPROVID FOR CONSTRUCTION	DATE - 03/10/05

ATP CORPORATION BLUEWATER INDUSTRIES PEGASUS

International

MC-711 FIELD DEVELOPMENT

PRODUCTION JUMPERS

00 8Ex

A2 05/13/2005 RILA ADDED PIPE COATING

A1 03/74/2006 RILA SSUED FOR REVIEW AND COMMENT

A1 03/74/2006 RILA SSUED FOR REVIEW AND COMMENT

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SCALE: N.T.S.

1166190N006

ATP OIL & GAS CORPORATION

May 23, 2005 *Revised 06/06/05*

Mr. Donald C. Howard Regional Supervisor U. S. Department of the Interior Minerals Management Service 1201 Elmwood Park Boulevard New Orleans, Louisiana 70123-2394

Attention:

Mr. Alex Alvarado

MS 5232

RE:

Application for a 6.895-Inch OD Bulk Oil Right-of-Way Pipeline, Production Riser, Rigid Jumper And Associated Umbilical To Be Installed In and/or Through Blocks 711 and 755, Mississippi Canyon Area, OCS Federal Waters, Gulf of Mexico, Offshore, Louisiana

Gentlemen:

Pursuant to the authority granted in Section 5 (e) of the Outer Continental Shelf Lands Act (67 Stat. 462) (43 U.S.C. 1331), as amended (92 Sta. 629), and in compliance with the regulations contained in Title 30 CFR, Part 250, Subpart J, ATP Oil & Gas Corporation (ATP) is filing this application in quadruplicate (original and three copies) for a right-of-way easement two hundred feet (200') in width for the construction, maintenance and operation of a 6.895-inch bulk oil right-of-way pipeline with a flexible production riser, rigid jumper and associated umbilical to be installed in and/or through Blocks 711 and 755, Mississippi Canyon Area, OCS Federal Waters, Gulf of Mexico, Offshore, Louisiana. ATP agrees that said right-of-way, if approved, will be subject to the terms and conditions of said regulations.

The proposed right-of-way pipeline and umbilical will originate at Subsea Well No. 006 located on ATP' Oil & Gas Corporation's (ATP'S) Lease OCS-G 14016, Mississippi Canyon Block 711, also known as Gomez, and proceed in a southernly direction, looping back to the host facility, ATP's proposed Floating Offshore Installation (FOI) "A", also located on ATP's Lease OCS-G 14016, Mississippi Canyon Block 711. Total length of the proposed right-of-way pipeline is approximately 7933-feet (1.50 miles). The associated umbilical will originate at the host facility and terminate at the PLET (Pipeline End Termination) also located in Mississippi Canyon Block 711.

The proposed oil pipeline, one of two to be constructed, will transport production from Subsea Well No. 004ST01, Lease OCS-G 14016 to the Gomez FOI "A" (described above) for processing and measurement. Once processed and measured, the produced hydrocarbons will depart the platform via a 8-inch oil right of way pipeline to a tie-in point with Equilon's existing oil right-of-way

MIRO ST/5/88 926865

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Bight-of W	ay Pipeline Application	0		Segment No.:				
Huiður-oi-wa	ay ripenne Application	ļ		Jeginent No				
2								
3 Instructions:								
4 1. Complete	one form for the pipeline segment submitted in your application. A ROW							
5 application	n may only contain one proposed pipeline segment.			ļ			!	
6 2. Complete of	one form for each unattached umbilical submitted in your application.						,	
7 3. Provide res	sponse/data for all items that are sharled. Other items as required.							
8 4. Provide on	e original and three identical copies of all application materials.							
9	V	Ï				i		
10 Pipeline Rout	te Data			†		[
	sks and lease numbers contacted by the pipeline. (Insert rows as needed)	Area	Block No.	Lease No.	<u>Operator</u>		i i	
	unleased, so note.)	10000000000					1	
13		Mississippi Canyon	711	G14016	Anadarko E&P Company LP/	TP Oil and	Gas Corp	oration
14		Mississippi Canyon	755	G24105	Nexen Petroleum U.S.A. Inc.			
15						:		
16		1		1	†			
17 Contact Infor	mation			†			: :	
	pany name (ROW permittee/holder)	ATP Oil and Gas Corporation						
	ompany representative signing application	Mickey W. Shaw						
20 Phone No.		713-622-3311				: !	: ! ;	
21 Fax	rangan kalabadan dan dalah dalah dan dalah dan dalah san dalah karan sangan sahin gan san sahida san sangari	713-403-7002						
22 E-Mail		mshaw®atpog.com		1		i I		
23 Mailing add	Mrpss	4600 Post Oak Place Suite 200						
24		Houston, Texas 77027-9726		1				
24	rando de la ción de la compaña de la comp	110001011, 10200 77027 0720						
as BOW hold	er's MMS code (five digit)	1819		†		l		
25 1101110101	or a mino-codo (nivo-cigit)	10.10		†		!		
20 Designated or	perator company name	ATP Oil and Gas Corporation		†		1		
29 Phone No.		713-622-3311		†			;	
30 Fax		NA I						
31 E-Mail		groland@atpog.com		ŀ		:		
32 Mailing add	trace	4600 Post Oak Place Suite 200		Ī	** / 1800	ì		
32 Maining auc		Houston, Texas 77027-9726				;	į	
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35 Delators	MIMIS CODE (TIME DIGIT)	1013				I	'	:
37 Regulatory co	otaet (Nama)	Sharon DeSimoni				i		
38 Company r		J. Connor Consulting, Inc.		†	!		,	
39 Phone No.		281-578-3388					:	: j
40 Fax		281-578-8895			1	:	ł i	
40 Fax		sharon desimon@iccteam com					;	
41 E-IVIAH		STATE OF COST TABLE COST				I	:	
43 Technical con	tsot (Name)	Daniel H. Longwell, P.E.		†	+		:	
		Bluewater Industries		1		1	[
44 Company r		713-802-2060						.
		713-802-2060			†	1	!	
46 Fax		dlongwell@bluewaterindustries.com		<u>+</u> ·	†	1	į į	
47 E-Mail	<u>an an antara de la certa de la desta de la deliminación de la de</u> Transporta	Garantiyen iyondewaten and isanes COIII		-		l	!	
48				†		1	į	
49 Fees	fee of \$2,350 enclosed? (Required)	Yes		†	1]		
50 Application	ree of \$2,350 enclosed? (Required) of \$15 per mile or every fraction thereof enclosed? (Required)	Yes Yes		+		İ	i j	
51 Hental lee	01-212 bet time of exert hachor metern englosen; (Ledanea)	1.50		+				
52 Hight-of-Wa	ay length (miles) e.g., 5.71	\$2,380.00	-	+			ļ	
53 Total check		\$2,380.00 5/18/2005		+				
54 Check date		415720		†	†	1		
55 Check num	nber	4				}	[
56 Name of fir	nancial Institution upon which check is written	CHASE BANK OF TEXAS		<u> </u>	<u> </u>			

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5	7		· · · · · · · · · · · · · · · · · · ·					
5	Basic Pipeline Data			i 			į	:
	Line service, e.g., oil, gas, bulk gas, lift, injection, service, etc.	Oil & gas						1
6		7,933		* !			:	
6		7,933		Ţ 			ļ	ı
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-	Pipeline designed for bi-directional flow? (Y/N)	No		t :			į l	1
6		N/A						ĺ
6		No		!· 				
6		N/A		İ	1		i	i
6								
	Pipeline Origin				† 			
6	Type Facility, e.g., Platform, Well, Subsea Well, PLEM, Subsea Manifold, Subsea Tie-in	MC 711 Subsea Well No 006					1	1
7		SS Well No. 006			:			
H		Yes -Floating Offshore Installation		! !	1			:
1 2	Manned platform? (Y/N/NA)	above		I I	0			i
7:		Mississippi Canyon			: 		·	Í
7:		711		į			; ;	i
7.		OCS-G-14016						
75		No		Ï			ļ	į
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7					•			
	Pipeline Destination					•		ĺ
7	■	MC 711 Gomez FOI						1
8		"A"					. !	i
8		Yes		ī i		1	. :	
83		Mississippi Canyon		ļ	i !	! !	!	
8		711				1		
8	OCS Lease	OCS-G-14016		i 		i		1
8		No						ı
8					,			ı
8	Pipeline Appurtenances			1				i
8		Yeş			Í			
8		Umbilical						
91	If yes, specify appurtenant area and block location, e.g., MP 134	MC 711			1			1
9				i ! !		i ı		
9:	Construction/Air Quality Data			1	! !	i	,	
9:		DP vessel		Į.	1			
9		NA .		1	:			
9	Onshore Facility Location	Amelia, LA		1		1	t	ŧ
9	Pipeline construction duration (days)	42 Days		: 	•			ŕ
9	Construction start date (projected)	8/1/2005		ļ .	1		, ;	į.
9					İ	!	i i	I
9:	Pipeline product data	Section 1997 and the section of the				! !	. :	!
10		10						1
10	Gravity of gas (Air = 1.0)	0.813						ļ
10	Design maximum flow rate of oil/condensate (b/d)	9,000		 		! !		i
10	3 API or specific gravity of oil/condensate	0.88		!	1		ĺ	
10	4 H2S concentration (ppm)	Nil		1		 	: !	I
10	5 Maximum anticipated pipeline temperature (degrees F)	120		1				ı
10	6 CO ₂ concentration (ppm)	4200				i		i
10		Yes				:		i
	Hydrates anticipated (Y/N)	No						F
	Paraffin anticipated (Y/N)	No		<u> </u>	İ.		: [i
1	d	200			i 1			
1	Submerged Component Design Data	Diameter 1	Diameter 2	Diameter 3	1			1
100	downing does come the control of the							

Δ.	1 8	T	T 0	T F	F	G	ТН
Outside diameter (inches)	6.895 - dynamic flexible pipe	Ÿ					
Wall thickness (inches)	1.4475 - layers, as per riser data					T	Ť
114 Grade	NA				T		
Hydrostatic test pressure (psig)	9,375				T		
HTP duration (hours) (Must be equal to or greater than eight)	8			1	1		-
117 Type external corrosion coating	polypropylene					T	
118 Corrosion coating thickness (mils)	236					T	
119 Concrete coating density (pcf)	NA NA						
120 Coating thickness (inches)	NA NA						
121 Type internal corrosion coating (Type/NA)	NA NA						.1
122 Coating thickness (mils) , Mils/NA)	NA NA				<u> </u>		<u> </u>
123 Bare pipe specific gravity	1.83						<u> </u>
124 Weighted pipe specific gravity:	NA NA	· · · · · · · · · · · · · · · · · · ·					
125 Pipe is non-standard? (Y/N)	Yes					ļ	1
lf yes, note type, e.g., coil tubing, pipe-in-pipe, flexible pipe, other (specify) (Type/NA)	Flexible Pipe					_	.
127				 	<u> </u>	-	
128 Cathodic Protection Design Data	N/A			 			-
129 Design Type, e.g., bracelet enodes, anode sleds 130 Anode Type, e.g. Galvalum III, Aluminum, etc.	NA NA			-	+	÷ -	+ 1
131 Net anode weight (pounds)	NA NA					-+	-
132 Spacing (feet)	NA NA						
133 Number of anodes:	NA NA						
134 Anode life (years)	NA NA				 		
135 Designs for systems other than bracelet anodes required. (Attached/NA)	NA NA				 		
136							
137				·	+		
138 Departing Riser Design Data	Diameter 1	Diameter 2	Diameter 3				
Outside diameter (inches)	6.895 - flexible pipe		<u> </u>		+	-	†
140 Wall thickness (inches)	1.4475 - layers, as per riser data				†-· · · · ·	-	1
141 Grade	NA			-	1		
142 Hydrostatić test pressure (psig)	9,375					T	
143 HTP duration (hours) (Must be equal to or greater than eight)	8			T		T	T
splash zone=S.Z.	Below S.Z.	In S.Z.	Above S.Z.		1		i
145 Type external corresion coating	same						
146 Coating thickness (mils or inches)						T	Ţ
147 Type internal corrosion coating (Type/NA)							
148 Coating thickness (mils) (Mils/NA)							
149 Riser guard design attached? Required if origin is calsson or platform (Y/NA)]
150 Catenary riser? (Y/N)				<u> </u>	<u></u>		
151 If yes, VIV reduction, installation tension, anchoring, tension monitoring attached? (Y/NA)		*		ļ	ļ., ,	.	l
152				 	ļ <u> </u>	ļ	
153 Receiving Riser Design Data	Diameter 1	Diameter 2	Diameter 3	 	ļ	1	
154 Outside diameter (inches)	N/A			+-			
155 Wall thickness (inches) 156 Grade					.	- 	
156 Grade 157 Hydrostatic test pressure (psig)							ļ
158 HTP duration (hours) (Must be equal to or greater than eight)							
159 splash zone=S.Z.	Below S.Z.	In S.Z.	Above S.Z.				
160 Type external corrosion coating	Delow 3.2.	111 3.2.	Above 3.2.		+		
160 Coating thickness (mils of inches)				·	 	·	
162 Type internal corrosion coating (Type/NA)						····	
163 Coating thickness (mils) (Mils/NA)				 	† · · · · · · · · · · · · · · · · · · ·	 	
164 Riser guard design attached? Required if origin is calsson or platform (Y/NA)				 	h	-f	I
165 Catenary riser? (Y/N)					†	- 	
166 If yes, VIV reduction, installation tension, anchoring, tension monitoring attached? (Y/NA)			***************************************		 		
				T	†	+	
1001				<u> </u>	1		

					r F	GН	\neg
A	В		U				\neg
168 Flange and Valve Data	150.000				1	1	H
169 Flange type (ANSVAPI)	API 10K	1			1	į	i
170 Flange pressure rating (psig)	10,000	Ï				ŀ	- 1
Derated pressure rating (pslg/NA)	N/A				1	ŀ	
172 Valve type (ANSI/API)	API 10K				1	İ	ı
173 Valve pressure rating (psig)	10,000	1		1	1 1	i	- 1
174 Derated pressure rating (psig/NA)	N/A			\$ 1	1	i	I
175				!	i c	i	- 1
176 Pipeline Burial Data							- 1
177 Buried minimum of three feet? Y/N/Self (Burial required if less than 200' water depth)	No					i	- 1
178 Burial method (jet, plow, self, other(specify))	N/A				!	i	
179 If self burial, provide seafloor strength in ksf. (Must be less than 0.2 ksf) (kips/NA)	N/A				1		
180 Data supporting self burial attached? (Y/NA)	N/A						
Data supporting self-burial attached? (T/NA)	11/2					i	ı
181		į				!	ŀ
182 Miscellaneous Data	Yaa	į				1	
Non-discrimination in employment form attached? (Required)	Yes				1	:	
184	7	i		F		:	į
185 Oil Spill Financial Responsibility Requirement Determination				-	1	1	
Static Pipeline Volume (Bbls.) If greater than 1,000 then WCD volume required	122			<u> </u>	1	ì	1
Worst case discharge volume (Bbls.) If greater than 1,000 then OSFR required	NA	į			i	İ	- 1
Proposed Right-of-Way included under company OSFR coverage? (Yes/Pending/NA)	NA NA	İ					l
189		;				i	- 1
190 Certified plat attached? Plat is required.	Yes	1		İ		i	
191 Diskette per NTL 98-09 attached? Diskette is required.	Yes	j		i			
192		i					- 1
193 Does pipeline cross into State waters (Y/N)	T No						l
194 If yes, State permit required (Attached/Applied For/NA)	N/A	1		Ī L	!		
195 If yes, COE permit required (Attached/Applied For/NA)	N/A	ţ			1.	1	- }
193 II yes, GCE permit required (Attached Applies 1 GATAT)							
197 Minimum water depth (feet below sea level)	2940	İ		l		i	l
198 Maximum water depth (feet below sea level)	2980	1		I		į	į
198 Maximum water deput (reet below sea lever)				!	1	f	
199	Yes		•				
200 Water depth greater than 400 meters? (Y/N)	previously submitted					!	- 1
201 If Yes, Chemo : tudy required (see NTL 2000-G20) (Attached/NA)	previously submitted			•		t	- 1
202	Yes	1			1	1	- 1
203 Deep Water Operations Plan submitted to MMS? (See NTL 2000-N06) (Y/NA)						i	- 1
204 If yes, date submitted (Date/NA)	25-Mar-05				1	!	
205				1	1	i	- 1
206 Pipeline to be towed to location? (Y/N)	No :				1	i	1
207 If yes, dragged on bottom? (Y/N/NA)	and the second account of the second			i	1		
208					1	ļ	
209 Artificial reef in vicinity? (Y/N)	No			+	1	İ	1
210 If Yes and PL in La., PL must be > 500' away. Confirm Y/NA					1	i	- !
Distance to reef (feet).				-	i	ļ	1
212 If Yes and PL in TX., PL must be > seven times water depth away. Confirm Y/NA	į						- 1
Distance to reef (feet).						ļ	
214							
215 Hazard Report submitted? (Yes) Hazard Report is required.	Yes			1		ļ	Į
216	The second secon	}				ļ	
217 Shallow Hazards Analysis Statement included? (Yes) SHAS is required in cover letter.	Yes						
Eri Olimon, Indenios Grandas, amarina in Francis de Paris, de Paris de Pari		İ				į	l
219 Umbilical associated with pipeline?: (Y/N):	Yes			1	1	1	ļ
220 Umbilical type, e.g., hydraulic, electric, other(specify) (Type or NA)	hydraulic/gas lift	,				1	1
Umbilical outside diameter (inches) (Diameter or NA)	4-inch					!	
222 Umbilical outside diameter (inches) (Diameter of NA) 222 Attached to pipeline? (Y/N/NA; If No, will be assigned a unique segment number)	No			1		1	- 1
Attached to pipeline? (Y/M/NA II No, will be assigned a unique segment number)	No - Considered Appurtenance			!			ļ
223 If no, separate application form attached? (Yes/NA)	1 140 - Considered Appurtenance			<u> </u>	<u> </u>		

... - ---- . .

	R		n n	F	F G	Н
	0	ļ			<u> </u>	
224	\(\text{\tince{\text{\tex{\tex					
225 Does pipeline contact anchorage area or fairways? (Y/N)	No					
226 If Yes, burial depth in anchorage areas or fairways consistent with COE permit? (Y/NA)	NA NA	<u> </u>				
227 If yes, COE permit attached? (Y/NA/Pending)	NA NA	ļ				
228					L	
229 Pipeline Crossing Data	**************************************			AF A 1 A 1 A 1 A 1 A 1 A 1 A 1 A 1 A 1 A		
230 Does proposed pipeline cross an existing pipeline (Y/N)	No					
231 If yes, enter noted data, adding data rows as required.	Operator	Segment No.	Size (inches)	Service	Notified?	
232						
233 If yes, minimum clearance between lines must be 18". (Yes/NA)	N/A					
If yes and < 500' water depth, must have 3' cover or concrete mats. (Confirm cover or						-
234 concrete mat.)	N/A					
235 If sand bags, slope is 3/1. (Confirm Yes/NA)	N/A				T	
236 If concrete mat, specify manufacturer	N/A	 				
237 If concrete mats, mat edges jetted below mudline. (Yes/NA)	N/A					"
238 Crossed pipeline operator notified? (Y/N/O O = crossed pipeline owned by applicant)	N/A				1	···
200 Clossed bibenine oberator nomined: (1000 C = crossed bibenine owned by applicant)	14/7	····	t			
240 H ₂ S Contingency Plan and Modeling Data					† †	
H ₂ S Operations Contingency Plan attached as H ₂ S concentration greater than 20 ppm			<u></u>		 	1 1
	N/A					
241 (Y/Pehding/NA)	NA	ļ			+	
242 Air Dispersion Model attached as H ₂ S concentration greater than 500 ppm (Y/pending/NA)	NA NA	<u> </u>			ļ -	-
H ₂ S Crossing Contingency Plan attached as crossed pipeline carries H ₂ S in concentrations						
243 greater than 20 ppm (Y/Pending/NA)	NA],				1.
244	444 P. C. C. C. C. C. C. C. C. C. C. C. C. C.				_	
245 Subsea Tie-in Data		L			L	
246 Does pipeline tle into a subsea pipeline? (Y/N)	No	<u> </u>			1	
Ties to existing valve or hot tap? (Identify which/NA)	L					I
		<u> </u>			1	
248 Segment number of pipeline being tied in to (SN/NA) 249 MAOP of pipeline being tied in to (MAOP/NA)			L			
250 If existing valve, letter of no objection from tie-in operator attached? (Yes/NA)				L	<u> </u>	
251 If hot tap, appurtenance application submitted to MMS? (Yes/NA)					1	
ls assembly snag proofed? (Y/NA) Required if less than 500' water depth.		T				
253 If sand bags used, slope is 3/1 (Y/NA)		T				
254 If sand bags used, 3' coverage required (Y/NA)		T			T	
255		<u> </u>			L	
256 Surface Tie-in Data		T	ļ			
257 Does pipeline tie directly into another pipeline at a surface location? (Y/N).	No		 		1	İ
258 Segment number of pipeline being tied in to (SN/NA)		+				
259 MAOP of pipeline being tied in to (MAOP/NA)						† :
200 June 5 promise sound and artifer 1707/		† · · · · · · · · · - · · -			†	
261 Spill Response Plan Data		L	i		11 " t."	- +,
262 Type of spill response plan (OSCP/OSRP per NTL 98-30)	OSRP				1	
263 Date spill plan submitted to MMS	3/23/2005	 			+	+
263 Date spill plan approved (Actual Date or "Pending")	3/29/2005				† · 	
264 Date Spin plan approved (Acada) Date or Fending)	3/29/2003	 				
265	10.0					ļ l
266 Safety Schematic Information	14/-14					
267 Pressure source identified? (well, separator, pump, etc.)	Well	 	 		ļ	+ 1
268 MSP/MAWP/SITP of source shown? (psig)	6,400	ļ	ļ	<u> </u>	++	+
269 Origin/destination specification breaks shown on schematic. (Y/NA)	Yes	ļ .		<u></u>	ļ .	
270 Receiving segment number noted? (Segment Number or N/A)	N/A				ļ	
Receiving segment no. MAOP (psig) (MAOP or N/A)	N/A				1	<u></u>
272 Calculated pipeline MAOP (psig)	7,500					1
273 Operator responsibility transfer point shown? (Yes/NA)	NA	<u></u>				1
274	1				1	1
275 Collapse Information (Deepwater Pipelines Only)	THE RESERVE OF THE PARTY OF THE					
					· · · · · · · · · · · · · · · · · · ·	

	· · · · · · · · · · · · · · · · · · ·	I B	C	D	E	T F	G	H
276	Water depth (feet)	2,975						
277	External pressure (psig)	1,333			† · · · · · · · · · · · · · · ·	1		I
278	Collapse pressure (psig)	3,237					1	
279	Safety factor	2.4				1		
		Attached - Performed by Flexible				Ī		
280	Collapse calculations are required. (Attached/NA)	Pipe manufacturer	L				ļ	1
281	· · · · · · · · · · · · · · · · · · ·					1	ļ <u> </u>	
282	afety Design Review				L == == == == == == == == == == == ==		ļ	
	ipeline Origin		1					
	SHL required at departing end of pipeline (Confirm Yes)	Yes	<u> </u>			ļ	ļ	
285 F	SHL must be downstream of choke and/or flow restrictions (Confirm Yes)	Yes	ļ	 		+	ļ	
	or a well, if MSP > MAOP, a redundant PSH and independent SDVs required (Confirm Yes)	N/A				· - · · · · · ·	·}-· ·	- · · [
	or production equipment, if MSP > MAOP, a redundant PSH with independent SDV is required r a vented PSV is required (Confirm Yes/NA)	N/A						
	bi-directional flow, SDV required (Confirm Yes/NA)	N/A	+		-		İ	-
	pig trap present, safety equipment can not be bypassed (Confirm True)	N/A					1	i - I
	pump on line, must be consistent with API RP 14C A7 (Confirm Yes/NA)	N/A			 			† "
	Pipeline Destination	14/6	<u> </u>	İ	· · · · · · · · · · · · · · · · · · ·		h +	1 1
292	production facility and uni-directional flow, SDV and FSV required (Confirm Yes/NA)	Yes	*			7	ľ.,	<u> </u>
293	production facility and bi-directional flow, SDV and PSHL required (Confirm Yes/NA)	N/A	T			Ι	<u> </u>	
1	production recently and or allowers in the production of the produ					1	T	
294	subsea tie-in and uni-directional flow, FSV and block valve required (Confirm Yes/NA)	N/A			<u> </u>	1		
	subsea tie-in and bi-directional flow, block valve required (Confirm Yes/NA)	N/A			<u> </u>	1	<u>.</u>	
296	gas lift or water injection flowline on unmanned platform, FSV required (Confirm Yes/NA)	Yes			<u> </u>			
297	gas lift or water injection flowline on manned platform, SDV required (Confirm Yes/NA)	Yes			<u></u>			
	crossover platform (pipeline does not receive production), SDV required at boarding point and				1			
298 F	SHL required at departing point (Confirm Yes/NA)	N/A	<u> </u>			ļ .	+	
1 1								
299	crossover platform is non-manned and non-production, FSV required (Confirm Yes/NA)	N/A	<u> </u>			· -		
300	The second secon	The second second second				+		
	Departure Data Valver from NTL 98-20 (buoying of hazards) requested? (Y/N)	Yes				 		
	other departures requested? (Y/N)	No No	· · · · · · · · · · · · · · · · · · ·		† · · ·		i · · ·	
303	If yes, specify.				T	T	İ	1
206	ii yes, specify.				T	†	i ·	
306	The state of the s					1	i .	1 1
307					T			
308	The state of the s		T		<u> </u>	1		
309						*		1
310	And the second s		.1		ļ	ļ.		
311	The second secon		. ↓					
312				ļ <u></u>	 			
313				<u></u>	 	+		
314	AND THE PARTY OF T	. ,			<u></u>	 	ļ .	- 1
315	o Not Enter Data Below This Line - MMS Use Only		<u> </u>	L	 	†	1	
316	IPELINE MASTER ENTRY SHEET				İ	· ·	İ	
0.1	lame		MMS Engineer en	t	 		1	1
	aame Oate		MMS Engineer en			-		
	legment Number		MMS Engineer en		· · · · · · · · · · · · · · · · · · ·	† · · · · · ·	İ	
	light-of-Way Number		MMS Engineer en					
	light-of-Way Permittee		1			I		
	light-of-Way Permittee Code		I	I		1		[i]
	Operator	ATP Oil and Gas Corporation	I					1
	Operator Code	1819				<u> </u>	<u>L.</u>	لـــــــــــــــــــــــــــــــــــــ
	<u> </u>							

A	8	CDD	Ĕ I	F	G	н
326 Approval Code	Right-of-Way					
327 Authority Code	,	MMS Engineer entry				ı
328 Pipe Size	6.895 - dynamic flexible pipe	, , , , , , , , , , , , , , , , , , ,				ı
329 Product Code		MMS Engineer entry			1	ı
330		J 1	ł			ı
331 ORIGIN			İ		İ	ı
332 Facility Type	MC 711 Subsea Well No 006					ı
3331 Identifier	SS Well No. 006		1		i .	i
334 Area	Mississippi Canyon		i		l j	ı
335 Block	711				l	ı
336 Lease	OCS-G-14016	'	İ			ı
317		"				J
338 DESTINATION			1			ı
339 Facility Type	MC 711 Gomez FOI	†				ı
340 Identifier	"A"	į į			! !	J
341 Area	Mississippi Canyon		į		i i	1
342 Block	711		ì		1	ı
343 Lease	OCS-G-14016					ı
344	000 0 7,010		İ			ı
345 OCS Segment Length	7,933				1	ı
346 State + Federal Pipeline Length	7,933					,
346 State + Federal Pipeline Length 347 Cathodic Code	NA					į
34H Cathodic Life Time (Years)		MMS Engineer entry			İ	
349 Minimum Water Depth (feet)	2940					1
350 Maximum Water Depth (feet)	2980	-				
2551	_344					
352 Buried Designator Flag	No					1
353 Bi-directional Flag	No		İ			1
354 Alternate Service	N/A	- 1				
355 Recv Segment No. (Sub-surface)	0					1
356 Recv MAOP	0					1
357 Assigned MAOP		MMS Engineer entry				1
358 Pipeline Status Code	Proposed	1,111				
359 Right-of-Way Status Code	Pending		-	İ		
360		†				
361 Comments		MMS Engineer entry	İ			

ATTACHMENT "B"

ATP OIL & GAS CORPORATION

WELL NO 6 PRODUCTION RISER AND FLOWLINE MISSISSIPPI CANYON AREA, BLOCK 711, PROPOSED GOMEZ PLATFORM THROUGH MISSISSIPPI CANYON AREA, BLOCK 755

PIPELINE SPECIFICATIONS

1. The company person to contact for information on technical points is as follows:

> Mr. Gregory D. Roland ATP Oil & Gas Corporation 4600 Post Oak Place Suite 200 Houston, Texas 77027-9726 Telephone: 713-622-3311

Fax: 713-403-7002

2. Production Flexible Riser and Jumper Description

Riser at MC-711 and Jumper at SS Well No 6, Proposed Gomez Platform

Riser Type

: Flexible Riser

Approx. Length

: 7933 ft.

Inner Diameter

: 4.00 in. ID

(Refer to Attached Data sheet for the 4.00 inch flexible riser properties)

3. Cathodic Protection System

The flowline will be protected by the sacrificial anode system described below. Neoprene lined riser clamps and insulating flange kit at the top of the riser will insulate the riser from the platform cathodic protection system. The flowline end fittings will be protected by anodes on the PLET.

4. Water Depth

Minimum Water Depth Maximum Water Depth : 2940 ft

: 2975 ft

5. **Description of Internal Protective Measures**

Internal Coating

: None

Corrosion Inhibition Program

: To Be Determined

Pigging Requirements

: To Be Determined

The analysis of the transported products will be monitored and preventive measures, such as inhibitors and pigs, will be employed as necessary.

Appendix B 06/03/05 Page 1

ATTACHMENT "B"

ATP OIL & GAS CORPORATION

WELL NO 6 PRODUCTION RISER AND FLOWLINE MISSISSIPPI CANYON AREA, BLOCK 711, PROPOSED GOMEZ PLATFORM THROUGH MISSISSIPPI CANYON AREA, BLOCK 755

6. Flexible Riser Pipe and Jumper at MC-711 Proposed 'Gomez' Platform

Pipe inner diameter = 4"
Pipe overall diameter = 6.895"
Design Pressure = 7500 psi
Operating Pressure = 4000 psi
Design Temperature = 54.4 ° C
Operating Temperature = 48.0° C

Min. Bend Radius Storage = 3.73 ft Min. Bend Radius Service = 7.2 ft

Burst Pressure = 17,203 psi Collapse Pressure = 3,237 psi Max Allowable Depth = 7.282 ft Failure Tension = 439 kips

Stiffness:

Axial Tension at 20° C = 35588 kip Bending at 20° C = 6786 lbf ft2 Torsional at 20° C = 706 kip ft2

Weight of Pipe	Empty	Liquid Filled
In Air	38.1 lb/ft	44.2 lb/ft
In Seawater	21.5 lb/ft	27.6 lb/ft
Relative gravity in seawater	1.83	1.88

7. Specific Gravity of the Product

The anticipated specific gravity of the pipeline product (Bulk Oil and Gas) is:

Gas SG	= 0.813 (Air = 1.0)
OiLSG	= 0.88

8. <u>Design Capacity</u>

The design capacity for the pipeline is 10 MMSCFD and 9,000 BOPD.

9. Maximum Allowable Operating Pressure

a) Wall thickness and pressure calculations performed by flexible pipe manufacturer.

b) Flanges, Valves and Fittings

All flanges, valves and fittings shall be the following: API 10,000#, 10,000 psig rated, 4 1/16" API Type 6BX.

ATTACHMENT "B"

ATP OIL & GAS CORPORATION

WELL NO 6 PRODUCTION RISER AND FLOWLINE MISSISSIPPI CANYON AREA, BLOCK 711, PROPOSED GOMEZ PLATFORM THROUGH MISSISSIPPI CANYON AREA, BLOCK 755

c) System MAOP

Maximum allowable operating pressure (MAOP) as determined in accordance with DOI, Title 30, Part 250, Code of Federal Regulations, as applicable, is 7500 psig for the 4-inch pipeline.

Hydrostatic Test Pressure (HTP) per CFR, Title 30, Part 250. The hydrostatic test pressure for the pipeline and riser will be based as given below:

Hydrostatic Test Pressure:

Pipeline & Riser

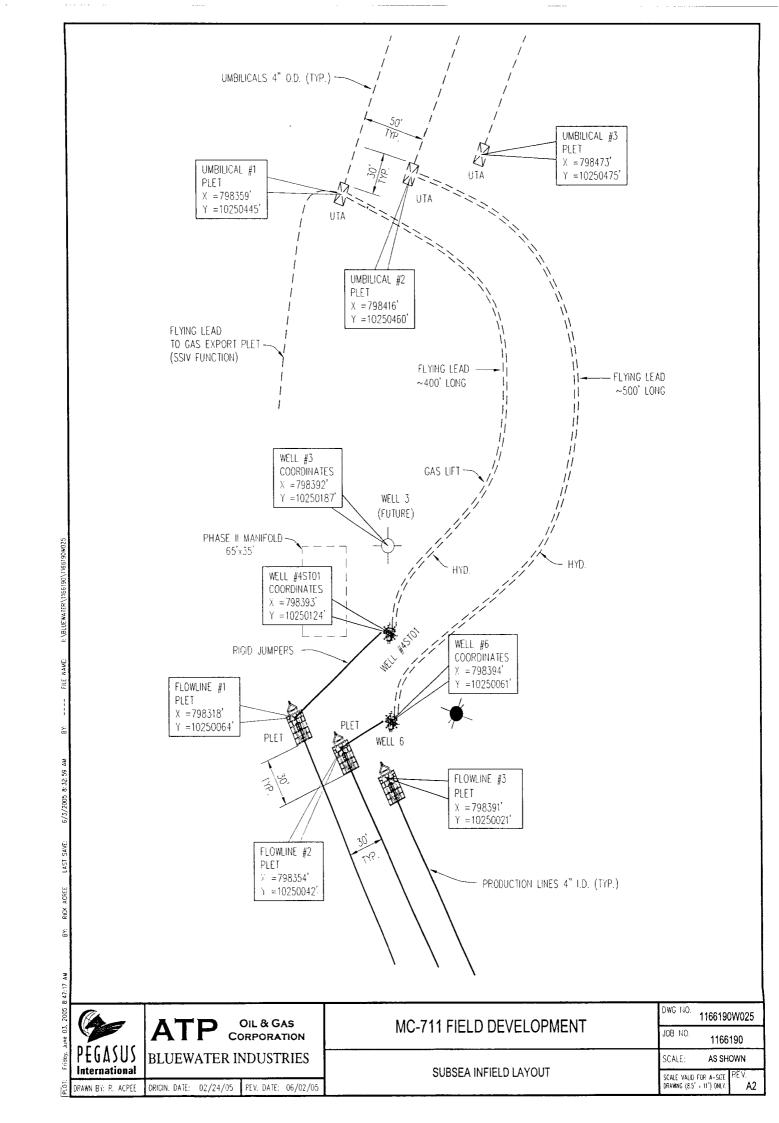
HTP = $1.25 \times 7500 \text{ psi}$ (MAOP) = 9375 psig, for minimum of 8 hours.

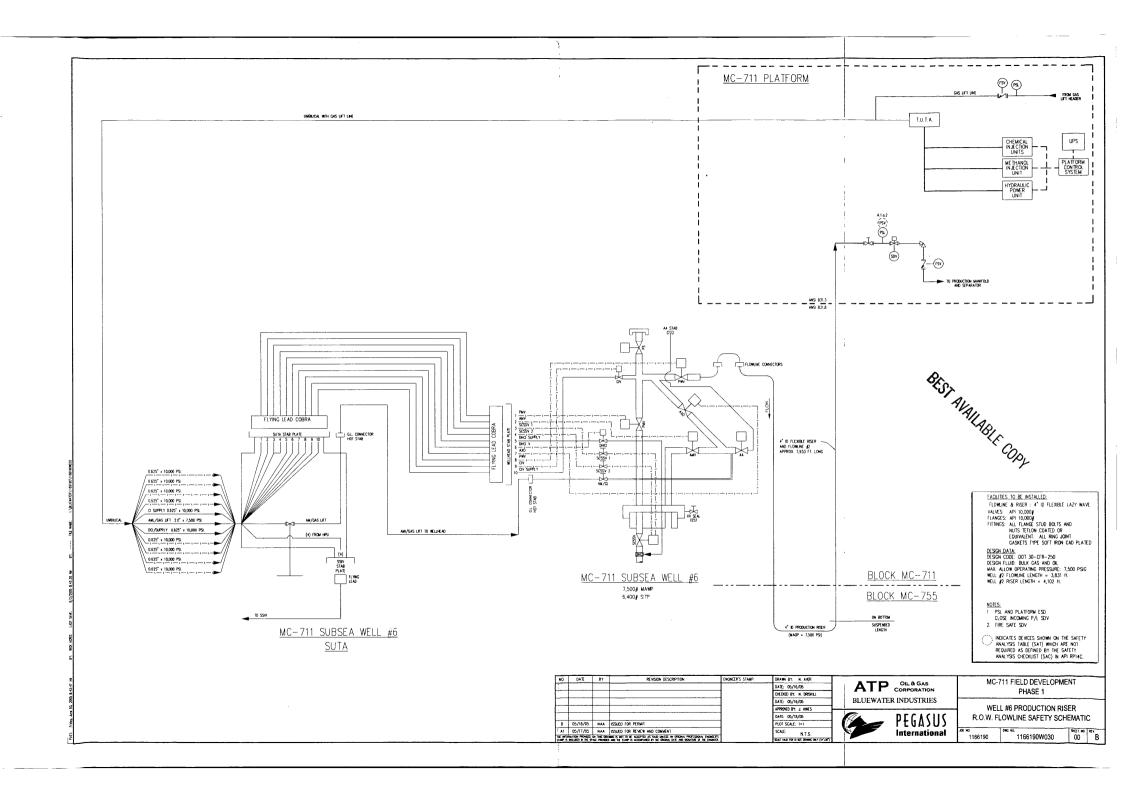
10. Design of the proposed flowline is in accordance with the "Oil and Gas and Sulphur Operations in the Outer Continental Shelf", Title 30, CFR, Part 250.

11. Construction Information

a) Anticipated start date August 1, 2005 b) Method of construction Reel Lay-barge Method of burial Not Required c) d) Time required to lay pipe Six (6) weeks Time required to complete the project Four (4) months e) f) Shore base for construction Mobile, Ala.

Appendix B Page 3 06/03/05





ATP OIL & GAS CORPORATION

S# 15168 15169 MURD



May 23, 2005

Mr. Donald C. Howard Regional Supervisor U. S. Department of the Interior Minerals Management Service 1201 Elmwood Park Boulevard New Orleans, Louisiana 70123-2394

Attention:

Mr. Alex Alvarado

MS 5232

RE: Application for a 6.895-Inch OD Bulk Oil Right-of-Way Pipeline, Production Riser, Rigid Jumper And Associated Umbilical To Be Installed In and/or Through Blocks 711 and 755, Mississippi Canyon Area, OCS Federal Waters, Gulf of Mexico, Offshore, Louisiana

Gentlemen:

Pursuant to the authority granted in Section 5 (e) of the Outer Continental Shelf Lands Act (67 Stat. 462) (43 U.S.C. 1331), as amended (92 Sta. 629), and in compliance with the regulations contained in Title 30 CFR, Part 250, Subpart J, ATP Oil & Gas Corporation (ATP) is filing this application in quadruplicate (original and three copies) for a right-of-way easement two hundred feet (200') in width for the construction, maintenance and operation of a 6.895-inch bulk oil right-of-way pipeline with a flexible production riser, rigid jumper and associated umbilical to be installed in and/or through Blocks 711 and 755, Mississippi Canyon Area, OCS Federal Waters, Gulf of Mexico, Offshore, Louisiana. ATP agrees that said right-of-way, if approved, will be subject to the terms and conditions of said regulations.

The proposed right-of-way pipeline and umbilical will originate at Subsea Well No. 206 located on ATP' Oil & Gas Corporation's (ATP'S) Lease OCS-G 14016, Mississippi Canyon Block 711, also known as Gomez, and proceed in a southernly direction, looping back to the host facility, ATP's proposed Floating Offshore Installation (FOI) "A", also located on ATP's Lease OCS-G 14016, Mississippi Canyon Block 711. Total length of the proposed right-of-way pipeline is approximately 7833-feet (1.48 miles). The associated umbilical will originate at the host facility and terminate at the PLET (Pipeline End Termination) also located in Mississippi Canyon Block 711.

The proposed oil pipeline, one of two to be constructed, will transport production from Subsea Well No. 004ST01, Lease OCS-G 14016 to the Gomez FOI "A" (described above) for processing and measurement. Once processed and measured, the produced hydrocarbons will depart the platform via a 8-inch oil right of way pipeline to a tie-in point with Equilon's existing oil right-of-way

Minerals Management Service 6.895-Inch Bulk Oil Right-of-Way Pipeline Production Riser, Rigid Jumper And Associated Umbilical Mississippi Canyon Area Block 711 & 755 Offshore, Louisiana May 23, 2005

Page Two

pipeline (Segment No. 11433) located in Grand Isle Block 115 or a 10-inch gas pipeline to a tie-in point with the Williams Energy, LLC's existing 20-inch gas right-of-way pipeline (Segment No. 11175) also located in Grand Isle Block 115, Offshore, Louisiana for ultimate delivery to shore. Other transportation facilities associated with the development of the Gomez field include an 8-inch oil right of way pipeline and a 10-inch gas right-of-way pipeline, infield flowlines, rigid jumpers, umbilical and flying leads. Applications for these facilities will be submitted under separate cover.

Upon assignment of a segment number to this application, ATP will proceed with covering the right-of-way pipeline under its current Certification of Oil Spill Financial Responsibility.

ATP will review the approved Regional Oil Spill Response Plan to determine if the installation of the subject right-of-way pipeline will affect the current worst case discharge, and, if applicable, will modify the plan to include the pipeline at the next scheduled update.

Installation of the proposed pipeline and flexible riser will be accomplished by utilizing an installation vessel with dynamic positioning capabilities specifically designed for service in deepwater and certified by the U.S. Coast Guard. The pipeline will be installed using the reel method. The flexible riser will be installed using the Lazy Wave method. The water depths along the route range from 2940-feet to 2980-feet; therefore, the pipeline will not be buried.

There are no foreign pipeline crossings along the proposed route.

The water depth in this area is 2975-feet. The flexible riser at the Gomez FOI "A" in Mississippi Canyon Block 711 will be protected by the pull tube.

ATP hereby requests a waiver from NTL 98-20, Section IV.B, which requires the buoying of all potential hazards located within 150 meters (490) feet of the proposed operations. Utilizing the onboard graphic system during construction operations, ATP will comply with the recommended avoidance criteria of the magnetic anomalies identified in the Fugro Geoservices, Inc. Archaeological , Engineering and Hazard Survey Report previously submitted with the export pipeline applications (Segments 15051 and 15052). Also, an additional report was prepared for ATP for the anchor locations that is included herewith.

During the performance of the engineering and hazard survey in water depths exceeding 1312-feet, the minimum depth for chemosynthetic community potential outlined in NTL2000-G20, some areas of potential active gas expulsion or hydrate mounds were identified in Mississippi Canyon Blocks 711 and 755.

Minerals Management Service 6.895-Inch Bulk Oil Right-of-Way Pipeline Production Riser, Rigid Jumper and Associated Umbilical Mississippi Canyon Area Block 711 & 755 Offshore, Louisiana May 23, 2005

Page Three

Based on data from the side-scan sonar, subbottom data and magnetic data, the probability of disturbing significant prehistoric cultural resources within the corridor for this proposed pipeline is not probable. Ten magnetic anomalies were recorded in the course of this survey, one of which is considered of an unknown nature, age or significance and could possibly represent a wrecked barge with coordinates as previously discussed herein. The remaining nine (9) are pipelines and one well, all considered modern debris from oil and/or gas activity.

The proposed activities will occur outside the Live Bottom (Pinnacle Trend) Stipulation Area.

The proposed pipeline route does not lie within any areas designated as having a high potential for historical archeological resources, prehistoric archaeological sites, or historic period shipwrecks. Therefore, an archeological assessment was not required.

The proposed construction operations will be supported by a crewboat and tug, each making approximately two (2) trips per week, respectively, from an onshore facility located in Amelia, Louisiana.

ATP anticipates commencing installation on approximately August 1, 2005. Estimated time to complete installation of the right-of-way flexible pipeline, flexible riser and umbilical associated with the Gomez project is 42 days. Estimated overall completion time for the entire Gomez project, including installation of right-of-way lines, flexible risers, umbilicals, anchors, the FOI, subsea trees and completion of the wells is 90 days.

ATP will be the operator of the subject right-of-way pipeline.

This application (and any amendments made hereto) is made with our full knowledge and concurrence with the OCS Lands Act (43 U.S.C. 1331, et. seq.), as amended (P.L. 95-372), including the following: Sec. 5(e) addressing pipeline rights-of-way, requirements of the Federal Energy Regulatory Commission relating to notice of hearing, transportation and purchase of oil and gas without discrimination; Sec. 5(f)(1) addressing operation of pipelines in accordance with competitive principles, including open and nondiscriminatory access to both owner and non-owner shippers; Sec. 5(f)(2) which may allow exemption of the requirements in Sec. 5(f)(1); Sec. 5(e) addressing the assuring of maximum environmental protection, including the safest practices for pipeline installation; and Sec. 5(f)(1)(B) which may require expansion of throughput capacity of any pipeline except for the Gulf of Mexico or the Santa Barbara Channel.

Additionally, we expressly agree that if any site, structure, or object of historical or archaeological significance should be discovered during the conduct of any operations within the permitted right-of-way, we shall report immediately such findings to the Director, Gulf of Mexico OCS Region, and

Minerals Management Service 6.895-Inch Bulk Oil Right-of-Way Pipeline Production Riser, Rigid Jumper and Associated Umbilical Mississippi Canyon Area Block 711 & 755 Offshore, Louisiana May 23, 2005

Page Four

make every reasonable effort to preserve and protect the cultural resource from damage until said Director has given directions as to its preservation.

In accordance with applicable regulations, we have forwarded information regarding the proposed project by certified mail, return receipt requested, to each designated oil and gas lease operator, right-of-way or easement holder whose lease, right-of-way or easement is so affected. A list of such designated operators, right-of-way or easement holders is included as Attachment A and copies of the return receipts showing date and signature as evidence of service upon such operators, right-of-way or easement holders will be forwarded to your office when received.

In order to expedite the permit process, we have requested a letter from the operator, right-of-way or easement holder expressing no objection to the proposed project. When obtained, these letters will be forwarded to your office. The proposed right-of-way does not adjoin or subsequently cross state submerged lands, or any designated shipping fairways/anchorage areas.

ATP agrees to be bound by the foregoing regulations, and further agrees to comply with the applicable stipulations as set forth in Title 30 CFR 250 (Subpart J) and that certain Letter to Lessees dated April 18, 1991.

In support of our application and for your review and use, the following maps, drawings and documents have been enclosed herewith and made a part hereof:

- 1. Originally signed copy of Nondiscrimination in Employment Stipulation;
- 2. Designated Oil & Gas Lease Operators and Right-of-Way Holders (Attachment A);
- 3. Plan and Profile Pipeline Route Map Pipeline and Umbilical (Sheet 1 of 1;
- 4. Pipeline Specifications & Calculations for the pipeline, flexible riser & rigid jumper;
- 5. Flexible Riser Details (Wellstream);
- 6. Production Lazy Wave Riser from the PLET to the FOI;
- 7. Production PLET General Arrangement
- 8. Umbilical Cross-section Drawing;
- Umbilical Lazy Wave Riser Drawing;
- 10. Subsea Umbilical Termination:
- 11. Subsea Infield Layout Schematic;
- 12. Safety Flow Schematic (Dwg. No. 166190W030);
- 13. Chemosynthetic Community Analysis by Fugro Geosciences, Inc.
- 14. MMS Pipeline Spreadsheet.
- 15. Check in the amount of \$2,380 covering the application fee of \$2,350 plus \$30 for the first year rental on 1.49 miles of right-of-way.

Minerals Management Service 6.895-Inch Bulk Oil Right-of-Way Pipeline Production Riser, Rigid Jumper and Associated Umbilical Mississippi Canyon Area Block 711 & 755 Offshore, Louisiana May 23, 2005

Page Five

Contact on technical points or other information:

Sharon DeSimoni
J. Connor Consulting, Inc.
16225 Park Ten Place, Suite 700
Houston, Texas 77084
(281) 578-3388
email address: sharon.desimoni@jccteam.com

ATP Oil & Gas Corporation hereby agrees to keep open at all reasonable times for inspection by the Minerals Management Service, the area covered by this right-of-way and all improvements, structures, and fixtures thereon and all records relative to the design, construction, operation, maintenance, and repairs, or investigations on or with regard to such area."

Please refer to your New Orleans Miscellaneous File No. 01819 for a copy of a resolution approved by the Board of Directors authorizing the undersigned to sign for and on behalf of ATP Oil & Gas Corporation. Additionally, ATP Oil & Gas Corporation has an approved \$300,000 Right-of-Way Grant Bond on file with MMS, covering installation of right-of-way pipelines in Federal Waters, Gulf of Mexico.

Sincerely,

Mickey W. Shaw

Vice President, Production Operations

Mickey W. SASW

MWS:GDR:SD

Attachments and Enclosures

cc: Nexen Petroleum U.S.A. Inc.

Mr. Larry D. McRae

12790 Merit Drive, Suite 800

Dallas, Texas 75251-1270

(Certified Mail No. 7003 2260 0003 0201 0929)

ATTACHMENT A

The following Designated Oil & Gas Lease Operators and Right-of-Way Holders have been furnished information regarding the proposed pipeline installation by Certified Mail, Return Receipt Requested. (Note: The status of blocks listed below is current, per research of https://www.consulting.consult

Mississippi Canyon Area

BLOCK 711

ATP Oil & Gas Corporation

OCS-G 14016

Oil & Gas Lease

BLOCK 755

Nexen Petroleum U.S.A. Inc.

OCS-G 24105

Oil & Gas Lease

NONDISCRIMINATION IN EMPLOYMENT

As a condition precedent to the approval of the granting of the subject pipeline right-of-way, the grantee, ATP Oil & Gas Corporation hereby agrees and consents to the following stipulation, which is to be incorporated into the application for said right-of-way.

During the performance of this grant, the grantee agrees as follows:

During the performance under this grant, the grantee shall fully comply with paragraphs (1) through (7) of section 202 of Executive Order 11246, as amended (reprinted in 41 CFR 60-1.4(a)), which are for the purpose of preventing discrimination against persons on the basis of race, color, religion, sex or national origin. Paragraphs (1) through (7) of section 202 of Executive Order 11246, as amended, are incorporated in this grant by reference.

Michey W. Stown Signature

23 May 2005

Date

T- SE BANK OF TEMAS -BAM ANGELO, N.A., - TIR YGELO, TEXAS TERCS

ATP OIL & GAS CORPORATION

4600 POST OAK PLACE, SUITE 200 HOUSTON, TEXAS 77027-9726

PAY

TO

THE

OF

ORDER

TWO THOUSAND THREE HUNDRED EIGHTY DOLLARS AND NO CENTS

Minerals Management Service

New Orleans, LA 70123-2394

1201 Elmwood Park Blvd.

CHECK MO DATE PAY SXACTLY

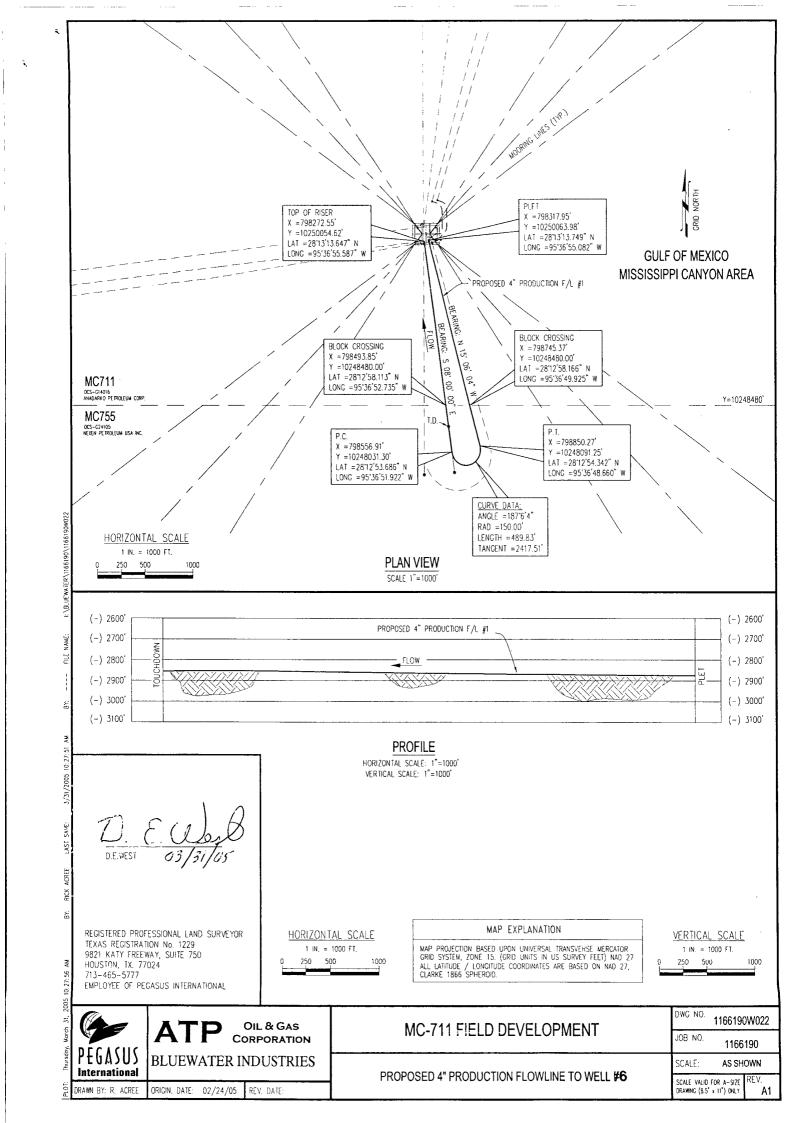
415720 05/18/05 *****2,380.00

VOID (FIT OF PRESENTED FOR PAYMENT WITHIN 180 DAYS

#415?20# #111300BBO#

"O6300050955"

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05-AP-4902 TOTAL INVO	20 051805 DICES PAID	05/17/05	2,380.00	0.	00	2,380.00 2,380.00



ATTACHMENT "B"

ATP OIL & GAS CORPORATION

WELL #6 PRODUCTION RISER AND FLOWLINE MISSISSIPPI CANYON AREA, BLOCK 711, PROPOSED GOMEZ PLATFORM THROUGH **MISSISSIPPI CANYON AREA, BLOCK 755**

PIPELINE SPECIFICATIONS

1. The company person to contact for information on technical points is as follows:

> Mr. Gregory D. Roland ATP Oil & Gas Corporation 4600 Post Oak Place Suite 200 Houston, Texas 77027-9726 Telephone: 713-622-3311

Fax: 713-403-7002

2. Production Flexible Riser and Jumper Description

Riser at MC-711 and Jumper and Well no 1, Proposed Gomez Platform

Riser Type

: Flexible Riser

Approx. Length

: 7141 ft.

Inner Diameter

: 4.00 in. ID

(Refer to Attached Data sheet for the 4.00 inch flexible riser properties)

3. Cathodic Protection System

> The flowline will be protected by the sacrificial anode system described below. Neoprene lined riser clamps and insulating flange kit at the top of the riser will insulate the riser from the platform cathodic protection system. The flowline end fittings will be protected by anodes on the PLET.

4. Water Depth

Minimum Water Depth

: 2940 ft

Maximum Water Depth

: 2980 ft

5. Description of Internal Protective Measures

Internal Coating

: None

Corrosion Inhibition Program

: To Be Determined

Pigging Requirements

: To Be Determined

The analysis of the transported products will be monitored and preventive measures, such as inhibitors and pigs, will be employed as necessary.

Appendix B 05/12/05 Page 1

ATTACHMENT "B"

ATP OIL & GAS CORPORATION

WELL #6 PRODUCTION RISER AND FLOWLINE MISSISSIPPI CANYON AREA, BLOCK 711, PROPOSED GOMEZ PLATFORM THROUGH MISSISSIPPI CANYON AREA, BLOCK 755

C. Flexible Riser Pipe and Jumper Pipe at MC-711 Proposed 'Gomez' Platform

Pipe inner diameter = 4"
Pipe overall diameter = 6.895"
Design Pressure = 7500 psi
Operating Pressure = 4000 psi
Design Temperature = 54.4 ° C
Operating Temperature = 48.0° C

Min. Bend Radius Storage = 3.73 ft Min. Bend Radius Service = 7.2 ft

Burst Pressure = 17,203 psi Collapse Pressure = 3,237 psi Max Allowable Depth = 7.282 ft Failure Tension = 439 kips

Stiffness:

Axial Tension at 20° C = 35588 kip Bending at 20° C = 6786 lbf ft2 Torsional at 20° C = 706 kip ft2

Weight of Pipe	Empty	Liquid Filled
In Air	38.1 lb/ft	44.2 lb/ft
In Seawater	21.5 lb/ft	27.6 lb/ft
Relative gravity in seawater	1.83	1.88

7. Specific Gravity of the Product

The anticipated specific gravity of the pipeline product (Bulk Oil and gas) is:

Gas SG	= 0.813 (Air = 1.0)
OiLSG	= 0.88

8. Design Capacity

The design capacity for the pipeline is 50 MMSCFD and 6,000 BOPD.

9. <u>Maximum Allowable Operating Pressure</u>

- a) Wall thickness and pressure calculations performed by flexible pipe manufacturer.
- b) Flanges, Valves and Fittings

All flanges, valves and fittings shall be the following: API 10,000#, 10,000 psig rated, 4 1/16" API Type 6BX.

ATTACHMENT "B"

ATP OIL & GAS CORPORATION

WELL #6 PRODUCTION RISER AND FLOWLINE MISSISSIPPI CANYON AREA, BLOCK 711, PROPOSED GOMEZ PLATFORM THROUGH MISSISSIPPI CANYON AREA, BLOCK 755

c) System MAOP

Maximum allowable operating pressure (MAOP) as determined in accordance with DOI, Title 30, Part 250, Code of Federal Regulations, as applicable, is 7500 psig for the 4-inch pipeline.

Hydrostatic Test Pressure (HTP) per CFR, Title 30, Part 250. The hydrostatic test pressure for the pipeline and riser will be based as given below:

Hydrostatic Test Pressure:

Pipeline & Riser

HTP = $1.25 \times 7500 \text{ psi (MAOP)} = 9375 \text{ psig, for minimum of 8 hours.}$

10. Design of the proposed flowline is in accordance with the "Oil and Gas and Sulphur Operations in the Outer Continental Shelf", Title 30, CFR, Part 250.

11. Construction Information

a) Anticipated start date : May 15, 2005
b) Method of construction : Reel Lay-barge
c) Method of burial : Not Required
d) Time required to lay pipe : Six (6) weeks
e) Time required to complete the project : Four (4) months

f) Shore base for construction : Amelia, La.

Wellstream Proprietary

Pegasus International DYNAMIC 4 in 7500 psi 3080 ft Bluewater-ATP MC711 Project Uninsulated Production Riser U. S. Units Pipe Data Sheet, B808-10-A01-040921-RQI Rev 1

Prepared by:		ecked by:	Approved by:			
Inside Diameter Design Pressure	4 in 7500 psl	Service S Conveyed Fluid o	Service Sweet dynamic d Fjuid oil/gas		Max. Fluid Temp. Water Depth	
Layer	Material	Strength	I.D.	Thick	O.D.	Weight
		[ksl]	[in]	[រក]	[ln]	[lbm/ft]
Flexbody	Stainless 316L		4.000	0.197	4.394	5.100
Flexberrier	PA 11(Natural)		4.394	0.236	4.866	1.564
Flex l ok	Carbon Steel	110	4.868	0.250	5.366	11.324
Fiextape 1	PA 11 P20 Tape, 30mll		5.366	0.060	5.486	0.464
Flextensile 1	Carbon Steel	190	5.486	0.157	5.800	7.840
Flextage 2	PA 11 P20 Tape, 30mil		5.800	0.060	5.920	0.501
Flextensile 2	Carbon Steel	190	5.920	0.157	6.234	8.432
Flextage 3	Polypropylene		6.234	0.023	6.280	0.184
Flextage 4	High Strength Glass File	ement	6.280	0.032	6.344	0.358
Flextape 5	Polypropylene		6.344	0.023	6.391	0.187
Flextage 6	Fabric	:	6.391	0.016	6.423	0.093
Flexshleld	Rubber Modified Polypropylene (Black)		6.423	0.236	6.895	2.014
Layer	Raw Material Di	mensions	Mfg Pitch	Wires	Angle	Filled
Flexbody	36.0mm x 1.0mm	1.417in x 0.039in			87.8	90.24%
Flexiok	14.4mm x 6.4mm	0.565in x 0.250in			88.6	91.49%
Fiextensile 1	8.0mm x 4.0mm	0.315in x 0.157in	18.36in	36	44.0	91.47%
Flextensile 2	8.0mm x 4.0mm	0.315ln x 0.157in	21.20ln	40	42.0	91.17%
Outside Diameter		6.895 in	Wt, Empty in Air			38.1 lb/
Storage Radius,	SBR	3.73 n	S/W filled in Air			44.2 lb/
Operating Radius	s, OBR	7.2 ft	Air filled in S/W			21.5 lb/
Bending Stiffness	s, El	6786 lbf ft*	S/W filled in S/W			27.8 lb/
Spooling Tension		487 lbf	Burst Pressure			17203 ps
Therm. Cond./Length, C/L		2.86 BTU/hift*F	Burst/Design Ratio			2.2
Effective Thermal Cond, ke		0.25 BTU/hiff*F	Collapse Pressure (Wat Collapse)		i Coliapse)	3237 ps
OHTC, Uo (based on ID)		2.73 BTU/hrit* F	Collapse Depth			7282
SWDR with bore empty		3.113 lbffft in	Collapse/Design ratio			2.3
SWDR with bore filled by SW		3.996 lb0ft in	Fallure Ten	sion		438969 Ib
Pipe torsional sti	ffness (GJ) at 20 °C:					
Limp direction		708 Kip ft²				
Stiff direction		1492 Kip ft*				
Axial Stiffness		35588 Kip				

Wellstream Proprietary

Pegasus International DYNAMIC 101.8 mm 51.711 MPa 938.8 m Bluewaier-ATP MC711 Project Uninsulated Production Riser S.I. Units Pipe Data Sheet, B808-10-A01-040921-RQI Rev 1

Design Pressure 51. Layer Material Mat	atural)	Service S Conveyed Fluid of Strength [MPa]	Sweet dynamic bil/gas I.D. Imml	Mex. Thick	Fiuld Temp. Water Depth	54.4 °C 938.8 m
Flexbody Stainless Flexbarrier PA 11(Na Flexlok Carbon S Flextape 1 PA 11 PA Flextape 1 Carbon S Flextape 2 PA 11 PA Flextape 2 PA 11 PA Flextape 2 PA 11 PA Flextape 3 Polyprop Flextape 4 High Stre Flextape 5 Polyprop Flextape 6 Fabric	: 316L atural)	• •		Thick		
Flexbarrier PA 11 (Na Flextape 1 PA 11 PZ Flextape 1 PA 11 PZ Flextape 2 PA 11 PZ Flextape 2 PA 11 PZ Flextape 3 Polyprop Flextape 4 High Stra Flextape 5 Polyprop Flextape 6 Fabric	atural)	[MPa]	[mm]		O.D.	Weight
Flexbarrier PA 11 (Na Flextape 1 PA 11 PZ Flextape 1 PA 11 PZ Flextape 2 PA 11 PZ Flextape 2 PA 11 PZ Flextape 3 Polyprop Flextape 4 High Stra Flextape 5 Polyprop Flextape 6 Fabric	atural)		ស្រែបហ៊	[mm]	[mm]	[kg/m]
Flextok Carbon S Flextape 1 PA 11 PA Flextapeile 1 Carbon S Flextape 2 PA 11 PA Flextape 2 PA 11 PA Flextape 3 Polyprop Flextape 4 High Stra Flextape 5 Polyprop Flextape 6 Fabric			101.60	5.00	111.60	7.590
Flextape 1 PA 11 PA Flextape 2 PA 11 PA Flextape 2 PA 11 PA Flextape 3 Polyprop Flextape 4 High Stre Flextape 5 Polyprop Flextape 6 Fabric	taal		111.60	6.00	123.60	2.328
Flextansile 1 Carbon S Flextape 2 PA 11 P2 Flextansile 2 Carbon S Flextape 3 Polyprop Flextape 4 High Stre Flextape 5 Polyprop Flextape 6 Fabric	, to co	758	123.60	6.35	136.30	16.853
Flextape 2 PA 11 PZ Flextensile 2 Carbon S Flextape 3 Polyprop Flextape 4 High Stre Flextape 5 Polyprop Flextape 6 Fabric	20 Tape, 30mi		136.30	1.52	139.34	0.691
Flextensile 2 Carbon S Flextape 3 Polyprop Flextape 4 High Stre Flextape 5 Polyprop Flextape 6 Fabric		1310	139.34	3.99	147.32	11.668
Flextape 3 Polyprop Flextape 4 High Stre Flextape 5 Polyprop Flextape 6 Fabric	20 Tape, 30mi	•	147.32	1.52	150.36	0.746
Flextape 3 Polyprop Flextape 4 High Stre Flextape 5 Polyprop Flextape 6 Fabric	• •	1310	150.36	3.99	158.33	12.549
Flextape 4 High Stre Flextape 5 Polyprop Flextape 6 Fabric		:	158,33	0.59	159.52	0.274
Flextape 5 Polyprop Flextape 6 Fabric	angth Glass Fi	lament	159.52	0.81	161.14	0.532
Flextape 6 Fabric		,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	161.14	0.59	162.32	0.279
	y10110		162.32	0.41	183.14	0.139
Flexshield Rubber I	Modified Polyp	ropylene (Black)	163.14	6.00	175.14	2.997
Layer R	taw Meteriai I	Dimensions	Mfg Pitch	Wires	Angle	Filled
	x 1.0mm	1.417in x 0.039in			87.8	90.24%
Flexiok 14.4mm	x 6.4mm	0.585ln x 0.250ln			88.6	91.49%
Flextensile 1 8.0mm	x 4.0mm	0.315in x 0.157in	466.3mm	36	44.0	91.47%
Flextensile 2 8.0mm	x 4.0mm	0.315ln x 0.157in	538.5mm	40	42.0	91.17%
Outside Diameter		175.1 mm	Wt, Empty	in Air		56.6 kg/m
Storage Radius, SBR		1.14 m	S/W filled in Air		65.7 kg/m	
Operating Radius, OBR		2.2 m	Air filled in S/W		31.9 kg/m	
Bending Stiffness, El		2.804 kNm²	S/W filled in S/W		41 kg/m	
Spooling Tension		2168 N	Burst Pressure		118.61 MPs	
Therm. Cond./Length, C/L		4.9 w/m°C	Burst/Design Ratio		2.29	
Effective Thermal Cond, ke		0,4 w/m°C	Collapse Pressure (Wet Collapse)		22.32 MPs	
OHTC, Uo {based on ID}		15.5 w/m³°C	Collapse Depth		2219 m	
SWDR with bore empty		1.79 N/m mm	Collapse/Design ratio		2.36	
SWDR with bore filled by	sw	2.3 N/m mm	Failura Tension			1952.6 kN
Pipe torsional stiffness (G						
•	· , 2. 2. 3.	292 kNm²				
Stiff direction	Limp direction					
Axiai Stiffness		616 kNm²				

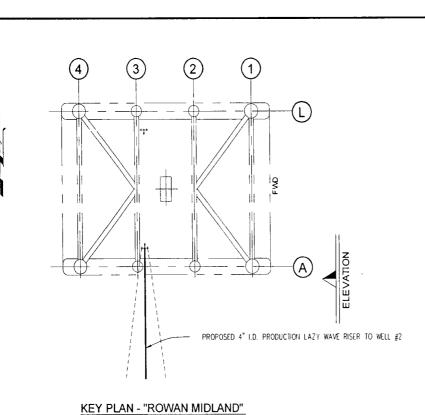
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Wellstream Proprietary

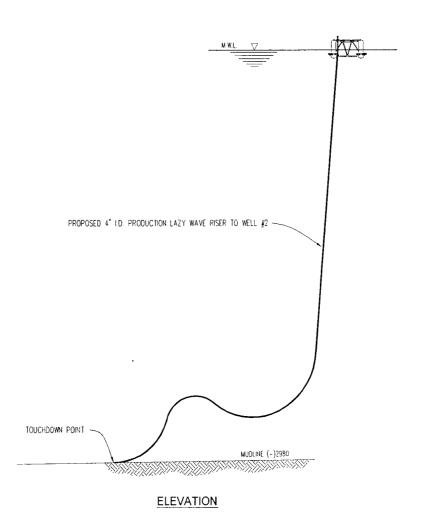
Pegasus International DYNAMIC 101.8 mm 51.711 MPs \$38.8 m Bluewater-ATP MC711 Project Uninsulated Production Riser Customer Pipe Data Sheet: 8808-10-A01-040921-RQI Rev 1

Prepared by:	Checked by:	Approved by:	
inside Diameter	101.60 mm	4.00 in Conveyed Fluid	oiVgas
Outside Diameter	175.14 mm	6.895 in Burst/Design Ratio	2.29
Water Depth	938.8 m	3080 ft Collapse/Design Ratio	2.36
Fluid Temperature	54.4 °C	130 ° F	

Design Pressure	51.71 MPa	7500 psi
Factory Test Pressure	77.57 MPa	11250 psl
Burst Pressure	118.61 MPa	17203 pai
Collapse Pressure (Wet Collapse)	22.32 MPa	3237 pai
Collapse Depth	2219 m	7282 ft
Fallure Tension	1953 kN	438969 lbf
Storage Bend Radius	1,14 m	3.73 ft
Operating Bend Radius	2.2 m	7.2 ft
Bending Stiffness	2.8 kNm²	6786 lbf R 3
Weight Empty in Air	58.85 kg/m	38.1 lb/ft
S/W filled in Air	65.7 kg/m	44.2 lb/ft
Air filled in S/W	31.9 kg/m	21.5 lb/ft
S/W filled in S/W	41 kg/m	27.6 lb/ft
Thermal Cond./Unit Length	4.95 w/m°C	2.86 BTU/hrft*F
OHTC, Uo (based on ID)	15.5 w/m ^{2*} C	2.73 BTU/hrtt ^{as} F
Pipe torsional stiffness (GJ) at 20 °C:	•	
Limp direction	292 kNm²	706 Kip ft⁴
Stiff direction	616 kNm²	1492 Klp ft ^a
Axial Stiffness	158304 kN	35588 Kip



SCALE: N.T.S.





OIL & GAS CORPORATION **BLUEWATER INDUSTRIES**

MC-711 FIELD DEVELOPMENT

1166190W021 JOB NO. 1166190

SCALE:

DRAWN BY: R. ACREE

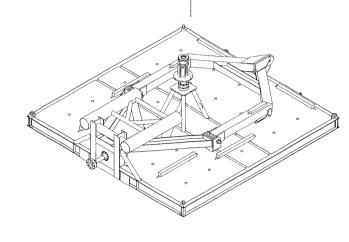
ORIGIN. DATE: 02/23/05

REV. DATE: 03/22/05

PROPOSED 4" I.D. PRODUCTION LAZY WAVE RISER TO WELL #6

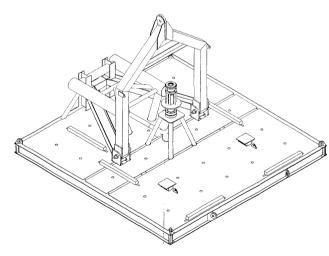
SCALE VALID FOR A-SIZE DRAWING (8.5" x 11") ONLY





PLET ISOMETRIC VIEW

SCALE: 1/2" = 1'-0"



PLET ISOMETRIC VIEW - YOKE AT 90° SCAE: 1/2" = 1'-0"

DRAWN BY: LL

DATE: 03/29/2005 CHECKED BY: MW DATE: 04/04/2005

APPROVED BY: DWF

DATE: 05/05/2005

PLOT SCALE: 1:1 SCALE: AS SHOWN SCALE WAS FOR DISCUSSION.

NO.	DATE	BY	REVISION DESCRIPTION	ENGINEER'S STAN
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				1
				1
0	05/05/2005	LL/MW	APPROVED FOR CONSTRUCTION	1
Al	04/04/2005	CDN/MW	APPROVED FOR TENDER	1
A			ISSUED FOR APPROVAL	1
H 167	DESMITCH PROVIDED	ON THE DAME	INC IS NOT TO BE ACCOMPAND AS MAJOR UNLISS AN ORDINAL PROFESSIONAL INCINCEPTS AND THE SHAP IS ACCOMPANDED AS THE DISCOURT DATE AND SCHOOLINE OF THE DISCOURT	1

ATP CORPORATION BLUEWATER INDUSTRIES

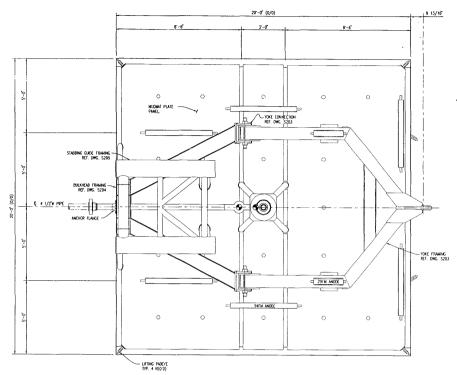
4" PRODUCTION PLET DESIGN PEGASUS

GENERAL ARRANGEMENT

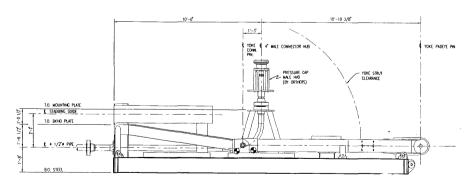
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MISSISSIPPI CANYON 711

International 1166865S201



PLET PLAN VIEW
SCALE: 1/2" = 1'-0"



PLET ELEVATION
SCALE: 1/2' = 1'-0'

PROPOSAL DRAWING

(10) .625" O.D. X .065" WALL -NITRONIC 19D ALLOY TUBES WITH EXTRUDED ZINC JACKET .685" DIA.

WIRE FILLERS WITH -HDPE JKT., .230" DIA.

MYLAR TAPE WRAP THEN GLASS REINFORCED TAPE .685" ZINC FILLERS (2) REQUIRED .188" DIA. GALV. STEEL

.250" WALL HDPE JACKET -4.040" FINISHED DIAMETER (1) 2.00" O.D. X .125" WALL X90C CARBON STEEL TUBING COLOR: YELLOW WITH BLACK

TUBING HYDRAULIC PROPERTIES

TORQUE STRIPE

TUBING SIZE	WORKING PRESSURE	TEST PRESSURE	BURST PRESSURE
.625" X .065" WALL	10,000 PSI	12,500 PSI	25,200 PSI
2.00" X .125" WALL	7,600 PSI	9,500 PSI	

NITRONIC 19D TUBING MANUFACTURED TO SEACAT SPECIFICATION SC80-1, REV. 12

NITRONIC 19D TUBING PER ASTM A-450 ZINC CLADDING PER ASTM B-6

TUBING SIZES INDICATED ARE OUTSIDE DIA'S. DIAMETER TOLERANCE : +/- .005"

DIAMETER/WEIGHT RATIO : $\frac{4.04"}{8.96} = .45$

MECHANICAL PROPERTIES

FBE COATING TO 2.14" DIA.

FINISHED O.D. : 4.04"

WEIGHT IN AIR : 13.81 LBS./FT. (TUBING EMPTY)

WEIGHT IN AIR : 14.67 LBS./FT.

(TUBING FILLED)

WEIGHT IN SEAWATER: 8.10 LBS./FT. (TUBING EMPTY)

WEIGHT IN SEAWATER: 8.96 LBS./FT. (TUBING FILLED)

SPECIFIC GRAVITY (FILLED): 2.57 IN SEAWATER

CALCULATED BREAK STRENGTH: 160,000 LBS.

MAXIMUM WORKING LOAD : 125,000 LBS.

MINIMUM BEND DIAMETER STATIC: 140"

MINIMUM BEND DIAMETER INSTALLATION: 190"

APPROX. BENDING STIFFNESS: 2,170 KIP-IN(2)

APPROX. AXIAL STIFFNESS : 78.800 KIP

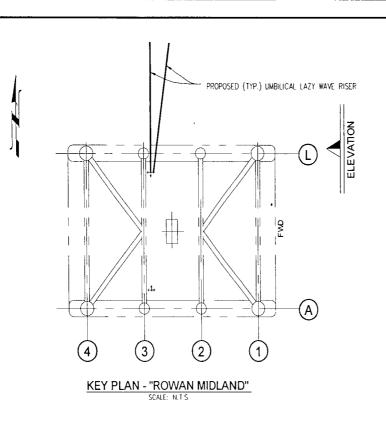
CABETT SUBSEA PRODUCTS

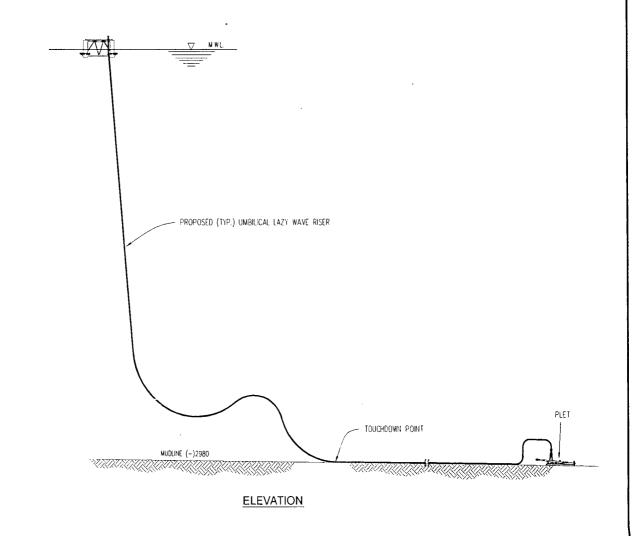


6827 SIGNAT DRIVE HOUSTON, TEXAS 77041

ATP BLUEWATER MISSISSIPPI CANYON 711 STEEL TUBE HYDRAULIC CONTROL UMBILICAL **DESIGN SPECIFICATION**

DATE 8/16/04 DWG NO CSP-1135 REV. SHEET 1 OF 1







2005 9:30:00 AM

OIL & GAS CORPORATION **BLUEWATER INDUSTRIES**

MC-711 FIELD DEVELOPMENT

DWG NO. 1166190W020 J08 NO. 1166190 1"=750"

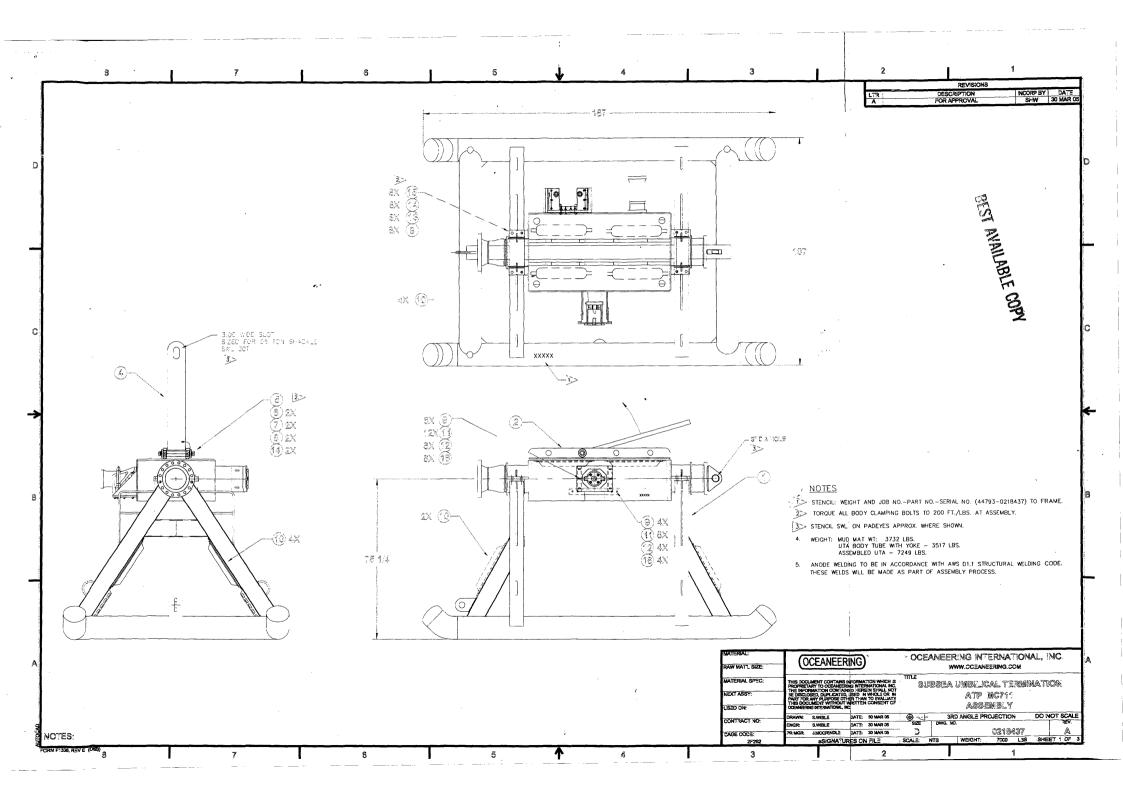
PROPOSED (TYP.) UMBILICAL LAZY WAVE RISER

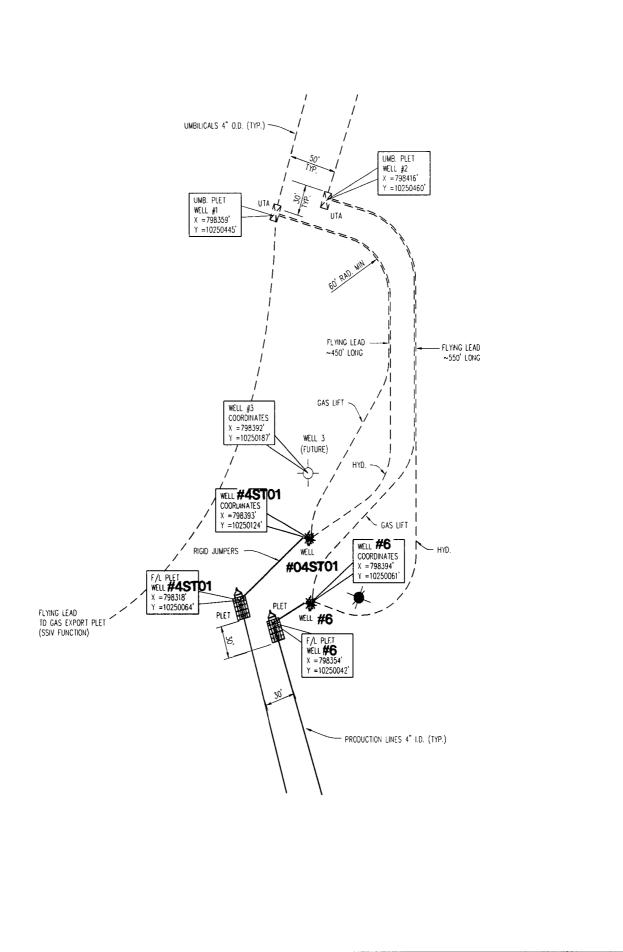
SCALE VALID FOR A-SIZE REV. DRAWING (8.5" x 11") ONLY.

DRAWN BY: P. ACPEE

ORIGIN DATE: 02/23/05

REV. DATE







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3/16/2005 9:49:45 AM

LAST SAVE:

RICK ACREE .: H

Friday, March 18, 2005 9:29:51 AM

OIL & GAS CORPORATION **BLUEWATER INDUSTRIES**

MC-711 FIELD DEVELOPMENT

DWG NO. 1166190W025 J08 NO. 1166190

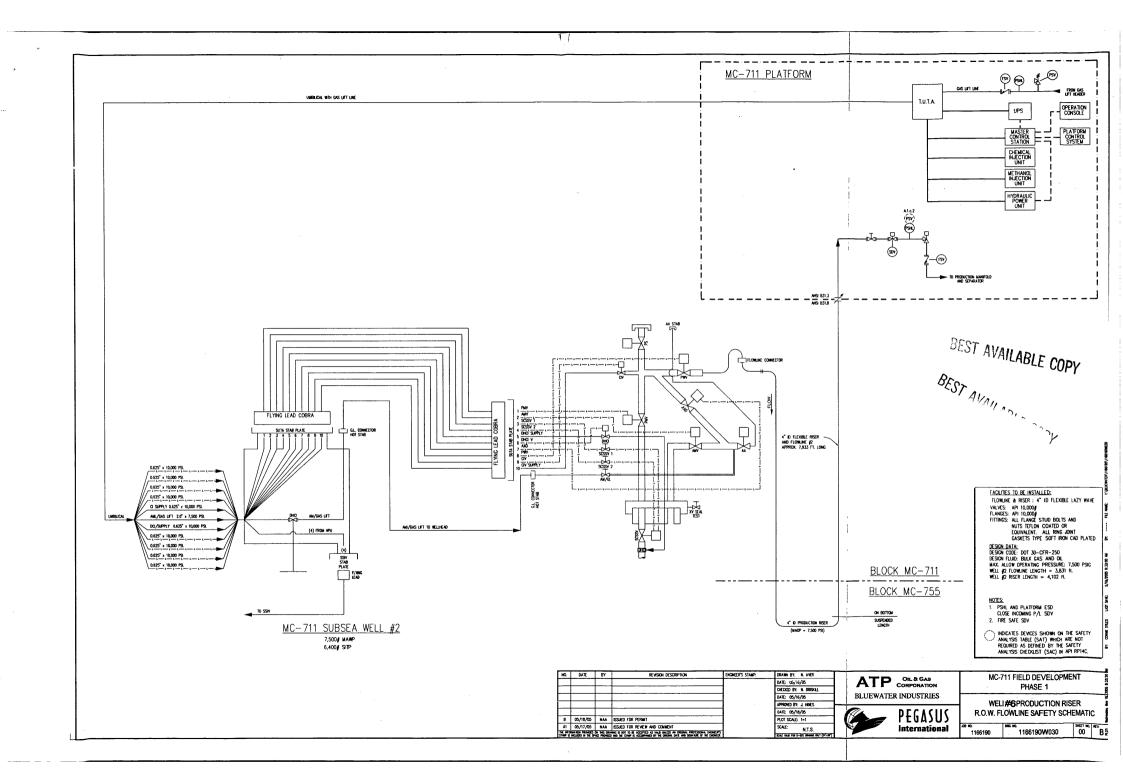
AS SHOWN

SUBSEA INFIELD LAYOUT

SCALE VALID FOR A-SIZE DRAWING (8.5" x 11") ONLY.

DRAWN BY: R. ACREE

ORIGIN. DATE: 02/24/05 REV. DATE:



FUGRO GEOSERVICES, INC.



Letter Report No. 2404-2081 April 13, 2005

ATP Oil & Gas Corporation 4600 Post Oak Place Houston, Texas 77027-9726

Attention: Robert M. Shivers III

6100 Hillcroft (77081) P.O. Box 740010 Houston, Texas 77274 Tel: (713)369-5800 Fax: (713)369-5811

Chemosynthetic Community Analysis
Gomez Development
Mississippi Canyon Blocks 711 and 755
Gulf of Mexico

Purpose and Scope

Submitted here is our analysis of the potential for disturbance of chemosynthetic communities in the vicinity of the proposed FPU (Floating Production Unit) mooring spread for the Gomez development in Mississippi Canyon Blocks 711 and 755 (OCS-G-14016 and 14017). The purpose of this analysis is to meet the requirements of MMS NTL No. 2000-G20, "Deepwater Chemosynthetic Communities" (Minerals Management Service, 2000) for deepwater development. This work was requested and authorized by ATP's Mr. Robert Shivers III via email dated 31 March 2005.

The scope of this study was limited to chemosynthetic analysis of the available pre-drilling geohazards ("site-survey"), 3-D exploration seismic, and geotechnical data. Assessment of any geohazards that may be present was beyond the scope of this study. Similarly, infrastructure, wellheads, debris, shipwrecks, and any other man-made features that may be present have not been investigated and are not shown on the map that accompanies this report.

Mooring Design

The proposed taut mooring system consists of four groups of three SEPLA anchors (Suction-Embedded PLate Anchors) each (Plate C-1). The anchor lines would include chain, extending 600 ft from each anchor, connected to poly line, which would extend to the FPU. The first 100 ft of chain from the anchor would be buried below the seafloor. The proposed anchor coordinates are as follows:

ANCHOR	WATER DEPTH	COORDINATES (I	NAD27; UTM16; FEET)
	(ft)		40.047.404
A1	~2,992	802,533	10,247,134
A2	~2,963	801,981	10,246,447
A3	~2,947	801,301	10,245,873
A4	~2,897	795,272	10,245,855
A5	~2,898	794,583	10,246,425
A6	~2,900	794,013	10,247,107
A7	~2,936	794,030	10,253,130
A8	~2,944	794,600	10,253,807
A9	~2,961	795,290	10,254,367
A10	~3,019	801,280	10,254,344
A11	~3,024	801,958	10,253,778
A12	~3,037	802,515	10,253,101
FPU	~2984	798,293	10,250,124



Plate C-1 shows in red the 500-ft maximum portion of each mooring chain that would lie on (or, within 100 ft of the anchor, below) the seafloor during the worst-case (that is, hurricane) conditions. The remaining 100 ft of chain and all of the poly line would always be above the seafloor in the water column, even during worst-case conditions. In practice, only the chains on the lee side of the spread would lie on the seafloor during a hurricane. Because it is a taut mooring system, the chains would not lie on the seafloor (except for the 100 ft of chain nearest to the anchor, which would always be buried) during installation or during normal (non-hurricane) operating conditions.

Data Used, Interpretive Methodology, and Mapping Criteria

1993 Pre-drilling Geohazards Data. A pre-drilling geohazards survey was done in 1993 by Kinsella, Cook & Associates covering MC Blocks 711 and 755. The grid surveyed was the standard 300 m by 900 m grid required by the MMS. Data collected included echo sounder, 3.5 kHz subbottom profiler, and analog FPUker data (no side-scan-sonar data were collected at this deepwater site). Because of the deepwater and analog data format, only the 3.5 kHz subbottom profiler (SBP) data were useful for this study. Overall, the quality of the SBP data is as good as can be expected when using near-sea-surface-deployed transducers at this deepwater site, and generally the quality is judged to be adequate for chemosynthetic community analysis.

2004 Pipeline Survey Data. In 2004 Fugro carried out a pipeline route survey between MC Block 711 and Grand Isle Block 115 using a deeptow system. Multibeam bathymetric, side-scan sonar, and subbottom profiler data were collected. The survey grid consisted of 5 parallel lines that run east-west and more-or-less straddle the boundary between blocks 711 and 755. Line spacing varies between about 850 and 1200 ft. Consequently, this data set covers only part of the anchor spread. However, all side-scan and SBP data were reviewed in the workstation as part of the chemosynthetic analysis. All of these data are judged to be of good quality.

3-D Exploration Seismic Data. A 3-D exploration seismic data volume was made available by ATP for this chemosynthetic analysis. The 3-D data coverage is shown on Plate C-1. Bin spacing is 87.5 by 87.5 ft. Although the 3-D data is of much lower vertical resolution than the SBP data, is does give useful bathymetric details, shows seafloor amplitude variations that helped to identify potential seep zones, and shows some hydrocarbon source zones. For 3-D exploration seismic data, the quality is judged to be generally good.

2005 Geotechnical Data. A jumbo piston core and a seafloor-deployed cone penetrometer test were done near the center of each of the four anchor clusters. In addition, one deep (130 ft BML) rotary boring and one seafloor-deployed cone penetrometer test were done at the center of the proposed anchor layout. This work was done in early 2005 (Fugro-McClelland, 2005a and 2005b). Data quality is very good.

Interpretive Methodology. To facilitate interpretation, the 3-D exploration seismic and deeptow data were loaded onto a PC-based workstation running SMT's Kingdom suite of interpretation software. In addition, selected lines of the 1993 analog geohazards data in the vicinity of proposed anchors were converted into SEG-Y format and also loaded onto the workstation, along with the available geotechnical data. We also reviewed all analog paper records of the 1993 SBP data. Our chemosynthetic analysis discussed here and results presented on the accompanying map were based on using and integrating all of these data.

Results of the 1993 survey as shown on the "Seafloor Features Map" included in the geophysical survey report prepared by Kinsella, Cook & Associates (1993) were supplemented and modified somewhat based on interpretation of the additional deeptow and 3-D exploration seismic data now available. Specifically, the outlines of some of the areas interpreted as possible seeps were modified from the 1993 interpretation, and some possible seeps not mapped in 1993 were added. The faults shown on Plate C-1 were copied without modification from the 1993 map.



Water depth contours shown on Plate C-1 were generated from the 3-D seismic data using the generic Advocate & Hood (1993) velocity function. Water depths are approximate and are estimated to be accurate within ±20 ft where the seafloor is flat and featureless. Depths may be less accurate elsewhere.

Mapping Criteria. Interpretation and mapping of features (possible seeps) that could support dense communities of chemosynthetic organisms were based on geomorphology, acoustic character, or a combination of the two (wipe-out zones, "gas chimneys", anomalously high amplitudes, seafloor mounds, disturbed seafloor seen on side-scan sonar data, etc.). Possible seeps were interpreted and mapped as shown on the Water Depth and Seafloor Features Map (Plate C-1) using all available subbottom profiler, side-scan sonar, and 3-D seismic data. All seep boundaries are interpretive, and actual boundaries may be somewhat different. Mapping scale was 1:12,000 (1" = 1,000 ft). Only those high-resolution tracklines that pass near possible seeps in the vicinity of the proposed anchor spread are shown on the map (Plate C-1).

Chemosynthetic Analysis

Principal Results. The principal results of our analysis show that there are several possible seafloor hydrocarbon seeps in the general vicinity of the proposed mooring spread (Plate C-1). No proposed anchor locations are within areas identified as possible seeps. Proposed locations for Anchors A-2 and A-3 are both within 450 ft of a relatively small area interpreted as a possible seep (possible seep 2 on Plate C-1), and the anchor chain for Anchor A-2 could lie on the seafloor across this same possible seep during worst-case (hurricane) conditions. The anchor chains for Anchors A-1 and A-3 could lie on the seafloor about 450 ft from possible seep 2 during worst-case (hurricane) conditions. The poly lines for Anchors A-2 and A-3 would always be in the water column in the vicinity of the nearby possible seep 3. Similarly, the poly line for Anchor A-12 would always be in the water column where it passes closest to possible seep 1.

Our judgment is that it is unlikely that there are dense chemosynthetic communities at the small possible seeps (possible seeps 2 and 3) near the locations proposed for anchors A-2 and A-3 and their associated anchor lines. Dense communities may populate the large possible seep (possible seep 1) past which the line for proposed Anchor A-12 would pass. However, the poly line for Anchor A-12 would always be well-up in the water column where it passes closest to possible seep 1.

Discussion of Possible Seeps. Many of the possible seeps in the study area, and all possible seeps within 500 ft of proposed anchor locations, are relatively small, are not always well-defined even on the high-resolution survey data, and cannot be detected using the 3-D seismic data. The notable exception is the large possible seep between proposed Anchors A-1 and A-12 (possible seep 1). All seismic data that images this feature suggest that it is a large, active, deep-seated seep.

None of the possible seeps, including possible seep 1 between Anchors A-1 and A-12, appear to be associated with deep-seated faults that could act as hydrocarbon migration pathways. All seafloor or near-seafloor faults in the area are relatively short, have small offset, and extend downward only to shallow depths. Most are slump faults that have resulted from differential consolidation and movement of shallow strata. Virtually all faults shown on Plate C-1 northeasterly of the proposed anchor spread are slump faults that toe-out within shallow buried landslide deposits that underlie this large area. We cannot determine conclusively from the available data if these faults are now active and continue to undergo slow differential offset, or if they are now stabilized. We found no evidence for leaking hydrocarbons associated with any of the faults.

The origin of the hydrocarbons that may be seeping out of the seafloor is uncertain. However, with one clear exception, possible seeps appear to overlie and be sourced from relatively small, local accumulations of hydrocarbons typically between ~500 and ~1200 ft BML rather than from deep reservoirs. These accumulations are generally seen as relatively small, scattered, isolated "bright spots", which are common on the 3-D seismic data in this interval. The notable exception is possible seep 1



between proposed Anchors A-1 and A-12, which appears to have a migration pathway that extends downward for thousands of feet.

If any of the seeps are actively venting adequate volumes of hydrocarbons, then they could support a dense community of chemosynthetic organisms. However, the data available does not allow us to conclusively determine if the seeps are active or not. Further, geophysical data alone is not capable of indicating the presence or absence of chemosynthetic organisms even if the seeps are active. None of the geotechnical sampling was done at possible seep sites.

Proposed Anchor Location A-1. Possible hydrocarbon seeps or other areas or features that could support high-density chemosynthetic communities are not located within 500 ft of any seafloor disturbances that would result from installation of Anchor A-1 at the proposed location. About 500 ft northwest of Anchor A-1, the anchor chain for Anchor A-1 would be within ~450 ft of the edge of possible seep 2 (Plate C-1). However, dense communities of chemosynthetic organisms are not expected at this possible seep because of its small areal size (~1050 ft by ~400 ft; ~6.9 acres), no clear seafloor expression, no associated deep-seated fault, and minimal acoustic signature on subbottom profiler data (it is not identifiable on the 3-D seismic data).

Proposed Anchor Location A-2. The proposed location for Anchor A-2 is ~80 ft east of possible hydrocarbon seep 2. For a distance of ~400 ft immediately northwest of Anchor A-2, the chain for Anchor A-2 could lie on the seafloor across this possible seep during worst-case (hurricane) conditions (Plate C-1). However, dense communities of chemosynthetic organisms are not expected at this possible seep because of its small areal size (~1050 ft by ~400 ft; ~6.9 acres), no clear seafloor expression, no associated deep-seated fault, and minimal acoustic signature on subbottom profiler data (it is not identifiable on the 3-D seismic data). The poly line for Anchor A-2 would always be in the water column in the vicinity of the nearby possible seep 3.

Proposed Anchor Location A-3. The proposed location for Anchor A-3 is ~450 ft southwest of possible hydrocarbon seep 2 described above. And, the anchor chain for Anchor A-3 would pass as close as ~450 ft to this possible seep zone (Plate C-1). However, dense communities of chemosynthetic organisms are not expected at this possible seep because of its small areal size (~1050 ft by ~400 ft; ~6.9 acres), no clear seafloor expression, no associated deep-seated fault, and minimal acoustic signature on subbottom profiler data (it is not identifiable on the 3-D seismic data). The poly line for Anchor A-3 would always be in the water column in the vicinity of the nearby possible seep 3.

Proposed Anchor Location A-4. Possible hydrocarbon seeps or other areas or features that could support high-density chemosynthetic communities are not located within 500 ft of any seafloor disturbances that would result from installation of Anchor A-4 or its associated anchor line at the proposed location.

Proposed Anchor Location A-5. Possible hydrocarbon seeps or other areas or features that could support high-density chemosynthetic communities are not located within 500 ft of any seafloor disturbances that would result from installation of Anchor A-5 or its associated anchor line at the proposed location.

Proposed Anchor Location A-6. Possible hydrocarbon seeps or other areas or features that could support high-density chemosynthetic communities are not located within 500 ft of any seafloor disturbances that would result from installation of Anchor A-6 or its associated anchor line at the proposed location.

Proposed Anchor Location A-7. Possible hydrocarbon seeps or other areas or features that could support high-density chemosynthetic communities are not located within 500 ft of any seafloor disturbances that would result from installation of Anchor A-7 or its associated anchor line at the proposed location.

Proposed Anchor Location A-8. Possible hydrocarbon seeps or other areas or features that could support high-density chemosynthetic communities are not located within 500 ft of any seafloor



disturbances that would result from installation of Anchor A-8 or its associated anchor line at the proposed location.

Proposed Anchor Location A-9. Possible hydrocarbon seeps or other areas or features that could support high-density chemosynthetic communities are not located within 500 ft of any seafloor disturbances that would result from installation of Anchor A-9 or its associated anchor line at the proposed location.

Proposed Anchor Location A-10. Possible hydrocarbon seeps or other areas or features that could support high-density chemosynthetic communities are not located within 500 ft of any seafloor disturbances that would result from installation of Anchor A-10 or its associated anchor line at the proposed location. All seafloor or near-seafloor faults in the vicinity of proposed anchor location A-10 (Plate C-1) are small-offset slump faults that extend downward only to shallow depths. We found no evidence for leaking hydrocarbons associated with these faults.

Proposed Anchor Location A-11. Possible hydrocarbon seeps or other areas or features that could support high-density chemosynthetic communities are not located within 500 ft of any seafloor disturbances that would result from installation of Anchor A-11 or its associated anchor line at the proposed location. All seafloor or near-seafloor faults in the vicinity of proposed anchor location A-11 (Plate C-1) are small-offset slump faults that extend downward only to shallow depths. We found no evidence for leaking hydrocarbons associated with these faults.

Proposed Anchor Location A-12. Possible hydrocarbon seeps or other areas or features that could support high-density chemosynthetic communities are not located within 500 ft of any seafloor disturbances that would result from installation of Anchor A-12 at the proposed location. All seafloor or near-seafloor faults in the vicinity of proposed anchor location A-12 (Plate C-1) are small-offset slump faults that extend downward only to shallow depths. We found no evidence for leaking hydrocarbons associated with these faults. The poly line for Anchor A-12 would always be well-up in the water column where it passes closest to possible seep 1.

Conclusions

We conclude that the proposed mooring spread is unlikely to disturb dense communities of chemosynthetic organisms. This is because both of the possible seeps within 500 ft of proposed anchor or on-bottom anchor-line locations (that is, possible seeps 2 and 3) are relatively small and do not appear to have a deep-seated "reservoir" origin that would probably be required to provide adequate rates of hydrocarbon seepage necessary to support dense chemosynthetic communities.

Closing

We appreciate the opportunity to work with you on this project and look forward to working with you again as your site investigation consultants. If you have any questions concerning this report, please contact me at (713) 369-5805 or via email at kcampbell@fugro.com.

Sincerely,

FUGRO GEOSERVICES, INC.

Kerry J. Campbell, P.G.

Manager, Geoscience Consulti

713-369-5805 kcampbell@fugro.co

Kerry J. Campbell Geology



REFERENCES

Advocate, D.M. and Hood, K.C., (1993), "An Empirical Time-Depth Model for Calculating Water Depth, Northwest Gulf of Mexico", in <u>Geo-Marine Letters</u>, Bouma, A.H., editor, Volume 13, p. 207-211.

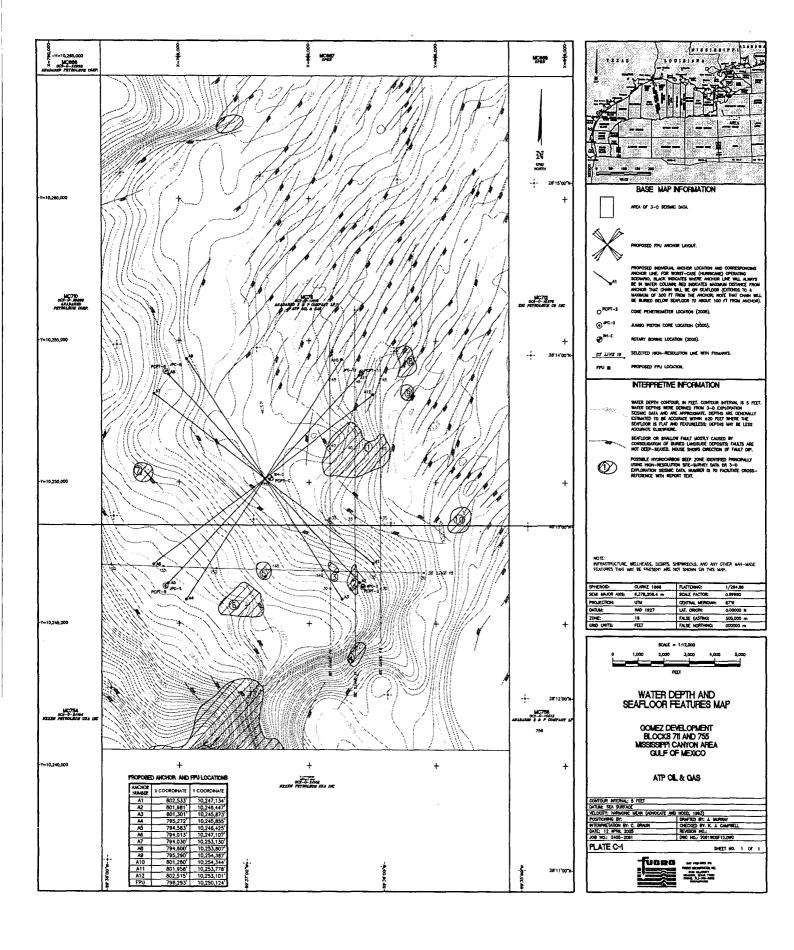
Fugro GeoServices, Inc., (2004), "Archeological, Engineering, and Hazard Survey of Proposed 8" Oil and 10" Gas Export Pipelines from Mississippi Canyon Area Block 711 to Grand Isle Area Block 115", deeptow survey report done for ATP Oil & Gas Corporation c/o Bluewater Industries (Report Number 2404-5005, 16 November 2004).

Fugro-McClelland Marine Geosciences, Inc., (2005a), "Geotechnical Investigation, Gomez Prospect, Blocks 711 & 755, Mississippi Canyon Area, Gulf of Mexico", field report on jumbo piston coring and PCPT testing done for ATP Oil & Gas Corporation (Field Report No. 0201-5420, 18 February 2005).

Fugro-McClelland Marine Geosciences, Inc., (2005b), "Addendum to the Geotechnical Investigation, Gomez Prospect, OCS-G-14016, Boring BH-C, Block 711, Mississippi Canyon Area, Gulf of Mexico", for ATP Oil & Gas Corporation (Field Report No. 0201-54207, addendum letter dated 7 March 2005).

Kinsella, Cook & Associates, Inc., (1993), "Geophysical Survey Report, Blocks 711 and 755, Mississippi Canyon Area, Offshore Louisiana, OCS-G-14016 and 14017", pre-drilling geohazards report done for Union Pacific Resources Company (13 September 1993).

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Complete one form for the pipeline segment submitted in your application. A ROW					<u> </u>		
application may only contain one proposed pipeline segment.							
Complete one form for each unattached umbilical submitted in your application.							
3. Provide response/data for all items that are shaded. Other items as required.		_					
Provide one original and three identical copies of <u>all</u> application materials.							
Pipeline Route Data			<u> </u>				
List all blocks and lease numbers contacted by the pipeline. (Insert rows as needed)	Area	Block No.	Lease No.	Operator			
2 (If block is unleased, so note.)	id DINA	<u> </u>	BOGOT 1151				
3	Mississippi Canyon	711	G14016	Anadarko E&P Company LP/	ATP Oil and	as Cor	poration
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Contact Information	ATD OIL I O O O O O O				 		-
Applicant company name (RQW permittee/holder) Name of company representative signing application	ATP Oil and Gas Corporation				1		
Name of company representative signing application	Mickey W. Shaw				ļ		
o Phone No.	713-622-3311		1			ļ	-
1 Fax	713-403-7002		ļ		<u> </u>		
2 E-Mail	mshaw@atpog.com						
s Mailing address	4600 Post Oak Place Suite 200						
1	Houston, Texas 77027-9726						
5							
e ROW holder's MMS code (five digit)	1819						
3 Mailing address 4 5 6 ROW holder's MMS code (five digit) 7							
B Designated operator company name	ATP Oil and Gas Corporation						
Phone No.	713-622-3311				1		
o Fax	NA NA						
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	4600 Post Oak Place Suite 200						
	Houston, Texas 77027-9726				 		
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4 5 Operator's MMS code (five digit)	1040				 		
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Regulatory contact (Name)	Sharon DeSimoni						<u> </u>
e Company name	J. Connor Consulting, Inc.		ļ		 		
Phone No.	281-578-3388				ļ		
o Fax	281-578-8895						L
ı E-Malf	sharon.desimoni@iccteam.com						
2							
Technical contact (Name)	Daniel H. Longwell, P.E.						
4 Company:name	Bluewater Industries						
5 Phone No.	713-802-2060						
s Fax	713-802-2063						
o rax 7 E-Mail	dlongwell@bluewaterindustries.com		1				—
7 E-Mait	dionawenazouewaternoustres com						
Fees				 			
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Rental fee of \$15 per mile or every fraction thereof enclosed? (Required)	Yes						
2 Right-of-way length (miles) e.g., 5.71	1.35		ļ		 		
3 Total check amount	\$2,380.00						
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12 Popular designed for thurschore floury / Y/N)							Length of pipenie in receilar waters (leer)	-
Alternate line service, e.g., cit. gas. Bulk ags. Iff, investion, service, etc. N/A							Length of pipeline in State waters (recovar)	
ss Speeviser Control and Clear Acquisition system for least detection inestigated (VIN). If yes, system type, e.g., overhindt, pressure point analysis, southwester, etc. If yes a system type, e.g., overhindt, pressure point analysis, southwester, etc. If yes a system type, e.g., overhindt, greater and system type and system type and system type and system type and system type and system designed for from the system type and system designed for from the system type and system designed for from type and system designed for type and system designed for type and system designed for type and system designed for type and system designed for from type and system designed for from type and system designed for from type and system designed for from type and system designed for from type and system designed for from type and system designed for from type and system designed for from type and system designed for from type and system designed for from type and system designed for from type and system designed for from type and system designed for from type and system designed for from t				 			Pripeline designed for bi-directional flow? (Y/N)	
West system type, e.g., overrishort, pressure point analysis, volumetric, etc. N/A							Alternate line service, e.g., oii: gas, bulk gas, lift, injection, service, etc.	84
2 Pipeline Origin				 			Supervisor Control and Data Acquisition system for teak detection installed / [17/N]	65
Section Sect							If yes, system type, e.g., over/short, pressure point analysis, volumetric, etc.	66
Topic Facility Co. Pattern Note Number Note Number Note Number								
NumberIdentifier, e.g. A. 1, 4.B; 19338 (Number/Segment NumberIdentifier/NA) S. Well No. 006							Pipeline Origin	68 F
Manned platform? (YVINA)							Type Facility; e.g.; Platform; Well; Subsea Well; PLEM; Subsea Manifold; Subsea i ie-in	69 T
27 Area							Number/Identities: e.g. A, 1, 4-B, 13336 (Number/Segment Number/Identities/NA)	70
Tri							Area:	72
Top System designed for family page 2, (V/N/NA) No							Biock	73
No System designed for smart* pigs? (VINNA) No				-				74
Transmission Tran							Pig launcher? (Y/N)	75
Tz Pipeline Destination Tz Type Facility Ein Pistform; Well St bsea Well PLEM Subsea Manifold Subsea Tiesin MC 711 Gomez FOI				 		NO	System designed for "smart" pigs? (Y/N/NA)	76
Type Facility: e.g. Platform, Well, St. basa Well: PLEM, Subsea Marifold, Subsea Te-in. MC 711 Gomez FOI				 				
Manned platform? (YM/NA) Test						110 744 0 501	Pipeline Destination	78 F
### Manned platform? (YMNA); Tes ### Acea Mississippi Canyon ### Acea Mississippi Canyon ### Acea Till ###				<u> </u>	L	CONTROL OF A CONTRACT	Type Facility, e.g.: Platform, Well, St. bsea Well, PLEM, Subsea Manifold, Subsea Tie-in.	79 Î
Section Process Proc							Number/Identifier, e.g. A. 1, 4-B (Number/Segment Number/Identifier/NA)	80
BE Pig risk alver? (YMNA) AND STATE AND STATE BO STATE							Manned platform? (Y/N/NA)	81
BE Pig risk alver? (YMNA) AND STATE AND STATE BO STATE							Area	82
BE Pig risk alver? (YMNA) AND STATE AND STATE BO STATE							Block	83
BE Pig risk alver? (YMNA) AND STATE AND STATE BO STATE							OCS Lease	84
Pipeline Appurtenances Sea Manifold's base templates/etc atong pipeline other than at obtain or destination? (Y/N) Yes							Pig receiver? (Y/N/NA)	85
### Mainfolds base are projected; along pipeline other than at origin or destination? (Y/N) ### Mainfolds base are projected; appurtenant type ### If yes, specify appurtenant type ### If yes, specify appurtenant area and block location, e.g., MP 134 ### If yes, specify appurtenant area and block location, e.g., MP 134 ### MC 711 ### Construction/Air quality Data ### Construction/Air quality Data ### If yes, specify appurtenant area and block location, e.g., MP 134 ### If yes, specify appurtenant area and block location, e.g., MP 134 ### If yes, specify appurtenant area and block location, e.g., MP 134 ### If yes, specify appurtenant type ### Description in the projected of the proje								86
If yes, specify appurtenant type If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, MC 711 If yes, specify appurtenant area and block location, MC 711 If yes, specify appurtenant area and block location, MC 711 If yes, specify appurenant and block location, MC 711 If yes, specify appurenant and block location, MC 711 If yes, specify appurenant and block location, MC 711 If yes, specify appurenant and block location, MC 711 If yes, specify appurenant and block location, MC 711 If yes, specify appurenant and block location, MC 711 If yes, specify appurenant and block location, MC 711 If yes, specify appurenant and block location and will appurenant and will appurenant and will appurenant and will appurenant and will appurenant and will appurenant and will appurenant and will appurenant and will appurenant and will appurenant and will appurenant and will appurenant and will appurenant and will appurenant and will appurenant and will appurenant and wi							Pipeline Appurtenances	87 F
If yes, specify appurtenant type If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, e.g., MP 134 If yes, specify appurtenant area and block location, MC 711 If yes, specify appurtenant area and block location, MC 711 If yes, specify appurtenant area and block location, MC 711 If yes, specify appurenant and block location, MC 711 If yes, specify appurenant and block location, MC 711 If yes, specify appurenant and block location, MC 711 If yes, specify appurenant and block location, MC 711 If yes, specify appurenant and block location, MC 711 If yes, specify appurenant and block location, MC 711 If yes, specify appurenant and block location, MC 711 If yes, specify appurenant and block location and will appurenant and will appurenant and will appurenant and will appurenant and will appurenant and will appurenant and will appurenant and will appurenant and will appurenant and will appurenant and will appurenant and will appurenant and will appurenant and will appurenant and will appurenant and will appurenant and wi							Manifold/subsea templates/etc. along pipeline other than at origin or destination? (Y/N)	88
Section Process Section Sect		·					If yes, specify appurtenant type	89
2 Construction/Air Quality Data						MC 711	If yes, specify appurtenant area and block location, e.g., MP 134	90
Solution Property								
Maximum anchor spread (feet or NA) NA S Onshripe Facility Ocation Amelia, LA S Pipeline construction duration (days) 42 Days S Pipeline product data S S Pipeline product data S S Pipeline product data S S Pipeline product data S S Pipeline product data S S Pipeline product data S S Pipeline product data S S Pipeline product data S S Pipeline product data S S Pipeline product data S S Pipeline product data S S Pipeline product data S S Pipeline product data S S Pipeline product data S S Pipeline product data S S Pipeline product data S S Pipeline product data S S Pipeline product data S S S S S S S S							Construction/Air Quality Data	92 C
Maximum anchor spread (feet or NA) NA S Onshripe Facility Ocation Amelia, LA S Pipeline construction duration (days) 42 Days S Pipeline product data S S Pipeline product data S S Pipeline product data S S Pipeline product data S S Pipeline product data S S Pipeline product data S S Pipeline product data S S Pipeline product data S S Pipeline product data S S Pipeline product data S S Pipeline product data S S Pipeline product data S S Pipeline product data S S Pipeline product data S S Pipeline product data S S Pipeline product data S S Pipeline product data S S Pipeline product data S S S S S S S S							Pipeline installation method, e.g., lay barge, DP vessel, lack up	
Se Pipeline construction duration (days) 97 Construction start date (projected) 98 Pipeline product data 100 Design maximum flow rate of gas (mmct/d) 101 Gravity of gas (Atr =: 5.0) 102 Design maximum flow rate of colorondensate (bid) 103 API or specific gravity of pil/condensate 104 H2S: concentration (ppm) 105 Maximum anticipated: pipeline temperature (degrees F) 106 CO ₂ concentration (ppm) 107 Inhibition program planned? (Y/N)							Maximum anchor spread (feet or NA)	94
Pipeline construction duration (days)		,					Onshore Facility Location	95
97 Construction start date: (projected): 98 99 Pipeline product data 100 Design maximum flow rate of gas (mmct/d): 101 Gravity of gas (Air = 1.0): 102 Design maximum flow rate of cil/condensate (b/d): 103 API or specific gravity of cil/condensate: 104 H2S concentration (ppm): 105 Maximum anticipated pipeline temperature (degrees: F): 106 CO ₂ concentration (ppm): 107 Inhibition program planned? (Y/N): 108 Yes							Dipoline construction duration (days)	
98 Pipeline product data 50 50 100 Design maximum flow rate of gas (mmct/d) 50 0.813 0						5/15/2005	Construction start date (projected)	97
100 Design: maximum flow rate of gas (mmct/d) 50 101 Gravity: of gas: (Alt = 1.0) 0.813 102 Design: maximum flow rate of pil/condensate (b/d) 6,000 103 API or specific gravity: of pil/condensate 0.88 104 H2S: concentration (ppm) Nil 105 Maximum: anticipated pipeline temperature (degrees: F) 120 106 CO ₂ concentration (ppm) 4200 107 Inhibition program planned? (Y/N) Yes								
100 Design: maximum flow rate of gas (mmct/d) 50 101 Gravity of gas (Ait = 1.0) 0.813 102 Design: maximum flow rate of pil/condensate (b/d) 6,000 103 API or specific gravity of pil/condensate 0.88 104 H2S concentration (ppm) Nil 105 Maximum anticipated pipeline temperature (degrees F) 120 106 CO ₂ concentration (ppm) 4200 107 Inhibition program planned? (Y/N) Yes							Pipeline product data	99 F
101 Gravity of gas (Air = 1.0) 0.813 0.800 102 Design maximum flow rate of oil/condensate (bid) 6,000 103 API bit specific gravity of oil/condensate 0.88 104 IP S concentration (ppm) Nil 105 Maximum anticipated pipeline temperature (degrees F) 120 106 CO ₂ concentration (ppm) 4200 107 Inhibition program planned? (Y/N) Yes							Design maximum flow rate of gas (mmct/d)	100 L
103 API or specific gravity of oil/condensate 0.88							Gravity of gas (Air = 1.0)	101
103 API or specific gravity of oil/condensate 0.88							Design: maximum flow rate of oil/condensate (b/d):	102 L
104 H2S concentration (ppm) Nil		·					API or specific gravity of oil/condensate	103
10s Maximum anticipated pipeline temperature (degrees F) 120 10e CO ₂ concentration (ppm) 4200 107 Inhibition program planned? (Y/N) Yes						The state of the s	H2S concentration (ppm)	104
106 CO ₂ concentration (ppm) 4200 107 Inhibition program planned? (Y/N) Yes					ļ		Maximum anticipated pipeline temperature (degrees F)	105 N
107 Inhibition program planned? (Y/N)							CO ₂ concentration (ppm)	106
								
							Hydrates anticipated (Y/N)	
Paraffin anticipated (V/N)							Paraffin anticipated (Y/N)	109 F
110								
Diameter 1 Diameter 3				Diameter 3	Diameter 2		Sub-marraed Component Dusign Data	111
1113 Dutside diameter (inches) 6.895 - dynamic flexible pipe		\			<u> </u>	6.895 - dynamic flexible pipe		

	·		····				<u> </u>
A SSW2028222222222222222222222222222222222	B	С	D	E	 	G	Н
113 Wall thickness (inches)	1.4475 - layers, as per riser data			 	+		
114 Grade	NA NA					 	
115 Hydrostatic test pressure (psig)	9,375		ļ <u>.</u>	<u> </u>			
116 HTP duration (hours) (Must be equal to or greater than eight)	8						
117 Type external corrosion coating	polypropylene						
118 Corrosian coating thickness (mils)	236						
119 Concrete coating density (pcr)	NA NA						
120 Coating thickness (inches)	NA NA						
121 Type Internal corrosion coating (Type/NA)	NA NA						
122 Coating thickness (mils) (Mils/NA)	NA NA						
123 Bare pipe specific gravity:	1.83						
124 Weighted pipe specific gravity	NA NA						
125 Pipe is:non-standard? (Y/N)	Yes						
If yes, note type, e.g., coil tubing, pipe-in-pipe, flexible pipe, other (specify) (Type/NA)	Flexible Pipe				+		
127	T TEXABLE TIPE						
128 Cathodic Protection Design Data			1				
129 Design Type; e.g. bracelet anodes, anode sleds	NA NA		 		1		
130 Anode Type; e.g. Galvalum III; Aluminum; etc.	NA NA				-		
The state of the s					-		
131 Net anode weight (pounds):	NA NA						
132 Spacing (feet):	NA NA			 	-		
133 Number of anodes	NA.					-	
134 :: Anode life (years):	NA NA						
135 Designs for systems other than bracelet anodes required: (Attached/NA):	NA NA					ļ	L
138							
137	and the second second second second second second second second second second second second second second seco						
138 Departing Riser Design Data	<u>Diameter 1</u>	Diameter 2	Diameter 3				
139 Outside diameter (inches)	6.895 - flexible pipe						
tický kim minimi iziticki kilomini, ktoré se se se se se se se se se se se se se							
140 Wall thickness (inches)	1.4475 - layers, as per riser data						
140 Wall Dickness (inches): 141 Grade:	1.4475 - layers, as per riser data NA						
141 Grade	NA						
141 Grade 142 Hydrostatic test pressure (psig)	NA 9,375	In S.Z.	Above S.Z.				
141 Grade 142 Hydrostatic test pressure (psig) 143 HTP duration (hours) (Must be equal to or greater than eight) 144 splash zone=S.Z.	NA 9,375 8	In S.Z.	Above S.Z.				
141 Grade 142 Hydrostatic test pressure (psig) 143 HTP duration (hours) (Must be equal to or greater than eight) 144 splash zone=S.Z. 145 Type external corresion coating	NA 9,375 8 Below S.Z.	in S.Z.	Above S.Z.				
141 Grade 142 Hydrostatic test pressure (psig) 143 HTP duration (frours) (Must be equal to or greater than eight) 144 splash zone=S.Z. 145 Type external corresion coating 146 Coating thickness (mile or inches)	NA 9,375 8 Below S.Z.	in S.Z.	Above S.Z.				
141 Grade 142 Hydrostatic test pressure (psig) 143 HTP duration (hours) (Must be equal to or greater than eight) 144 splash zone=S.Z. 145 Type external corrosion coating 146 Coating thickness (mile or inches) 147 Type internal corrosion coating (Type/NA)	NA 9,375 8 Below S.Z.	in S.Z.	Above S.Z.				
141 Grade 142 Hydrostatic test pressure (psig) 143 HTP duration (hours) (Must be equal to or greater than eight) 144 splash zone=S.Z. 145 Type external corrosion coating: 146 Coating thickness (mile or inches) 147 Type internal corrosion coating (Type/NA) 148 Coating thickness (mile) (Mils/NA)	NA 9,375 8 Below S.Z.	in S.Z.	Above S.Z.				
141 Grade Hydrostatic test pressure (psig)	NA 9,375 8 Below S.Z.	in S.Z.	Above S.Z.				
141 Grade 142 Hydrostatic test pressure (psig) 143 HTP duration (hours) (Must be equal to or greater than eight) 144 splash zone=S.Z. 145 Type external corrosion coating: 146 Coating thickness (mils or inches) 147 Type internal corrosion coating (Type/NA) 148 Coating thickness (mils) (MisrNA) 149 Riser guard design attached? Required if origin is calsson or platform (Y/NA) 150 Catenary riser? (Y/N)	NA 9,375 8 Below S.Z.	in S.Z.	Above S.Z.				
141 Grade 142 Hydrostatic test pressure (psig) 143 HTP duration (hours) (Must be equal to or greater than eight) 144 splash zone=S. Z. 145 Type external corrosion coating. 146 Coating thickness (mils or inches) 147 Type internal corrosion coating (Type/NA) 148 Coating thickness (mils) (Mils/NA) 149 Riser guard design attached? Required if origin is calsson or platform (Y/NA) 150 Catenary riser? (Y/N) 151 If yes, VIV reduction, installation tension, anchoring, tension monitoring attached? (Y/NA)	NA 9,375 8 Below S.Z.	in S.Z.	Above S.Z.				
141 Grade	NA 9,375 8 Below S.Z. same						
141 Grade	NA 9,375 8 Below S.Z. same	in S.Z. Diameter 2	Above S.Z. Diameter 3				
141 Grade 142 Hydrostatic test pressure (psig) 143 HTP duration (hours) (Must be equal to or greater than eight) 144 splash zone=S.Z. 145 Type external corrosion coating 146 Coating thickness (mils or inches) 147 Type internal corrosion coating (Type/NA) 148 Coating thickness (mils) (Mils/NA) 149 Riser guard design attached? Required if origin is calsson or platform (Y/NA) 150 Catenary riser? (Y/N) 151 If yes, VIV reduction, installation tension, anchoring, tension monitoring attached? (Y/NA) 152 Receiving Riser Design Data 154 Outside diameter (inches)	NA 9,375 8 Below S.Z. same						
141 Grade 142 Hydrostatic test pressure (psig) 143 HTP duration (hours) (Must be equal to or greater than eight) 144 splash zone=S.Z. 145 Type external corrosion coating 146 Coating thickness (mils: or inches) 147 Type internal corrosion coating (Type/NA) 148 Coating thickness (mils) (Mils/NA) 149 Riser guard design attached? Required if origin is calsson or platform (Y/NA) 150 Cateriary riser? (Y/N) 151 If yes, VIV reduction, installation tension, anchoring, tension monitoring attached? (Y/NA) 152 153 Receiving Riser Design Data 154 Cutside diameter (triches) 155 Wall thickness (inches)	NA 9,375 8 Below S.Z. same						
Interpretation (Processor (Page) Interpretation (Processor (Page)) Inter	NA 9,375 8 Below S.Z. same						
Grade Hydrostatic test pressure (psig) Hydrostatic test pressure (psig) HTP duration (hours) (Must be equal to or greater than eight) splash zone=S.Z. splash zone=S.Z. Sp	NA 9,375 8 Below S.Z. same						
Grade Hydrostatic test pressure (psig) HTP duration (hours) (Must be equal to or greater than eight) Splash zone=S.Z. Splash zone=S.Z. Splash zone=S.Z.	NA 9,375 8 Below S.Z. same Diameter 1 N/A	Diameter 2	Diameter 3				
Grade Hydrostatic test pressure (psig) HTP duration (frours) (Must be equal to or greater than eight) Splash zone=S.Z.	NA 9,375 8 Below S.Z. same						
Grade Hydrostatic test pressure (psig)	NA 9,375 8 Below S.Z. same Diameter 1 N/A	Diameter 2	Diameter 3				
141 Grade 142	NA 9,375 8 Below S.Z. same Diameter 1 N/A	Diameter 2	Diameter 3				
Grade Hydrostatic test pressure (psig) HYP duration (hours) (Must be equal to or greater than eight) splash zone=S.Z. Splash zone=S.Z. Splash zone zone-Splash zone zone-Splash zone-S.Z. Splash zone=S.Z. Splash zone-S.Z. Splash zone-Splash z	NA 9,375 8 Below S.Z. same Diameter 1 N/A	Diameter 2	Diameter 3				
Grade Hydrostatic test pressure (psig)	NA 9,375 8 Below S.Z. same Diameter 1 N/A	Diameter 2	Diameter 3				
Grade Hydrostatic test pressure (psig) HTP duration (frours) (Must be equal to or greater than eight) splash zone=S.Z.	NA 9,375 8 Below S.Z. same Diameter 1 N/A	Diameter 2	Diameter 3				
Grade Hydrostatic test pressure (psig)	NA 9,375 8 Below S.Z. same Diameter 1 N/A	Diameter 2	Diameter 3				
Internation Internation	NA 9,375 8 Below S.Z. same Diameter 1 N/A	Diameter 2	Diameter 3				
Internation Internation	NA 9,375 8 Below S.Z. same Diameter 1 N/A	Diameter 2	Diameter 3				
141 Grade	NA 9,375 8 Below S.Z. same Diameter 1 N/A	Diameter 2	Diameter 3				

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	В	С	Г	I E	T F	G	н
169 Flange type (ANSI/API)	API 10K						
170 Flange pressure rating (psig)	10,000				<u> </u>	1	
170 Flange pressure rating (psig) 171 Derated pressure rating (psig/NA)	10,000 N/A					 	
1/1 Detailed pressure rating (paig/NA)					 	 	
172 Valve type (ANSI/API)	API 10K	·	<u> </u>			 	
173 Valve pressure rating (psig)	10,000					 	
174 Derated pressure rating (psig/NA)	N/A				<u> </u>	ļ	
175						<u> </u>	
176 Pipeline Burial Data						<u> </u>	
177 Buried minimum of three feet? Y/N/Self (Burial required if less than 200 water depth)	No						
178 Burial method (jet, plow, self, other(specify))	N/A						
179 If self burial, provide seafloor strength in ksf. (Must be less than 0.2 ksf) (kips/NA)	N/A						i I
Data supporting self burial attached? (Y/NA)	N/A						
1811		·					
182 Miscellaneous Data							
	V						
183 Non-discrimination in employment form attached? (Required)	Yes					·	
184						 	<u> </u>
185 Oil Spill Financial Responsibility Requirement Determination					ļ		
186 Static Pipeline Volume (Bbls.) If greater than 1,000 then WCD volume required.	111				ļ	<u> </u>	ļ
197 Worst case discharge volume (Bbls.) If greater than 1,000 then OSFR required.	NA NA					L	ļ
Proposed Right-of-Way included under company OSFR coverage? (Yes/Pending/NA)	NA NA						
189							
190 Certified plat attached? Plat is required:	Yes	-					
191 Diskette per NTL 98-09 attached? Diskette is required:	Yes					<u> </u>	
192	130						
	No				-		
193 Does pipeline cross into State waters (Y/N)	N/A					 	
If yes, State permit required (Attached/Applied For/NA)					 	-	
195 If yes, COE permit required (Attached/Applied For/NA) 196	N/A	•			 		
196							
197 Minimum water depth (feet below sea level)	2940						
198 Maximum water depth (feet below sea level)	2980						
199							
200 Water depth greater than 400 meters? (Y/N)	Yes						
201 If Yes, Chemo study required (see NTL 2000-G20) (Attached/NA)	previously submitted			_			
202							
203 Deep Water Operations Plan submitted to MMS? (See NTL 2000-N06) (Y/NA)	Yes						
204 If yes, date submitted (Date/NA)	25-Mar-05						
and the state of t							
206 Pipeline to be towed to location? (Y/N)	No		·· ·				
	110				 		
207 If yes, dragged on bottom? (Y/N/NA)							
208					ļ		ļI
209 Artificial reef in vicinity? (Y/N)	No						
210 If Yes and PL in La., PL must be > 500' away. Confirm Y/NA							
211 Distance to reef (feet).							
212 If Yes and PL in TX., PL must be > seven times water depth away. Confirm Y/NA							
213 Distance to reef (feet).							
214							
215 Hazard Report submitted? (Yes) Hazard Report is required:	Yes				İ		
279 History Nation and indicate the state of	les				 		
					 		
217 Shallow Hazards Analysis Statement included? (Yes) SHAS is required in cover letter.	Yes				ļ	 	
218							
219 Umbilical associated with pipeline? (Y/N):	Yes						
Umbilical type, e.g., hydraulic, electric, other(specify) (Type or NA)	hydraulic/gas lift						
Umbilical outside diameter (inches) (Diameter or NA)	4-inch				L		
222 Attached to pipeline? (Y/N/NA; If No, will be assigned a unique segment number)	No						
	No - Considered Appurtenance				1		
223 If no, separate application form attached? (Yes/NA) 224							
14471							

		В	С	D	ш	F	G	H
		No						
225 Does pipeline contact and	horage area or fairways? (Y/N)	NA						
226 If Yes, burial depth in a	inchorage areas or fairways consistent with COE permit? (Y/NA)	NA NA						<u> </u>
227 If yes, COE permit atta	ched? (Y/NA/Pending)							
228		Ties .						
229 Pipeline Crossing Data		No						
	ross an existing pipeline (Y/N)	Operator	Segment No.	Size (inches)	Service	Notified?		
	, adding data rows as required.	Оролцо.						Li
232	Later Street Proof De (Noo(NA)	N/A						ļI
233 If yes, minimum cleara	nce between lines must be 18". (Yes/NA) depth, must have 3' cover or concrete mats. (Confirm cover or							
	depth, must have 3 cover of condete mais. (Gorman cover of	N/A						
234 concrete mat.)	V4 (Confirm Voc(NA)	N/A						
235 If sand bags, slope is 3		N/A						
236 If concrete mat, specif	/ manufacturer	N/A						
237 If concrete mats, mat e	edges jetted below mudline. (Yes/NA) ator notified? (Y/N/O O = crossed pipeline owned by applicant)	N/A						
238 Crossed pipeline opera	ator notified? (17/4/O O = clossed pipeline owned by approant)							
239 240 H ₂ S Contingency Plan a	nd Modeling Data					ļ		
H & Operations Continue	ncy Plan attached as H ₂ S concentration greater than 20 ppm							
241 (Y/Pending/NA)	100g	NA						├ ──
241(17/7-enging/19/4)								
	La La Canada tration program than 500 som (Vinending/NA)	NA NA					ļ	ļ
242 Air Dispersion Model atta	thed as H ₂ S concentration greater than 500 ppm (Y/pending/NA) y Plan attached as crossed pipeline carries H ₂ S in concentrations							1
H ₂ S Crossing Condigenc	y Figir attached as crussed piperine carroo 1/20 in conscious	NA						
243 greater than 20 ppm (Y/P	ending/NA)					<u></u>		<u> </u>
244	The state of the s							
245 Subsea Tie-in Data	ibsea pipaline? (Y/N)	No						1
246 Does pipeline tie into a si	IDSER DIDERRE (1 \$ 1)():::::::::::::::::::::::::::::::::::					<u> </u>		4
7 Ties to existing valve of particular and particul	or hot tap? (Identify which/NA) peline being tied in to (SN/NA)							
248 Segment number of pi 249 MAOP of pipeline beir 250 If existing valve, letter 251 If hot tap, appurtenance	g tied in to (MAOP/NA)						ļ	
249 MAOP of pipeline bell	of no objection from tie-in operator attached? (Yes/NA)							
250 If existing valve, letter	e application submitted to MMS? (Yes/NA)						<u> </u>	ļ
251 If not tap, appurtenant	red? (Y/NA) Required if less than 500' water depth.							
252 Is assembly snag proc253 If sand bags used, slo	ne is 3/1 (Y/NA)							-
253 If sand bags used, slo254 If sand bags used, 3' or	coverage required (Y/NA)						ļ <u></u>	
255 II Sand Dags used, 5 C	overage required (1774)						-	
256 Surface Tie-in Data	into another pipeline at a surface location? (Y/N)	No				-		-
	peline being tied in to (SN/NA)						ļ	
 Segment number of p MAOP of pipeline beir 	ng tied in to (MAOP/NA)							
259 MAOP of pipelifie bell 260	19 100 iii to (112 y					<u> </u>		
Soill Peenonee Plan Da	ta .			ļ		 	 	+
	plan (OSCP/OSRP per NTL 98-30)	OSRP		<u></u>			 	+
age Date smill plan submit	ed to MMS	3/23/2005				 		+
263 Date spill plan submit 264 Date spill plan approv	ed (Actual Date or "Pending")	3/29/2005						+
204 :::: Late spain plati approx		10 To 10 To				 	+	+
265 266 Safety Schematic Inform	nation			<u> </u>				+
200 Safety Schematic Information	d? (well; separator; pump, etc.)	Well				 	 	
MSDMAND/SITE OF	source shown? (psig)	6,500				-		+
ass Origin/destination specific	cation breaks shown on schematic. (Y/NA)	Yes				 		+
200 Receiving segment number	per noted? (Segment Number or N/A)	N/A					+	+
271 Receiving segment no	D. MAOP (psig) (MAOP or N/A)	N/A			<u> </u>		+	+
and Colevilated hingling MAO	P (osia):	7,500				+		+
273 Operator responsibility tr	ansfer point shown? (Yes/NA)	NA NA				+	+	
274				 	 	+		+
275 Collapse Information (E	Deepwater Pipelines Only)		 			+	+	+
276 Water depth (feet)		3080			1			
270 Water deptir (100)	· · · · · · · · · · · · · · · · · · ·							

	A	В	C	D	E	F	G	н
277	External pressure (psig)	1333						
	Collapse pressure (psig)	3.237						
278 279	Safety factor	2.4	1					
		Attached - Performed by Flexible						
280	Collapse calculations are required. (Attached/NA)	Pipe manufacturer						
281	, and the second							
	Safety Design Review							
	Pipeline Origin							
	PSHL required at departing end of pipeline (Confirm Yes)	Yes	**					
205	PSHL must be downstream of choke and/or flow restrictions (Confirm Yes)	Yes						
203	Total must be downstream of choke and/or now restrictions (Commit Tes)	163		-				
286	For a well, if MSP > MAOP, a redundant PSH and independent SDVs required (Confirm Yes)	N/A						
	For production equipment, if MSP > MAOP, a redundant PSH with independent SDV is required	100	+					
	or a vented PSV is required (Confirm Yes/NA)	N/A						
						 		
	If bi-directional flow, SDV required (Confirm Yes/NA)	N/A	-		<u> </u>	+		
	If pig trap present, safety equipment can not be bypassed (Confirm True)	N/A		+		-		
	If pump on line, must be consistent with API RP 14C A7 (Confirm Yes/NA)	N/A	4			+		
	Pipeline Destination	.,,		-		 		
	If production facility and uni-directional flow, SDV and FSV required (Confirm Yes/NA)	Yes		1				
293	If production facility and bi-directional flow, SDV and PSHL required (Confirm Yes/NA)	N/A				-		
	If subsea tie-in and uni-directional flow, FSV and block valve required (Confirm Yes/NA)	N/A						
	If subsea tie-in and bi-directional flow, block valve required (Confirm Yes/NA)	N/A						
	If gas lift or water injection flowline on unmanned platform, FSV required (Confirm Yes/NA)	Yes						
297	If gas lift or water injection flowline on manned platform, SDV required (Confirm Yes/NA)	Yes						
	If crossover platform (pipeline does not receive production), SDV required at boarding point and							i
298	PSHL required at departing point (Confirm Yes/NA)	N/A				1		
299	If crossover platform is non-manned and non-production, FSV required (Confirm Yes/NA)	N/A						1
300								
301	Departure Data	and the second s				,		
302	Waiver from NTL 98-20 (buoying of hazards) requested? (Y/N)	Yes						
	Other departures requested? (Y/N)	No						
304	If yes, specify.							
305							***	
306								
307								
308						-		
309			<u> </u>					
310							i i	
311								
371						1		
312			 			 		
313				-		 		
314	De Ned Federa Dede Delevir Third Line			 		ļ		
315	Do Not Enter Data Below This Line - MMS Use Only		ļ	 				
316	TANK WE ARE SAITOV AUGST	***	 					
	PIPELINE MASTER ENTRY SHEET		100 =	<u> </u>		-		
-	Name		MMS Engineer en					
	Date		MMS Engineer en					
	Segment Number		MMS Engineer en					
	Right-of-Way Number		MMS Engineer en	itry				
	Right-of-Way Permittee							
	Right-of-Way Permittee Code							
	Operator	ATP Oil and Gas Corporation]
325	Operator Code	1819						
	Approval Code	Right-of-Way						

A	В	1 c	T 6 T			G	н
327 Authority Code	1	MMS Engineer entry			<u> </u>	\	<u> </u>
328 Pipe Size	6.895 - dynamic flexible pipe	Mano Engineer e	, idy				
329 Product Code	G.GGG GYTGITHIG HOMERO PIPE	MMS Engineer er	ntry				
330		WING LIIGHTCCI CI					
331 ORIGIN		-	T			1	
332 Facility Type	MC 711 Subsea Well No 006						
333 Identifier	SS Well No. 006						
334 Area	Mississippi Canyon						
335 Block	711						
336 Lease	OCS-G-14016						
337		1					
338 DESTINATION							
339 Facility Type	MC 711 Gomez FOI		T		100000		
340 Identifier	"A"						
341 Area	Mississippi Canyon						
342 Block	711						
343 Lease	OCS-G-14016						
344							
345 OCS Segment Length	7,141						
346 State + Federal Pipeline Length	7,141						
347 Cathodic Code	NA NA						
348 Cathodic Life Time (Years)		MMS Engineer er	ntry				
349 Minimum Water Depth (feet)	2940						
350 Maximum Water Depth (feet)	2980						
351				•			
352 Buried Designator Flag	No No		<u> </u>				
353 Bi-directional Flag	Yes						
354 Alternate Service	N/A						
355 Recv Segment No. (Sub-surface)	0	<u> </u>					
356 Recv MAOP	0						
357 Assigned MAOP		MMS Engineer er	ntry				
358 Pipeline Status Code	Proposed		4				
359 Right-of-Way Status Code	Pending		ļ				
360							
361 Comments	1	MMS Engineer er	ntry				

Pipeline Review Report

Review : Adjudication Review

Permit Number: P-15168 Permit Type: ROW Application Submittal Received: 05/31/2005

Operator : ATP Oil & Gas Corporation

ROW Number: G26865 Reviewer Received Date: 06/02/2005 Review Completed: 06/02/2005

Segments : 15168, 15169

Reviewer : GLAZNERA

Remark :

Item	Response Text
2	The corporation is qualified.
	On file with MMS.
	\$300,000 right-of-way grant bond on file.

ATP OIL & GAS CORPORATION

June 7, 2005

Mr. Donald C. Howard Regional Supervisor U. S. Department of the Interior Minerals Management Service 1201 Elmwood Park Boulevard New Orleans, Louisiana 70123-2394



Attention:

Mr. Alex Alvarado

RF:

Application for a 6.895-Inch OD Bulk Oil Right-of-Way Pipeline, Production Riser, Rigid Jumper And Associated Umbilical To Be Installed In and/or Through Blocks 711 and 755, Mississippi Canyon Area, OCS Federal Waters, Gulf of Mexico, Offshore, Louisiana

Gentlemen:

By letter dated May 23, 2005 (revised June 6, 2005), ATP Oil & Gas Corporation (ATP) filed an application for a right-of-way easement two hundred feet (200') in width for the construction, maintenance and operation of a 6.895-inch OD bulk oil right-of-way pipeline and associated umbilical to be installed from subsea Well No. 006, in and/or through Blocks 711 & 755, Mississippi Canyon Area; OCS Federal Waters, Gulf of Mexico, Offshore, Louisiana. Minerals Management Service has assigned the application as Segment No. 15168 and 15169.

In accordance with the regulations contained in Title 30 CFR 250.1015(c), ATP sent a copy of the above referenced pipelines via certified mail, return receipt requested to every lessee and/or right-of-way holder whose lease or right-of-way was intersected by the proposed right-of-way. In further support of our application, enclosed are copies of the executed mail return receipts from the following affected operators and/or right-of-way holders:

Nexen Petroleum U.S.A., Inc.

7003 2260 0003 0201 0912

Should you have any questions or require additional information please contact our regulatory representative, Sharon DeSimoni at (281) 578-3388.

Sincerely,

ATP OIL & GAS CORPORATION

Michay W. Shaw &

Vice President, Production Operations

MWS:SD

Enclosure

HOUSTON, TEXAS 77027-9726 713-622-3311

FAX: 713-622-5101

SENDER: COMPLETE THIS SECTION	COMPLETE THIS SECTION ON DELI	VERY
 Complete items 1, 2, and 3. Also complete item 4 if Restricted Delivery is desired. Print your name and address on the reverse 	A Signature X)) could	☐ Agent ☐ Addressee
so that we can return the card to you. Attach this card to the back of the mailpiece, or on the front if space permits.	B. Received by (Printed Name)	C. Date of Delivery
Article Addressed to:	 D. Is delivery address different from iten If YES, enter delivery address below 	
Neven Pettoleum, USA, The 12790 Ment Dr., Ste. 800 Dallas, TX 76251-1270	,	
12790 Ment Dr., Ste. 800		
MILOS IX 10501-1510 F	3. Service Type	
ILME of	Certified Mail Express Mai	1
Allh: Larry McRae	1 /	eipt for Merchandise
•	4. Restricted Delivery? (Extra Fee)	☐ Yes
2. Article Number 7003 2	560 0003 0501 0915	**************************************
DO E 0011 A 10001		

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